

MAHARASHTRA POLLUTION CONTROL BOARD

Minutes of Third Meeting of the Technical Committee Under Product Mix Date-12/12/2022

Venue- Conference Hall, 4th Floor, Maharashtra Pollution Control Board, Sion, Mumbai.
Outstation Members were present via Microsoft Team Video Conference.

Technical Committee Members Present for the meeting:

- | | |
|---|-----------------|
| 1. Dr. J. B. Sangewaar, Assistant Secretary(Technical), MPCB, | Chairman |
| 2. Sh. B.R. Naydu, Ex-Regional Director, CPCB, Vadodara, | Member |
| 3. Dr. Ravindar Kontham, National Chemical Laboratory, Pune, | Member |
| 4. Sh. N.N. Gurav, Regional Officer(BMW), MPCB | Member Convener |

The Chairman of the Committee welcomed the Committee members and minutes of the 3rd meeting of the Technical Committee Under Product Mix were confirmed. Committee deliberated on the eleven agenda items and following decisions were taken:

Agenda Item No.	1
Proposal No.	MPCB-CONSENT-0000137807
Project Details	M/s. Maharashtra Aldehydes & Chemicals LTD. Plot No. A-17, MIDC area, Mahad, Tal.- Mahad, Dist. Raigad.
NIPL Certificate	NIPL Certificate issued by Aditya Environmental Services Pvt. Ltd., dtd. 20.04.2022.
Name of the Industry Representative present	1. Mukesh Shahari, Director 2. D.N. Patil, General Manager

Introduction:

This has reference to the online proposal submitted vide No. MPCB-CONSENT-0000137807 along with the copies of documents seeking consent to establish for expansion under change in product – mix as per the provisions of EIA Notification, 2006 amended on 23/11/2016 & on 02/03/2021.

Existing Clearances:

1. Environmental Clearance is vide No. SEIAA-EC-0000002254 Dated. 24/04/2020.
2. Consent to Establish for expansion obtained with vide No. Format 1.0/AS(T)/UAN No. 0000092765/CE2011000757 dtd. 12.11.2020 granted for a period upto commissioning of the project or upto 5 year whichever is earlier.
3. First consent to Operate obtained with vide No. Format 1.0/AS(T)/UAN No.0000104788/ CO dtd. 17/08/2021 valid upto 28/02/2024.

This is resubmission case. The case was discussed in earlier meeting i.e. first sitting of 2nd Technical Committee meeting of product mix dtd.18/08/2022. During this meeting it was noticed by the committee that:

- i) PP has not switched to the cleaner fuel.
- ii) PP was unable to submit the details of Liquor Ammonia generation either in By-products or in Hazardous Wastes Category and disposal of the same.
- iii) The total water consumption and trade effluent generation will be increased.
- iv) The Coal consumption and steam requirements will be increased.

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- v) PP was unable to submit the details of the process emissions from the existing products as well as from proposed products and details of comparison of the pollution load.

After due deliberations Technical Committee had been decided to defer the case and asked PP to reassess their pollution load, along with the NIPL certificate and was advised the PP to furnish above details.

The industry has given presentation regarding compliances with earlier MOM of first sitting of 2nd Technical Committee meeting of product mix dtd.18/08/2022. and gist of the same is as follows:

Project Details:

A. Products with change in product mix as below:

Sr.no.	Product	As per EC (*)	As Per CTO (#)	Proposed change	After product mix	Remarks
		Quantity in MTPM				
1	Alkyl Esters of Phthalic acids	1600	1200	0	1200	No change
2	Ethyl Benzoate	30	30	0	30	No change
3	Ethyl Butyrate	100	50	0	50	No change
4	Ethyl Propionate	50	50	0	50	No change
5	Ethyl Laurate	5	0	0	0	No change
6	Ethyl Caprate	5	0	0	0	No change
7	Ethyl Caproate	5	0	0	0	No change
8	Ethyl Heptanoate	5	0	0	0	No change
9	Ethyl 2-Methyl Butyrate	5	0	0	0	No Change
10	Ethyl Valerate	5	0	0	0	No Change
11	Ethyl Cinnamate	4	0	0	0	No Change
12	Triethyl Citrate	100	50	0	50	No Change
13	Tributyl Citrate	15	0	0	0	No Change
14	AcetylTributyl Citrate	35	35	0	35	No Change
15	Syngaldehyde	1.5	1.5	0	1.5	No Change
16	Trimethyl Hydroquinone (TMHQ)	20	20	-7	13	Decrease in Quantity
17	Anisole	500	0	0	0	No Change
18	Anethole	300	0	0	0	No Change
19	4-Methoxyl Acetophenone	260	0	0	0	No Change
20	1-Piperidino 1- cyclohexene	40	0	0	0	No Change
21	Di hydra Anethole	20	0	0	0	No Change
22	Cis Anethole	10	0	0	0	No Change
23	2-Methoxy Acetophenone (2 MAP)	1	0	0	0	No Change
24	2,4-Diacetyl Anisole	1	0	0	0	No Change




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Sr.no.	Product	As per EC (*)	As Per CTO (#)	Proposed change	After product mix	Remarks
		Quantity in MTPM				
25	Cyclopentanone	100	0	0	100	No Change
26	Anhydrous Alcohol	1200	500	0	500	No Change
27	Distillation of solvents	400	365	0	365	Non- EC product
28	Maxvit Vitamin Formulation	100	100	0	100	Non- EC product
29	Sodium Sulphate	500	50	0	50	No Change
30	Acetic Acid	105	0	0	0	No Change
31	Propionic acid	180	0	0	0	No Change
32	Sanitizers	0	200	0	200	Non- EC product
33	Acetonitrile	0	0	+300	300	New Plant
34	Diethyl Ketone	0	0	+100	100	New Plant
	TOTAL	5442.5	2751.5	+400	3144.5	Capacity increase by 11.5% against CTO, but within EC quantity

Query No. 1: PP has not switched to cleaner fuel.

PP reply : CTO has fuel for TFH (41kcal) as Coal/ FO. However, the TFH installed is designed for Coal, and they only use Coal as fuel. PP has confirmed that they will not use FO in future in TFH. PP has applied on MPCB portal for amendment in CTO for deleting FO as Fuel - Application no-MPCB -Consent- 0000104788

Query No. 2: PP was unable to submit the generation of liquor ammonia either in by-products or in hazardous waste category and disposal of the same.

PP Reply: In proposed Acetonitrile manufacture, raw materials Acetic acid and Ammonia are reacted in catalytic bed reactor, the product is flashed in a column to separate part of the unreacted ammonia, acetonitrile-water as overhead vapours.

- On condensation in heat exchanger, acetonitrile-water mixture is sent to purification column and uncondensed ammonia is sent to scrubber.
- Similarly balance ammonia from polishing reactor is separated and sent back to scrubber.

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- Ammonia from both reactor is scrubbed in ammonia scrubber and liquor ammonia generated from scrubber is sent to ammonia stripper for ammonia recovery. The recovered ammonia is totally recycled back to reactor.
- Stripper bottoms liquid is recycled back to ammonia scrubber. Entire ammonia is handled in close loop

Thus, there is no liquor ammonia generation as by-product / hazardous waste in the manufacturing process

Query No. 3: Total water consumption and effluent generation will be increased.

(i) Water Aspect:

Purpose/Category	Quantity (cmd)		
	as per EC	** Existing Consented	Post change of product mix
1) Industrial Cooling	295	125.5	298.5
2) Domestic Purpose	15	11.5	11.5
3) Processing whereby water gets polluted, and pollutants are easily biodegradable	75	82	53
5) Gardening	25	7	7
Total Water	410	226	370
Recycled water		32.3	22
Fresh water requirement	352	193.7	348

The Additional water requirement is mainly due to the new proposed new cooling tower Process water will be reduced due to (a) reduction in TMHQ production quantity and (b) reduction in plant/equipment washing

It is submitted that the water quantity post product mix change is within the EC sanctioned limit and hence permissible.

(ii) Waste water aspect

Category		Quantity (CMD)			Remarks
		As per EC (*)	**Existing Consented	Post product mix	
Trade effluent	Process Effluent	95	43.2 47.65	39.5 43.32	Reduction due Change of product mix (TMHQ production reduced)
	Plant washings		39	25	Optimization of number of products change-overs eliminating equipment washings
	Cooling & utilities		17.6	29.32	New proposed cooling tower




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Total Trade effluent	95	100	94	
Dom. Sewage	12	8	8	No change
Total Effluent	107	108	102	
Condensate recycled		4.5	12	Back to process
Effluent to ETP	100.5	103	89.8	
Treated Eff recycled	33	35.5	22.32	to process
Effluent discharge	67.5	67.5	67.5	to CETP

- o Reduction in 8 CMD process effluent is due to reduction of TMHQ production from 20 MTPM to 13 MTPM.
- o 10 CMD washing effluent reduction is due plant washing optimization (Some reactors dedicated for making DEP only, thus avoiding their washings)
- o Thus, overall effluent generation will be reduced from existing 108 CMD to 102 CMD.

Query No. 4: The coal consumption and steam requirements will be increased.

PP Reply:

- Increased steam requirement is due to new products (ACN and Diethyl Ketone)
- The existing boilers are sufficient to cater the additional steam requirement and coal consumption will be 33 MTPD (within consented limit).
- Coal consumption in existing TFH (4kcal/hr) is 2.8 MTPD.
- Coal consumption in proposed TFH (7kcal/hr) will be 5 MTPD
- The total coal consumption after proposal is 41 MTPD which is within EC sanctioned limit 43 MTPD (Sr No. 32 (1) of EC No. SEIAA-EC-0000002254 dt 24-04-2020).

Sr.no.	Type of Fuel	As per Existing (CTO)	Proposed Additional	Total Reqd	Remark
1	Imported coal (10% Ash + 0.5% S)/ Briquettes	Boilers-33 TPD TFH-2.8 TPD	New TFH-5TPD	40.8 TPD	EC granted for 43 MTPD coal consumption

- In addition, PP is discontinuing use of FO at site –thus there will be net reduction in air pollution load of SO₂ by 108 kg/d

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Thus, there is net reduction in air pollution load due to fuel burning as against the EC sanctioned limits.

Query No. 5: PP was unable to submit the details of process emissions from existing products and details of comparison of the pollution load.

iii) Process Emissions:

SR NO	AS PER EC	STACK NO	New stack proposed	APC System Provided
1	Process reactor	1 No. (57)	Proposed vent (acetonitrile plant)	Two stage water scrubbers followed by bubbling through Water Tank

- a. Ammonia gas from acetonitrile plant is fed to ammonia scrubber D-206. Scrubber vent gases are taken to secondary scrubber D 206 to absorb residual ammonia. The secondary scrubber vent is bubbled through water tank to ensure complete removal of any traces of ammonia.
- b. Scrubber bottom liquid is liquor ammonia which is fed to ammonia stripper D-207.
- c. The ammonia stripper D-207 overhead is recovered ammonia which is passed through entrainment separator SEP-202 and recycled back to acetonitrile reactor- thus the ammonia remains in primarily closed loop.
- d. Stripper bottom is lean water which is again recycled back to ammonia scrubber after passing through coolers C-207B to again scrub ammonia from the process.
- e. The emission from water tank will only have traces of organics and air.

EC already has approved one process vent – and currently PP does not have any Process vent in existing plants - thus there will be no additional vent than what is permitted in EC.

Technical Committee Deliberations:

The proposed project is resubmission case. It was discussed based on compliances submitted against earlier MOM of first sitting of Technical Committee of product mix dtd. 18.08.2022, NIPL Certificate and presentation made by the industry. Product wise load calculation in terms of wastewater, Air emissions & Hazardous waste generation were discussed. Existing consent to operate, Environmental Clearance, NIPL Certificate issued by Aditya Environmental Services Pvt. Ltd., and product –mix Proforma are taken on the record.

After due deliberations, Committee noticed that:

1. PP unable to produce adequacy of Ammonia stripper used for recovery of Ammonia.

Technical Committee Decision:

Technical Committee decided to **refuse** the case due to concern about Ammonia emission from the process.



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Agenda Item No.	2
Proposal No.	MPCB-CONSENT-0000142930
Project Details	M/s. Hikal Ltd.(T-21, MIDC Ind. Area, Taloja, Dist.-Raigad, Maharashtra)
NIPL Certificate	NIPL Certificate issued By Goldfinch Engineering Systems Private Limited dtd. 04/06/2022
Name of the Industry Representative present	1. Ravinder Harkare, Head 2. N. Dharmadhikari, Technical Team

Introduction:

This has reference to the online proposal submitted vide No. MPCB-CONSENT-0000142930 along with the copies of documents seeking amendment in existing consent to operate under change in product-mix under the provisions of EIA Notification 2006 amended on 23/11/2016 & amended on 02/3/2021. Industry has obtained Consent to Operate on 10/11/2021 & requested for amendment in consent to operate under change in product mix.

Existing Clearances:

- Environment Clearance obtained with vide no. F.No.J-11011/63/2007-IA II(I) dated 28/08/2007.
- Consent to operate for proposed change in product mix vide No. Format 1.0/BO/CAC-Cell/UAN No. 0000036593/5th CAC-0224 dtd.13/03/2019.
- Consent to Operate obtained with vide no. Format 1.0/CAC/UAN no. MPCB-CONSENT-0000113461/CR-2111000349 dtd.10/11/2021.
- Industry has submitted proposal on PARIVESH portal on 28.07.2022. Single Window No (SW/2127/2022).

The Industry has given the presentation regarding NIPL proposal before the committee and gist of the presentation is as follows:

Project Details:

A. Production Details:

Sr. no.	Name of Product	EC Quantity Granted	Existing Consent quantity after product mix (MT/A)	Proposed quantity after change in product mix (MT/A)
1	Thiabendazole(TBZ)	700	490	550
2	Bifenazate	100	0	0
3	ADMP	200	0	0
4	Fenamidone(HTP-213)	300	100	150
5	IDPO	300	0	0
6	Intermediate of HTP-293	200	0	0
7	Isofetamide(IKF)	-	60	40

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Sr. no.	Name of Product	EC Quantity Granted	Existing Consent quantity after product mix (MT/A)	Proposed quantity after change in product mix (MT/A)
	OR MPDC-DME	-	60	100
	OR MPDC	-	0	100
8	Ametoctradibne(B.A,S.650/HTP-650)	-	750	700
9	MPDC-DME	-	400	650
10	MPDC	-	0	100
	OR Cyclaniliprole(IKI)	-	0	50
	OR Valifenalate	-	0	50
	OR Isofetamide(IKF)	-	0	20
11	Pyriprol, Azamethiphos &All developing molecule(R&D products)etc.	-	0	30
	Total	1800	1800	2280

By-Product

Sr. no	Name of By-product	UOM	As per CTO	Existing Qty.	After Change in Product Mix Qty.
1	By product HCl	MT/A	1462	1461.6	1245.7
2	By product NH ₃ Solution	MT/A	900	899.4	1009.5
3	By product H ₂ SO ₄	MT/A	904	903.8	1014.4
4	By Product Aluminum Chloride	MT/A	382	381.9	381.9
5	Recovered Solvents (Mono Chloro Acetone/ Toluene/ Methanol/ IPA/ DMF/ Mono Chloro Benzene/ Benzene)	MT/A	500	500	500
	Total	MT/A	4148	4146.7	4151.5




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B. Pollution load Details:

i) Water consumption & Wastewater Aspect

Before Product Mix

Sr. no.	Particulars	Quantity in CMD	Effluent generation in CMD		COD				TDS			
					Strong		Weak		Strong		Weak	
			Strong	Weak	Kg/Day	Mg/l	Kg/Day	Mg/l	Kg/Day	Mg/l	Kg/Day	Mg/l
1	Water Consumption	1162	Not Applicable									
2	Trade Effluent Generation											
A	Process & Washing Activity	673.8	--	--	--	--	--	--	--	--	--	--
B	Cooling Tower & Boiler	68	--	--	--	--	--	--	--	--	--	--
	Total	741.8	54.8	687	11332.5	206797	827.8	1205	21812.8	39804.4	991.6	1443
3	Domestic Effluent Generation, CMD	30	30		--	--	--	--	--	--	--	--

Effluent Generation: Domestic -30 CMD + Industrial -741.8 CMD

After Product Mix

Sr. no.	Particulars	Quantity in CMD	Effluent generation in CMD		COD				TDS			
					Strong		Weak		Strong		Weak	
			Strong	Weak	Kg/Day	Mg/l	Kg/Day	Mg/l	Kg/Day	Mg/l	Kg/Day	Mg/l
1	Water Consumption	1161.4	Not Applicable									
2	Trade Effluent Generation											
A	Process & Washing Activity	671.9	--	--	--	--	--	--	--	--	--	--
B	Cooling Tower & Boiler	68	--	--	--	--	--	--	--	--	--	--

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	Total	739.9	118	621.9	11393.7	96557	749.4	1205	18099 .6	15338 7	897.4	1443
3	Domestic Effluent Generation (CMD)	30	30	--	--	--	--	--	--	--	--	--

Effluent Generation: Domestic - 30 CMD + Industrial – 739.9 CMD i.e. Total- 769.9 CMD (EC permitted quantity- 823 CMD)

- Water Consumption will reduce by 0.2 CMD compared with earlier C to O
- Effluent generation will reduce by 1.9 CMD
- Average COD Load will reduce by 17.2 Kg/Day

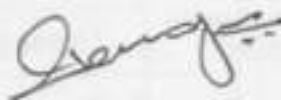
Treatment System

a) Trade Effluent:

- Effluent generating from process will be segregated in two streams high TDS & low TDS stream.
- High TDS stream from process is being treated in MEE.
- Condensate from evaporator along with low TDS stream from process will be fed to the secondary treatment. Primarily treated stream will be fed to secondary treatment followed by tertiary treatment. Tertiary treated waste water is sent to CETP for further disposal.

b) Domestic Effluent:

Domestic Sewage 30 CMD is treated separately in STP of design capacity 50 CMD based in MBBR technology.

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ii) Air Emission Load:

Flue Gas Emissions

Sr. No.	Stack Attached to	Fuel	Existing Fuel Consumption	Fuel Consumption after Change in Product Mix	Remark
1	Emergency D.G. Set (1500 KVA)	HSD	10 MT/M	10 MT/M	No Change
2	Steam Boiler [B-920A/B (standby)]	LSHS	943 MT/M	LSHS: 932 MT/M OR Natural Gas: 34596 SCM/Day	Switched over to cleaner fuel LSHS/LDO/NG in place of Furnace oil
3	Briquette Boiler (MR-1)	Briquette	3000 MT/M	Briquette: 2960 MT/M	No Change
4	Baby Boiler (MR-1))	Natural Gas	5 MT/M	Natural Gas: 5 MT/M or LSHS: 11 MT/M	No change

Process emissions control systems:

Sr. No.	Stack attached to	Stack height (m)	APCM
1	Ventilation Blower Plant-1 (BLW-201)	27	Stack with Adequate height
2	Acid Scrubber (C-502)	25	Water Scrubber & Stack with Adequate height
3	Vent Sorb Blower Plant-2 (BLW-501)	25	Stack with Adequate height
4	Ventilation Blower Plant (BLW-605)	13	Stack with Adequate height
5	Ventilation Blower MCA (BLW-101)	13	Stack with Adequate height
6	Emergency Chlorine Blower	17	Stack with Adequate height
7	Ammonia Scrubber (C-1203)	20	Scrubber Water & Stack with Adequate height
8	Bag Filter Blower (BLW-601)	22	Fabric Bag Filter & Stack with Adequate height
9	Bag Filter Blower (BLW-602)	22	Fabric Bag Filter & Stack with Adequate height
10	Bag Filter Blower (BLW-603)	22	Fabric Bag Filter & Stack with Adequate height
11	Scrubber For HTP-213	30	Scrubber Caustic & Stack with Adequate height

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Sr. No.	Stack attached to	Stack height (m)	APCM
12	General Common Scrubber HTP-213	30	Scrubber Caustic & Stack with Adequate height

Note: * Consumption of briquette in current CTO 1000 MT/M. However, in earlier consent (2013) consumption of briquette was 3000 MT/M. At the time of renewal application of the CTO which was valid up to 30.07.2017, by mistake it was mentioned as 1000 MT/M instead of 3000 MT/M although there was no change in production quantity & other CTO limits. The same was repeated while issuing the CTO which is valid up to 31.07.2024. PP requested to correct the briquette consumption as per earlier permission of 3000 MT/M.

As per the guidelines issued by MPCB dated 5th February 2020, unit is using LSHS in place of FO as fuel for boiler.

Process Emissions details:

Sr. No.	Parameters	Before change in product-mix	After change in product-mix	As per EC	Consented Limit
1	Acid Mist	BDL	BDL	No concentration mentioned in the Environmental Clearance.	20 mg/Nm ³
2	Chlorine	BDL	BDL		5 mg/Nm ³
3	Ammonia	0-10 mg/Nm ³	0-10 mg/Nm ³		30 mg/Nm ³
4	H ₂ S	N.D.	N.D.		5 mg/Nm ³
5	Benzene	<0.05 ppm	<0.05 ppm		Not Specified*
6	CS ₂	BDL	BDL		Not Specified*
7	HCl	BDL	BDL		Not Specified*
	Acetone	<0.12	<0.12		100 mg/Nm ³
9	Toluene	<0.19	<0.19		
10	Xylene	<0.22	<0.22		

Note: * In valid CTO these parameters are not mentioned. Now, included in the application of ACTPO under CIPM.

iii) Hazardous Waste Load

Sr. No	Type of Waste	Cat. No.	As Per CTO.	Existing Qty.	After Change in Product Mix Qty.	UOM	Disposal
1	Used Oil/ Spent Oil	5.1	9	9	9	MT/A	Sale to Authorized Party Re-Processor
2	Process Residue & waste	29.1	2112.65	2112.65	2092.6	MT/A	Sale to MPCB or CPCB Auth. Preprocessor/CHWTSDF
3	Sludge Containing residual Pesticides	29.2	30	29.8	33.4	MT/A	Sale to MPCB or CPCB Auth. Preprocessor/ CHWTSDF.

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Sr. No	Type of Waste	Cat. No.	As Per CTO.	Existing Qty.	After Change in Product Mix Qty.	UOM	Disposal
4	Spent Solvent	29.4	3713	3712.7	3865.2	MT/A	Sale to MPCB or CPCB Auth. Preprocessor/ CHWTSDF.
5	Empty Barrels/ Containers/ liner	33.1	1800 (Nos per year)	1800 (Nos per year)	1800 (Nos per year)	Nos./A	Sale to Autho. Party /Recycle /CHWTSDF
6	Chemical sludge from waste water treatment	35.3	30	30	30	MT/A	CHWTSDF
7	Filter Medium	36.2	100	100	100	MT/A	Sale to MPCB or CPCB Auth. Preprocess or/ CHWTSDF
8	Ash and Flue gas Cleaning residue	37.2	10	10	10	MT/A	CHWTSDF
9	Concentration or Evaporation Residue	37.3	9000	9000	9000	MT/A	CHWTSDF
10	Potassium Bromide	-	308	307.8	307.8	MT/A	Sale to Authorized Party / recycle/ CHWTSDF
11	Spent Caustic	-	520	520	520	MT/A	Sale to Authorized Party / recycle/ CHWTSDF
12	Sodium Hydro sulphide (NaSH)	-	150	149.6	224.3	MT/A	Sale to Authorized Party / CHWTSDF

Condition under Batteries (Management & Handling) Rule 2001

Sr. No	Type of Waste	Existing Qty.	After Change in Product Mix Qty.	Disposal Path
1	Used Batteries	30 Nos./Y	30 Nos./Y	Sale to Auth. Recycler/ Reprocess or

Condition under Plastic waste Management Rule 2016

1	Plastic Waste	50 KG/D	50 KG/D	Sale to Auth. Party/Recycler
2	Plastic Bottles	5 KG/D	5 KG/D	Sale to Auth. Party/Recycler

Treatment and disposal of Biomedical waste generated to CHWTSDF

1	Biomedical Waste	5 KG/M	5 KG/M	CBMWTSDf/CHWTSDF
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Non-Hazardous Waste

1	Boiler Ash	5400 MT/A	5400 MT/A	Sale to brick Manufacturer
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Sr. No	Type of Waste	Cat. No.	As Per CTO.	Existing Qty.	After Change in Product Mix Qty.	UOM	Disposal
2	Metal Scrap		50 MT/M	50 MT/M			Sale to Auth. Party.
3	Wood		5 MT/M	5 MT/M			Sale to Auth. Party scrap merchant
4	Glass Bottles		20 No/D	20 No/D			Sale to Auth. Party scrap merchant

Note: After change in product mix hazardous waste will be reduced by 20.4 MTA. There is no category & quantity of Hazardous waste mentioned in the Environmental Clearance.

Technical Committee Deliberations:

The proposed project was discussed based on submitted documents, NIPL Certificate and presentation made by the industry. Product wise load calculation in terms of wastewater, Air emissions & Hazardous waste generation were discussed. Existing consent to operate, Environmental Clearance, NIPL Certificate issued by Goldfinch Engineering Systems Pvt. Ltd and Product Mix Pro-forma are taken on the record.

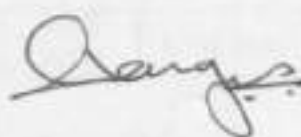
Committee after due deliberations noticed that;

- i. After product mix the total production capacity of the plant will be increased from 1800 MT/A to 2280 MT/A i.e., 480 MT/A.
- ii. There is no process emissions & Hazardous Waste category & quantity mentioned in the Environmental Clearance.
- iii. The water consumption, trade effluent generation & organic load will be slightly reduced as compared to existing consent to operate.
- iv. The overall Hazardous waste quantity after product mix will be reduced by 20.4 MTA.
- v. The overall pollution load will not increase after change in product mix.

Technical Committee Decision:

Technical Committee decided to recommend the case for change in product under Product Mix with a compliance of the following conditions:

- (i) Industry shall comply with all the conditions stipulated in Environmental Clearance and ensure display/upload of six-monthly compliance monitoring report on their official website.
- (ii) Industry shall not manufacture any other product for which permission is not granted by the MPCB.
- (iii) The by-products shown to be shifted to Hazardous Waste & disposed as per the provisions of H&OW Rule and classify as a by-product from committee constituted for classification of waste.
- (iv) Industry shall ensure connectivity of OCEMS data to Boards server and transmit the data continuously for wastewater treatment facility.
- (v) Considering the quantity of Hazardous waste and category is not mentioned in the Environmental Clearance, NIPL with respect to Hazardous Waste may be compared with this Consent to Establish henceforth if application is received from the industry.

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Agenda Item No	Item No. 3
Proposal No.	MPCB-CONSENT-0000142551
Project Details	Yashwantrao Mohite Krishna Sahakari Sakhar Karkhana Ltd.(A/p- Shivnagar), Karad.
NIPL Certificate	NIPL certificate issued by M/s. Enviro Analysts & Engineers Pvt. Ltd. Borivali, Mumbai.
Name of the Industry Representative present	Mr. Suryakant Dalvi (Managing Director) Mr. Khanvilkar – Environmental Officer.

Introduction:

This is an existing distillery unit having C-Molasses as raw material. This has reference to the online proposal submitted vide No. MPCB-CONSENT-0000142551 along with the copies of documents seeking amendment in existing consent to operate under change in product – mix under the provisions of EIA Notification, 2006 amended on 23/11/2016 & on 02/3/2021. Industry has applied for change in product mix by switching the raw material from C-molasses to B-Molasses or cane juice.

Exiting Clearances:

1. Environmental Clearance is obtained in the name of M/s. Krishna Sahakari Sakhar Karkhana Ltd., vide No. F. No. J-11011/3/2002-IA II (I) dated 19th June 2006.
2. Consent to Operate obtained vide No. Format1.0 / CAC/ UAN No. MPCB-CONSENT-0000119478 / CR-2112001471 dated 27.12.2021 valid upto 31/08/2022.

The industry has given the presentation regarding NIPL proposal before the committee and gist of the presentation is as follows:

A) Project details:

Particulars	Existing	After Product Mix	
		145 KLPD	145 KLPD
Capacity	95 KLPD	145 KLPD	145 KLPD
Raw Material	C Molasses	B- heavy Molasses	Syrup
Production	Rectified spirit: 95 KLPD Ethanol: 60 KLPD	Rectified spirit: 145 KLPD Ethanol: 145 KLPD	Rectified spirit: 145 KLPD Ethanol: 145 KLPD
Co products	Fusel Oil: 5.5 KLPD CO2 : 45 TPD	Fusel Oil: 20 KLPD CO2 :68 TPD	Fusel Oil: 20 KLPD CO2 :68 TPD

B) Pollution load Details:

i) Water Consumption & Wastewater Aspect

Sr. No.	Particulars	Existing (60 KLPD)			After Product Mix (90 KLPD)		
		C- Molasses			B- heavy Molasses / Syrup		
		Quantity in CMD	COD in mg/l	COD in kg/day	Quantity in CMD	COD in mg/l	COD in kg/day
1	Water Consumption in CMD	1305	NA	NA	1255	NA	NA
2	Industrial Effluent generation						
A	Spent Wash	920	130000	119600	876	110000	96360

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	In CMD						
B	Other in CMD	20	1500	30	20	1500	30
	Total	940		119630	896		96390

COD will reduce by 23240 kg/day after change in raw material.

Treatment System

i. Trade Effluent: 876 m³/day treated by bio methanation - MEE followed by bio composting.

ii. Domestic Effluent: 5 m³/day treated in ETP and reused for irrigation.

ii) Air Emission Load:

Flue Gas Emissions

Sr. No.	Stack Attached to	Fuel	Existing Fuel Consumption	Fuel Consumption after Change in Product Mix	Remark
1	Boiler, 90 TPH	Bagasse	Bagasse	960 TPD	No change, inhouse bagasse generated from sugar factory will be used as a fuel.
2	DG set with stack -500 kVA	Diesel	Diesel	100 lit/hr.	No change

Process Emissions

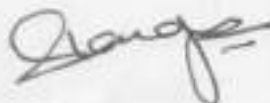
Sr. No.	Stack attached to	Stack height (m)	APCM
1	Steam taken from existing sugar unit	72	ESP (at sugar unit)
2	DG set with stack -500 kVA	3.5 above roof top	stack

iii) Hazardous Waste Load:

There is no generation of Hazardous Waste before and after product mix.

iv) Non-Hazardous Waste

Sr. No	Type of Waste	Existing Qty.	After Change in Product Mix Qty	Remarks
1	Yeast Sludge	30 TPD	30 TPD	no increase in solid waste generation

Technical Committee Deliberations:

The proposed project was discussed based on the submitted documents, NIPL Certificate and presentation made by the industry. Product wise load calculation in terms of wastewater, Air emissions & Hazardous waste generation were discussed. Existing consent to operate, Environmental Clearance, NIPL Certificate issued by Enviro Analysts and Engineers Pvt Ltd. and Product Mix Pro-forma are taken on the record.

After due deliberations

Technical Committee decided to **recommend** the case for change in product under product mix with a compliance of the following conditions;

1. PP shall submit undertaking stating that they will install CO₂ bottling plant within 6 months.
2. PP shall submit sugar production details after change in product mix.
3. Industry shall comply with all the conditions stipulated in Environmental Clearance and ensure display/upload of six-monthly compliance monitoring report on their official website.
4. Industry shall transmit OCEMS data directly to Board's server through the data logger.
5. Industry shall submit undertaking stating that, no new plant & machinery will be installed, and production activity will be carried out in existing plant & machinery only.
6. Industry should not manufacture any other product for which permission is not granted by the MPCB.



MAHARASHTRA POLLUTION CONTROL BOARD

Agenda item No	Item No. 4
Proposal No.	MPCB-CONSENT-0000143466
Project Details	M/s. Godrej Agrovet Limited MIDC, Lote Parshuram, Chiplun, Tal. Khed, Dist. Ratnagiri.
NIPL Certificate	NIPL certificate dated 23/06/2022 issued by M/s, Environmental Auditor: Institute of Chemical Technology (NBA Accredited, Grade 'A' by MHRD)
Name of the Industry Representative Present	Sh. Manohar Shinde, Factory Manager Sh. Sanjay Bhosale

Introduction:

This has reference to the online proposal submitted vide No. MPCB-CONSENT-0000143466 along with the copies of documents seeking consent to operate under change in product – mix under the provisions of EIA Notification, 2006 amended on 23/11/2016 & on 02/3/2021.

Existing Clearances:

1. Environmental Clearance granted vide No. vide No. F.NO.J11011/231/2003-IA-II(I), dated 09/03/2021.
2. Consent to Operate obtained vide No. Format1.0/AS(T)/UAN No.MPCB-CONSENT-0000113617/CR/2202001727, Date. 28/02/2022, valid upto 30/06/2022.

The industry has given the presentation regarding NIPL proposal before the committee and gist of the presentation is as follows:

Project details:.

A) Production Details:

Sr.no.	Name of the Product	Existing/ Consented (TPA)	Proposed after product mix change (TPA)
	Technical		
1	Homobrassinolide (Hbr)	1.5	1.5
2	God-Hh001 Pyriothioack Sodium Technical	60	100
3	Bispyribac Sodium Technical	60	60
4	Florchlorfenuron Technical	50	40
5	Quizalofap-P-Ethyl Technical	60	45
6	Dimethomorph Technical	60	60
7	Metribuzin Technical	60	40
8	Thiophanate Methyl Technical	60	60
9	Trifloxystrobin Technical	60	45
10	Mepiquat Chloride Technical	0	10
11	Hitweed Pyriothioack Sodium 10%	36	10
	Total	507.5	471.5

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Sr.no.	Name of the Product	Existing/ Consented (TPA)	Proposed after product mix
Formulation			
12	Repacking of Quizalofap-P-Ethyl	480	480
13	Dilute caustic lye 27% By Diluting to 48%	360	360
14	Bispyribac Sodium formulation	144.405	100
15	Florchlorfenuron Formulation	10.12	10.12
16	Achook/Nimin	36	36
17	Bumper/Bountee	12	12
18	Combined PGR Like Super shakti, Dimore Combine, Double	12	12
19	Dapcoat	24	0
20	Agroneem	200	190
21	Liquid Vipul, Vipul Granules, Suruchi, Ruchira	36	36
22	Neem oil Emulsifiable	24	0
23	Hitweed, Pyriithiobac sodium Formulation	0	100
Total		1338.525	1336.12
Grand Total		1846.025	1807.62

A. Pollution load Details:

i) Water consumption and Wastewater Aspect

Water Consumption Aspect

Sr.no.	Purpose	Quantity of existing water requirement (as per EC/CTO) (KLD)	Quantity of water requirement after the proposed change in product mix or raw material mix (KLD)
1	Process	4.42	3.23
2	Washing	3.00	3.00
3	Boiler Makeup	3.70	3.70
4	Cooling Tower Makeup	31.50	31.50
5	Scrubbing system	2.00	2.00
6	Green Belt	3.50	3.50
7	Domestic	4.00	4.00
Total		52.12	50.93

Wastewater Aspect

Sr.no.	Purpose	Quantity of existing effluent generation (as per EC/CTO) (KLD)	Quantity of effluent generation after the proposed change in product mix or raw material mix (KLD)	Mode of Disposal and Ultimate Receiving Body	Change Envisaged
1	Process	5.39	4.13	<p align="center">HTDS: HTDS effluent sent to MEE system followed by ETP.</p> <p align="center">LTDS: LTDS effluent treated in ETP – RO Plant. RO Rejects to MEE System and RO permeate to reuse, Condensate from MEE to reuse and MEE residue to ATFD.</p>	<p align="center">Project is already Zero Liquid Discharge Unit (ZLD) and shall continue to do so after change in product mix.</p>
2	Washing	3.00	3.00		
3	Boiler Makeup	0.70	0.70		
4	Cooling Tower Makeup	3.50	3.50		
5	Scrubbing	2.00	2.00		
6	Green Belt	0.00	0.00		
7	Domestic	3.50	3.50		
Total		18.09	16.83		

Treated Effluent disposal:
Treated effluent is segregated

i) Strong COD/TDS stream of 5.98 CMD - Treatment system comprising of Primary, Multi effect evaporator with design capacity of 15 CMD followed by ATFD. The MEE condensate is treated in weak stream ETP.

ii) Weak COD/TDS stream of 12.11 CMD - Treatment system comprising of Primary, Secondary (Activated sludge process), Tertiary, Reverse osmosis. Industry has achieved ZLD

Domestic Effluent:

The domestic effluent is combinedly treated in ETP.




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ii. Air Emission Load: -

Sr.no.	Point Source	Height of Stack (m)	Existing-Emission Rate in (Nm ³ /hr)	Operational Hours in a day	No. of Operational Days in a year	Existing-Total Emissions (Nm ³ /hr)	After the proposed change in product mix or raw material mix Emission Rate (Nm ³ /hr)	After the proposed change in product or raw material mix Total emission (Nm ³ /hr)
1	Boiler-1	18	1342.35	24	300	1342.35	1342.35	1342.35
2	Boiler-2	21	2285.92	24	300	2285.92	2285.92	2285.92
3	DG Set	3	1092.66	1	300	1092.66	1092.66	1092.66
4	Thermic	18	1168.08	24	300	1168.08	1168.08	1168.08
5	Process	10	1342.35	24	120	1342.35	1342.35	1342.35

Quality of Emissions from various Stacks

Sr.no.	Stack attached to	Stack height (m)	APCM	Parameters (e.g., PM ₁₀ / PM _{2.5} / SO ₂ / NO _x / Others)	Unit	Existing Emission Rate	After the proposed change in product or raw material mix Emission Rate
1	Boiler-1 (0.6 TPH)	18	Stack	SO ₂	Kg/day	10.56	10.56
2	Boiler-2 (0.6 TPH)	21	Stack	SO ₂	Kg/day	10.36	10.36
3	DG set (200 KVA)	3	Acoustic enclosure/	SO ₂	Kg/day	10.36	10.36
5	Thermic Fluid	18	Stack	TPM	mg/Nm ³	-	-
6	Process Reactor	10	Scrubber	Acid mist	mg/Nm ³	35	35

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Total Load of Process Emissions

Sr.no.	APCM	Operational	No. of	Total load	APCM	Total load in	Remarks
1	stack	24	300	0.54	Stack	0.54	PM Load
2	Stack	24	300	0.54	Stack	0.54	PM Load
3	Acoustic	1	120	0.058	Acoustic	0.058	PM Load
4	Stack	24	300	0.058	stack	0.058	PM load
5	Scrubber	18	300	0.36	Scrubber	0.36	Acid Mist

iii) Hazardous Waste Load

HAZARDOUS WASTE MANAGEMENT (PROCESS)						
Sr.no	Waste	Category (as per HWM Rules,2016)	(Existing)	(Total after product mix change)	Treatment	Disposal
			Quantity of generatio n (TPA)	Quantity of generation (TPA)		
1	Process waste or residues (Herbicides Residues and waste)	29.1	54	54	Incineration	CHWTSDF
2	Chemical sludge from waste water treatment	35.3	13.2	13.2	Incineration	CHWTSDF

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3	Empty barrels / containers/ liners contaminated with hazardous chemicals /wastes	33.1	5304	5304	Recycle	Sold to authorized party/CHWTSDf
4	Process Residue and waste (Process Organic Residue)	28.1	354.6	283.79	Incineration	CHWTSDf
5	Distillation Residue (Solvent Distillation Residue)	20.3	120.6	101.61	Incineration	CHWTSDf

S.No.	Waste	Category (as per HWM Rules,2016)	(Existing)	(Total after product mix change)	Treatment	Disposal
			Quantity of generation (TPA)	Quantity of generation (TPA)		
6	Process Residue and wastes (Silica)	28.1	86.4	67.81	Landfill	CHWTSDf
7	Concentration or evaporation residue (MEE Salts)	37.3	242.28	173.01	Incineration	CHWTSDf
8	Concentration or evaporation residue (Organic Distillate from MEE Stripper)	37.7	75.6	75.6	Incineration	CHWTSDf

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9	Used or spent oil	5.1	0.05	0.05	Recycle	Sold to authorised party/ CHWTSDF
10	Process Residue and waste (Chlorides Of CA & NA)	28.1	9	9	Incineration	CHWTSDF
	TOTAL		6257.7	6080.07		

Technical Committee Deliberations:

The proposed project was discussed based on documents – NIPL Certificate and presentation made by the industry. Product wise load calculation in terms of wastewater, Air emissions & Hazardous waste generation were discussed. Existing consent to operate, Environmental Clearance, NIPL Certificate issued by Institute of Chemical Technology and product –mix Proforma are taken on the record.

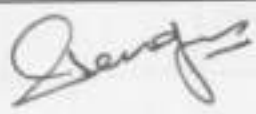
Committee after due deliberations noticed that;

- It was noted that the quantification of pollution was done considering,
 - Decreasing production capacity of the 07 nos of existing products.
 - Increasing production capacity of the 01 nos of existing products.
 - Deletion of 02 nos of existing products.
 - Addition of 02 new products.
 - Keeping the same production capacity of 11 nos of existing product.
- Thereby the total production capacity of Technical grade Products will decrease from 507.5 TPA to 471.5 TPA & Formulation products will decrease from 1338.525 TPA to 1336.12 TPA i.e., combined decrease in total production capacity from 1846.025 TPA to 1807.62 TPA.
- It was noted that the overall water consumption will reduce from 52.12 CMD to 50.93 CMD thereby reduction in wastewater generation from 18.09 CMD to 16.83 CMD.
- The committee also noted that there is no change in Hazardous waste and Air pollution aspects due to change in product under product mix.

Technical Committee Decision:

After due deliberations, Technical Committee has decided to **recommend** case for change in product under product mix with compliance of the following conditions:

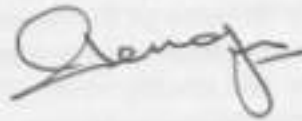
- Industry shall comply with all the conditions stipulated in Environmental Clearance and ensure display/upload of six-monthly compliance monitoring report on their official website.
- Industry shall submit the undertaking stating that, no plant & machinery will be installed, and production activity will be carried out in existing plant & machinery only.
- Industry should not manufacture any other product for which permission is not granted by the MPCB.

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Agenda item No	Item No. 5
Proposal No.	MPCB-CONSENT-0000143371
Project Details	M/s. Sahkar Maharshi Shankarrao Kolhe Sahkar Karkhana Ltd., Sahajanand Nagar, Kopargaon, Ahmednagar.
NIPL Certificate	NIPL Certificate issued by M/s. Goldfinch Engineering Systems Pvt. Ltd., dtd. 14.03.2022.

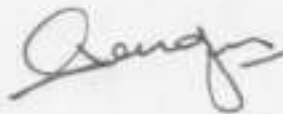
PP has submitted leave of absence letter for the meeting. Therefore, the committee has decided to defer the case and resubmit in the ensuing meeting.



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Agenda item No	Item No. 6
Proposal No.	MPCB-CONSENT-0000143371
Project Details	M/s. Bharat Petroleum Corporation Limited Refinery, Mahul, Chembur, Mumbai
NIPL Certificate	NIPL Certificate issued by Ultratech Environmental Consultancy & Laboratory dtd. 03/09/2022
Name of the Industry Representative present	BPCL Manager

1. As per the EIA notification published by MOEFCC, Delhi no. S.O. 980(E) dtd. 2nd March 2021 Appendix XIII 1.-"The project proponent is required to obtain a certificate of „no increase in the pollution load" from the environmental auditors or reputed institutions, to be empanelled by the State Pollution Control Board or Central Pollution Control Board or Ministry of Environment, Forest and Climate Change."
2. PP has NIPL certificate of "no increase in the pollution load" from the environmental auditor who is not accredited for the said specific sector (Petroleum).
3. Therefore, the case is **rejected** by the committee.



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Agenda Item No	Item No. 7
Proposal No.	MPCB-CONSENT-0000154116
Project Details	M/s. Alkyl Amines Chemicals Limited, Kurkumbh Industrial Area, Pune.
NIPL Certificate	NIPL Certificate issued by M/s. Goldfinch Engineering Systems Pvt. Ltd., dtd. 26.08.2022.
Name of the Industry Representative present	Sh. D.S. Jadhav, Manager(EHS)

Introduction:

This has reference to the online proposal submitted vide No. MPCB-CONSENT-0000147333 along with the copies of documents seeking amendment in existing consent to operate under change in product mix under the provision of EIA Notification 2006 amended on 02.03.2021.

Exiting Clearances:

1. Environmental Clearance is granted to the industry vide SEIAA-EC-0000002296 dated 08.07.2020. The unit has valid consent to operate vide No. Format 1.0/CAC/UAN No.0000118121/CO/-2202000168 dated 02.02.2022.
2. Industry has submitted proposal on PARIVESH portal on 03.10.2022. Single Window No (SW/2235/2022).

The Industry has given the presentation regarding NIPL proposal before the committee and gist of the presentation is as follows:

Project details:

A) Products with change in product mix as below:

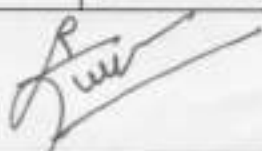
Sr. No	Name of Product	Production quantity as per EC, MT/A	Existing Production Quantity, MT/A	Proposed Production Quantity, MT/A after product mix
A to E Aliphatic Amines, Aliphatic Mixed Amines, Aromatic Amines, Aromatic Mixed Amines, Others Mixed Amines				
A	Aliphatic Amines			
1	Monomethyl Amine (MMA)	10	10	10
2	Dimethyl Amine(DMA)	10	10	10
3	Trimethyl Amine(TMA)	10	10	10
4	Monoethyl Amine (MEA)	1340	1340	1340

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Sr. No	Name of Product	Production quantity as per EC, MT/A	Existing Production Quantity, MT/A	Proposed Production Quantity, MT/A after product mix
5	Diethyl Amine (DEA)	2300	2300	2300
6	Triethyl Amine (TEA)	13880	13880	13880
7	Monoisopropyl Amine (MIPA)	10	10	10
8	Diisopropyl Amine (DIPA)	5	5	5
9	N – Propylamine (NPA)	5	5	5
10	Di – N – PROPYL AMINE (DNPA)	5	5	5
11	Tri-N- Propyl Amine (TNPA)	5	5	5
12	Mono – N – Butylamine (MNBA)	5	5	5
13	Di-N-Butylamine(DNBA)	5	5	5
14	2-Etylhexaylamine (2-EHA)	10	10	10
15	Bis-2-Ethylhexylamine(BIS-2-EHA)	50	50	50
16	Mono-Cyclohexylamine(MCHA)	5	5	5
17	Di-Cyclohexylamine(DCHA)	5	5	5
18	Morpholine	500	0	500
19	Piperazine (PIPZ)	480	0	480
B	Aliphatic Mixed Amines			
20	Diisopropylethyl Amine (Hunig's Base)(DIPEA)	1650	1650	1650
21	Dimethyl Isopropyl Amine(DMIPA)	20	20	20
22	Ethylmethyl Amine(EMA)	5	15	5
23	Diethylmethyl Amine(DEMA)	0	5	0
24	Dimethylcyclohexyl Amine(DMCHA)	10	10	10
25	N-ethylcyclohexyl Amine(NECHA)	5	5	5
26	N-Methylisopropyl Amine(NMIPA)	5	5	5
27	Diisopropylmethyl Amine(DIPMA)	10	10	10
28	Dimethylbutylamine(DMBA)	10	10	10
29	Dimethylethylamine(DMEA)	10	10	10
30	Ethylpropyl Amine(EPA)	5	5	5
31	N,N Dimethylpropyl Amine (DMPA)	5	20	5
32	N-Methyl Morpholine (NMM)	10	10	10
33	N-ethyl Piperazine (NEPIPZ)	200	0	200
34	N-Methyl Piperazine (NMPIPZ)	300	0	300
35	Dimethyl Piperazine (DMPIPZ)	120	0	120
36	Mixed Amines	1838	0	183
C	Aromatic Amines			
37	N,N Dimethylbenzyl Amine(BDMA)	10	10	10
38	1-Methyl-3 Phenyl Propyl Amine(MPPA)	5	5	5

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Sr. No	Name of Product	Production quantity as per EC, MT/A	Existing Production Quantity, MT/A	Proposed Production Quantity, MT/A after product mix
39	Furfurylamine(FFA)	150	150	150
40	Benzylamine(MBA)	10	10	10
41	Dibenzyl Amine(DBA)	10	10	10
42	N-Ethyl Benzyl Amine (NEBA)	5	5	5
43	4-Methyl-N,N-Dimethylbenzyl Amine (4MBDMA)	5	5	5
44	Beta – Phenylethylamine(PHEA)	10	10	10
45	Alpha-Phenylethylamine(APEA)	5	5	5
46	N-Isopropyl Benzene Amine(NIPBA)	5	5	5
47	1-(Inaphthyl) Ethylamine(ANEA)	5	5	5
48	3,5 Dichloroaniline(3,5 DCA)	10	10	10
49	Para Cumidine(PCD)	5	5	5
D	Aromatic Mixed Amines			
50	Thiophene – 2 Ethyl Amine(THEA)	5	5	5
51	2-Cyclohexylethyl Amine(CHEA)	10	10	10
52	Piperidine(PIP)	1650	1850	1650
53	Trans-4-Methylcyclohexyl Amine(4MCHA)	10	10	10
54	N-Methylbenzyl Amine(NMBA)	60	60	60
55	N-Benzylethanol Amine(NBEA)	10	10	10
E	Other Mixed Amines			
56	Methoxypropylamine(MOPA)	20	20	20
57	Dimethylaminopropyl Amine(DMAPA)	5500	5000	5500
58	Methylaminopropyl Amine(MAPA)	50	100	50
59	N-Methyl Imino Bis Propyl Amine(MIBPA)	30	30	30
60	Tetramethylenediamine(TMEDA)	30	100	30
61	Tetramethyl Amino Bis Propyl Amine(TMBPA)	10	10	10
62	Ethoxy Propyl Amine(ETHOPA)	30	100	30
63	Ethoxyethyl Amine(EEA)	5	5	5
64	Diethylaminopropylamine(DEAPA)	5	5	5
65	Ethylaminoethyl Amine(EAEA/NEEDA)	5	5	5
66	Dimethylamino Ethyl Amine(DMAEA/DMEDA)	5	5	5
67	1,3 Propylene Diamine(1,3-DAP)	5	5	5
68	3- Aminopropanol(3-AP)	20	100	20
69	Hydroxynovaldamine/N Bis(2hydroxyethyl) F-Phenylendiamine. Sulphatephenylenediaminesulphate (HND/HEPD SULPHATE)	5	5	5




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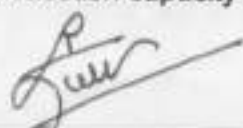
Sr. No	Name of Product	Production quantity as per EC, MT/A	Existing Production Quantity, MT/A	Proposed Production Quantity, MT/A after product mix
70	N,N Bis (2 Amminopropyl) Ethylenediamine (N-4 AMINE)	5	5	5
71	3-Methylamino-1-Phenyl-1-Propanol(MAPP)	5	5	5
72	Diethyl Hydroxylamine(DEHA)	3500	1750	3500
73	Dibenzyl Hydroxylaine(DBHA)	5	5	5
74	Isopropyl Hydroxylamine(IPHA)100%(sold as 15% soln)	50	50	50
75	N-Ethyl 1,2 – Dimethyl Propylamine (EDMPA)	10	10	10
76	1,2 Dimethylpropylamine(1,2 DMPA)	5	5	5
77	Tris-2- (Ethyl Hexyl) Amine(TRIS-2-EHA)	100	100	100
78	3-(2-ethylhexoxy) Propylamine(EHOPA)	50	50	50
79	Iminobispropylamine(IBPA)	5	5	5
80	F-Betaines	0	1250	0
G	Aliphatic amine hydrochloride			
81	Dimethylamine Hydrochloride(DMA HCL)	27500	27500	27500
82	Dimethylaminopropylchloride Hydrochloride(DMAPC.HCL)	0	5	0
83	Diethylamine Hydrochloride(DEA HCL)	150	150	150
84	Monomethylamine Hydrochloride(MMA HCL)	5	5	5
85	2-Chloroethylamine Hydrochloride(CEA HCL)	5	5	5
86	Triethylamine Hydrochloride(TEA HCL)	1500	1500	1500
87	Trimethylamine Hydrochloride(TMA HCL)	50	50	50
88	H-Aliphatic Amine Hydrochloride Solution	5000	15000	5000
I	Amide			
89	Diethyltoluamide (DEET)	100	380	100
90	Diethylphenyl Acetamide(DEPA)(sold as solution in IPA)	120	120	120
91	J-Pearlising Agent	100	500	100
92	K-Hydrogen	874.2	600	874.2
93	L- Retesting, Repacking, Relabeling of Primene 81 R & Amines (Contract Manufacturing)	625	100	625
M	Specialty Intermediates			
94	4-Methylcyclohexanone(4 MCHN)	5	5	5
95	3- Methoxypropanol(3 MOPL)	5	5	5
96	Dimethyl Propylene Urea (DMPU)	40	40	40
97	1,8 – Diazabicyclo (5.4.0) Undec – 7 Ene(DBU)	400	200	400
98	Ethyl Piperazinedione(EDP)	5	5	5



MAHARASHTRA POLLUTION CONTROL BOARD

Sr. No	Name of Product	Production quantity as per EC, MT/A	Existing Production Quantity, MT/A	Proposed Production Quantity, MT/A after product mix
99	B – Dimethylaminopropionitrile(DMAPN)	100	100	100
100	N- Sodium Acetate Solution	5400	5400	5400
101	Acetonitrile(AN)	11300	13000	11300
102	N,N – Dimethyl Imidazolidone(DMI)	5	5	5
103	1,5- Diazobicyclo (4,3,0) non-5-Ene (DBN)	5	5	5
104	2- Methyl Tetrahydrofuran (2-MTHF)	20	100	20
105	Phenyl Ethyl Alcohol(PHEA)	20	80	20
106	2- Methyl Resorcinol(3 MR)	5	5	5
107	2 Methylcyclohexylacetate (2 MCA)	20	100	20
108	Diethylsulphate (DES)	500	500	500
109	Calcium Sulphate	323.5	0	323.5
110	Hindered Amines Light Stabiliser (HALS) Typical- Bis(2,2,6,6 Tetramethyl-4-Piperidyl) Sebacate	200	200	200
111	N-Methylmorpholineoxide (NMMO)	200	200	200
112	2,2,6,6-Tetramethylpiperine 1-Oxyl (TEMPO)	10	100	10
113	4-Hydroxy-2,2,6,6-Tetramethylpiperine 1-Oxyl (HYDROXY TEMPO)	200	200	200
114	Mixed Amines(MIXAMIN)	250	250	250
115	Tri Acetone Amine	250	250	250
116	Diacetonealcohol (DAAL)	10	10	10
117	Mesityl Oxide (MEO)	10	10	10
118	2,2,6,6-Tetramethyl 2,3- Dihydropyridine (TMDP)	20	20	20
119	Diethyl ketone	3000	1200	3000
120	Carbon dioxide (CO2)	1238	0	1238
121	Dimethylformamide (DMF)	859	0	5000
Other Products				
122	Diethyltoluamide DEET Aqueous Solution	33.2	90	33.2
123	Sodium Sulphate	2200	2200	2200
124	Sodium carbonate Solution	859	1352	859
125	Dilute Sulphuric Acid	2156	2156	2156
	Total	---	104043	102441.9
125	Captive Co-generation Power (MW)		1.5	1.5

- The total production capacity as per existing CTO before shifting of products mentioned under other products to Hazardous waste was 110180 MT/A. However, after shifting some of the products mentioned under other products which are 6137 MT/A into the hazardous waste, total production capacity becomes 104043 MT/A.




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- For change in product mix the production quantity will get reduced from 104043 MT/A to 102441.9 MT/A i.e. 1601.1 MT/A is reduction in production capacity due to shifting of some of the products mentioned under other products.
- Hence, while issuing amendment in CTO under product mix proposed products and their quantities will be considered i.e. totalling to 102441.9 MT/A.

B) Pollution load Details:

i) Water consumption & Wastewater Aspect

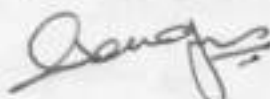
Before Product Mix

Sr. No.	Particulars	Quantity in CMD	Effluent generation in CMD		COD				TDS			
					Strong		Weak		Strong		Weak	
			Strong	Weak	Mg/l	Kg/Day	Mg/l	Kg/Day	Mg/l	Kg/Day	Mg/l	Kg/Day
1	Water Consumption	2091			Not Applicable							
2	Trade Effluent Generation											
A	Process & Washing Activity	187.3	--	--	--	--	--	--	--	--	--	--
B	Cooling Tower & Boiler	274	--	--	--	--	--	--	--	--	--	--
	Total	461.3	187.3	274	1998	374.2	200	54.8	1573	294.6	1200	328.8
3	Domestic	48	48		--	--	--	--	--	--	--	--

Domestic -48 CMD + Industrial - 461.3 CMD

After Product Mix

Sr. No.	Particulars	Quantity in CMD	Effluent generation in CMD		COD				TDS			
					Strong		Weak		Strong		Weak	
			Strong	Weak	Mg/l	Kg/Day	Mg/l	Kg/Day	Mg/l	Kg/Day	Mg/l	Kg/Day
1	Water Consumption	2091			Not Applicable							
2	Trade Effluent Generation											
A	Process & Washing Activity	186.5	--	--	--	--	--	--	--	--	--	--

MAHARASHTRA POLLUTION CONTROL BOARD

B	Cooling Tower & Boiler	274	--	--	--	--	--	--	--	--	--	
	Total	460.5	186.5	274	1963	366.1	200	54.8	1092	203.7	1200	328.8
3	Domestic Effluent Generation, CMD	48	48	--	--	--	--	--	--	--	--	

Domestic -48 CMD + Industrial – 460.5 CMD

- Water Consumption will reduce by 0.1 CMD
- Effluent generation will reduce by 0.8 CMD
- Average COD Load will reduce by 8.1 Kg/Day

Treatment System

i) Trade Effluent:

- The generated waste water is being treated in full-fledged ETPs (2 nos) of design capacity of 100 CMD each consisting of primary, Anoxic treatment followed by secondary treatment.
- Out of 462 CMD industrial effluent, 188 CMD from process is treated in ETPs (2 no.)
- Remaining 274 CMD effluent generating from boiler & cooling tower blow downs is being treated in tertiary treatment along with secondary treated effluent from process.
- After tertiary treatment 208.5 CMD is discharged to CETP as per the MPCB norms and remaining (253.5 CMD) is passed through RO having capacity 280 CMD. RO permeate (253.5 CMD) is being recycled in utilities.
- RO reject (12.6 CMD) is fed to MEE having capacity 20 CMD followed by centrifuge.
- MEE condensate (along with live steam 2.53 CMD) is being further recycled back to utilities and MEE salts are dispose to CHWTSDF.
- This existing effluent treatment facility is adequate even after proposed change in product mix.

ii) Domestic Effluent:

- Sewage Domestic sewage 48 CMD is being treated separately in STP having capacity 50 CMD. Treated domestic sewage after meeting the norms mentioned in the consent is being used for gardening.

ii) Air Emission Load:

Sr. No.	Stack Attached to	Fuel	Existing Fuel Consumption	Fuel Consumption after Change in Product Mix	Remark
1	Boiler-1	Imported Coal	7.50 MT/Hr	7.50 MT/Hr	No Change
		OR Indian Coal	10.21 MT/Hr	10.21 MT/Hr	

SP

Sanjay

MAHARASHTRA POLLUTION CONTROL BOARD

2	Boiler-2	OR Bagasse	16.7 MT/Hr	16.7 MT/Hr	No Change
		Imported Coal	4.85 MT/Hr	4.85 MT/Hr	
		OR Indian Coal	6.56 MT/Hr	6.56 MT/Hr	
		OR Bagasse	5.0 MT/Hr	5.0 MT/Hr	
3	Boiler-3	Imported Coal	2.65 MT/Hr	2.65 MT/Hr	No Change
		OR Indian Coal	3.65 MT/Hr	3.65 MT/Hr	
		OR Bagasse	5.0 MT/Hr	5.0 MT/Hr	
4	Acetonitrile TFH- (15 Lac Kcal/Hr)	Furnace Oil*	LDO-125 Kg/Hr	LDO-125 Kg/Hr Or LSHS-125 Kg/Hr Or NG- 100 Kg/Hr	Switched over to cleaner fuel LSHS/LDO/NG in place of Furnace oil
5	Derivative TFH- (10 Lac Kcal/Hr)	Furnace Oil*	LDO-70 Kg/Hr	LDO-70 Kg/Hr Or LSHS-70 kg/Hr Or NG-55 Kg/Hr	Switched over to cleaner fuel LSHS/LDO/NG in place of Furnace oil
6	H2 Plant TFH-5 Lac Kcal/Hr	Methanol/Hydrogen	55 Kg/Hr	55 Kg/Hr	No Change
7	DG Set (1000 KVA) Boiler	HSD	210 Lit/Hr	210 Lit/Hr	No Change
8	DG Set (1000 KVA)-Derivative	HSD	243 Lit/Hr	243 Lit/Hr	No Change
9	DG Set (320 KVA)-Derivative	HSD	60 Lit/Hr	60 Lit/Hr	No Change
10	Incinerator	HSD	20 Kg/Hr	20 Kg/Hr	No Change

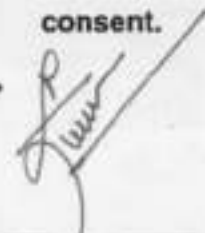
Note: * Switched over to cleaner fuel LSHS/LDO/NG in place of Furnace oil

Process Emission Parameters

Sr. No	Parameters	Before change in product-mix	After change in product-mix
1.	HCl	< 35 mg/Nm ³ Actual as per Analysis report is in between 2 to 4 mg/Nm ³	< 35 mg/Nm ³
2.	NH ₃ *	< 50 ppm Actual as per Analysis report is in between 5 to 8 mg/Nm ³	< 50 ppm

Note:

- NH₃ is a parameter generating from existing Products but missed in current CTO, now incorporated in Amended CTO.
- In earlier CTO dated 11.01.2019 it was mentioned, hence limit was taken from the said consent.




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iii) Hazardous Waste Load

Sr. No	Type of Waste	Cat. No.	As Per CTO.	Existing Qty.	After Change in Product Mix Qty.	UOM	Disposal
1	Spent ion exchange resin containing toxic metals	35.2	0.5	0.5	0.5	MT/M	CHWTSDf
2	Distillation Residue	20.3	90.5	90.44	90.42	MT/M	Co-Processing/ Pre-processing/Sale to authorized party/CHWTSDf
3	Used or Spent Oil	5.1	1.34	1.34	1.34	MT/M	Sale to Authorised Party/CHWTSDf
4	Spent Solvents	28.6	30.44	30.43	30.19	MT/M	Sale to Authorised Party/CHWTSDf
5	Empty Barrels/Containers/Liners contaminated with hazardous Chemicals/Wastes	33.1	500	500	500	No/M	Sale to Authorised Party/CHWTSDf
6	Concentration or Evaporation Residue	37.3	1.67	1.67	1.67	MT/M	CHWTSDf
7	Spent Catalyst	28.2	0.42	0.42	0.42	MT/M	Sale to Authorised Party/CHWTSDf
8	Chemical sludge from Waste water Treatment	35.3	28	28	28	MT/M	Co-Processing/Pre-processing /CHWTSDf
9	Wastes or Residues Containing oil	5.2	0.17	0.17	0.17	MT/M	CHWTSDf
10	Contaminated aromatic, aliphatic or naphthenic solvents may or may not be fit for reuse.	20.1	4.04	4.04	4.04	MT/M	Sale to Authorised Party/CHWTSDf
11	Spent Carbon	28.3	0.25	0.25	0.25	MT/M	CHWTSDf




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12	Ash from Incinerator and flue gas cleaning residue	37.2	0.17	0.17	0.17	MT/M	CHWTSDF
13	Process Residue (Dilute Caustic Lye)	28.1	5000	5000	3883.0	MT/A	Sale to Authorised Party/CHWTSDF
14	Spent Catalyst (Metal Catalyst)	28.1	33	33	33	MT/A	Sale to Authorised Party/CHWTSDF
15	Dilute Ammonia Solution	28.1	716	716	716	MT/A	Sale to Authorised Party/CHWTSDF
16	Process Residue (Calcium Carbonate)	28.1	388	388	12.1	MT/A	Sale to Authorised Party/CHWTSDF

Note:

- The revised list of hazardous waste after transferring some of the products mentioned under other products are incorporated from serial no. 13 to 16 under hazardous waste due to its disposal path.

E – Waste & Biomedical Waste

Sr. No	Type of Waste		Existing Qty.	After Change in Product Mix Qty.	Disposal Path
1	E - Waste		0.75 MT/M	0.75 MT/M	Return to Manufacturer through authorized dealer on buy back procurement/ Disposal through authorized party
1	Yellow	Solid Waste	8.33 KG/M	8.33 KG/M	CBMWTSDF
2	White (Translucent)	Waste Sharps Including Metals	0.13 KG/M	0.13 KG/M	CBMWTSDF

Technical Committee Deliberations:

The proposed project was discussed based on submitted documents, NIPL Certificate and presentation made by the industry. Product wise load calculation in terms of wastewater, Air emissions & Hazardous waste generation were discussed. Existing consent to operate, Environmental Clearance, NIPL Certificate issued by Goldfinch Engineering Systems Pvt. Ltd and product mix Proforma are taken on the record.

Committee after due deliberations noticed that:

- The water consumption, trade effluent generation & organic load will be slightly reduced.
- The overall Hazardous waste quantity after product mix will not be increased.
- The overall pollution load is not increased after change in product mix.



MAHARASHTRA POLLUTION CONTROL BOARD

Technical Committee Decision:

Technical Committee decided to **recommend** the case for change in product under product mix with compliance of the following conditions:

1. Industry shall transfer other products mentioned in current C to O which are Dil. Caustic lye, Metal Catalyst, Dilute Ammonia solution, and Calcium Carbonate to hazardous waste and submit modification letter accordingly.
2. Industry shall comply with all the conditions stipulated in Environmental Clearance and ensure display/upload of six-monthly compliance monitoring report on their official website.
3. Industry should not manufacture any other product for which permission is not granted by the MPCB.
4. Industry shall ensure connectivity of OCEMS data to Boards server and transmit the data continuously for wastewater treatment facility.



MAHARASHTRA POLLUTION CONTROL BOARD

Proposal No. 8	MPCB-CONSENT-0000151260
Project Details	M/s. Padmabhushan Krantiveer Dr. Nagnathanna Naykwadi Hutatma Kisan Ahir Sahakari Sakhar Karkhana Ltd., Walva, Sangli.
NIPL Certificate	NIPL Certificate issued by M/s. Technogreen Environmental Solutions, Pune.
Name of the Industry Representative present	Sh. N.D. Patil, D.M. Sh. Suryavanshi, Env. Eng.

Introduction:

This has reference to the online proposal submitted vide No MPCB-CONSENT-0000151260 along with copies of the documents seeking amendment in existing consent to operate under change in product mix under the provision of EIA Notification 2006 amended on 02.03.2021.

Existing Clearances:

1. Environmental Clearance is granted to the industry vide F. No. Delhi F.No. J-11011/661/2007-IA-II (I) dated 17th September 2007.
2. The unit has valid consent to operate vide No.- Format1.0/CAC/UAN No. MPCB-CONSENT-0000140563/CR/221100354 dated 4th November 2022.

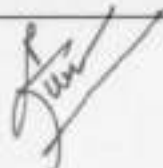
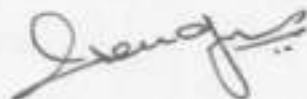
The industry has given the presentation regarding NIPL proposal before the committee and gist of the presentation is as follows:

Project details:

A) Production details

Industry is having existing 30 KLPD distillery utilizes C- heavy molasses as raw material to produce rectified spirit (RS), Extra Neutral Alcohol (ENA) and ethanol. Industry has proposed increase in ethanol production by 15 KLPD to use raw material viz. B-heavy molasses and syrup.

Particulars	Existing	After Product Mix	
Capacity	30 KLPD	45 KLPD	45 KLPD
Raw Material	C Molasses 120 MT/day	B- heavy Molasses 145 MT/day	Syrup 150 MT/day
Production	ENA: 30 KLPD Rectified spirit: 30 KLPD Ethanol: 30KLPD	ENA: 30 KLPD Rectified spirit: 45 KLPD Ethanol: 45 KLPD	ENA: 30 KLPD Rectified spirit: 45 KLPD Ethanol: 45 KLPD
Co products	Fusel Oil: 0.03 KLPD Biogas: 12480 m3/day Bio Compost: 7275.6 TPA CO2 : 22 TPD	Fusel Oil: 0.03 KLPD Biogas:9126 m3/day Bio Compost: 6220 TPA CO2 :34TPD	Fusel Oil: 0.03 KLPD Biogas: 2925 m3/day Bio Compost: 2592 TPA CO2 :34TPD

MAHARASHTRA POLLUTION CONTROL BOARD

B) Pollution load Details:

i) Water Consumption & Wastewater Aspect

Sr. no.	Particulars	Existing (60 KLPD)			After Product Mix (90 KLPD)			After Product Mix (90 KLPD)		
		C- Molasses			B- heavy Molasses			Syrup		
		Quantity in CMD	COD in mg/l	COD in kg/day	Quantity in CMD	COD in mg/l	COD in kg/day	Quantity in CMD	COD in mg/l	COD in kg/day
1	Water Consumption in CMD	555 (Fresh water 340+Recycle 215)	NA	NA	467 (Fresh water 248+ Recycle 219)	NA	NA	440 (Fresh water 282 + Recycle 158)	NA	NA
2	Industrial Effluent generation									
A	Spent Wash In CMD	240	150000	36000	203	130000	26390	100	90000	9000
B	Other in CMD	60	1500	90	88	1500	132	88	1500	132
	Total	300		36090	291		26522	188		9132

COD will reduce by 9568 kg/day using B- heavy Molasses and 26958 kg/day by using syrup.

Treatment System

1. Trade Effluent:

Spent wash directly treated through Bio-methanation followed by multi-effect evaporator and Bio composting. Condensate from MEE treated in CPU.

2. Other effluent: Industry has provided Effluent Treatment Plant and treated effluent is recycled in the process.

ii) Air Emission Load:

Flue Gas Emissions

Sr. No.	Stack Attached to	Fuel	Existing Fuel Consumption	Fuel Consumption after Change in Product Mix	Remark
1	Boiler 28 TPH x2 (sugar Industry)	Bagasse	610 MT/day	610 MT/day	No Change
2	Boiler 50 TPH (Sugar Industry)	Bagasse	480 MT/day	480 MT/day	No Change

MAHARASHTRA POLLUTION CONTROL BOARD

iii) Hazardous Waste Load:

No hazardous waste generation

Solid waste:

Sr. No.	Particulars	Existing	After Product Mix	Remark
1	Yeast Sludge	3 MT/day	3 MT/day	No change

Technical Committee Deliberations:

The proposed project was discussed based on documents – NIPL Certificate and presentation made by the industry. Product wise load calculation in terms of wastewater, Air emissions & Hazardous waste generation were discussed. Existing consent to operate, Environmental Clearance, NIPL Certificate issued by Techno green Environmental Solutions and product mix Pro-forma are taken on the record.

After due deliberations

Technical Committee decided to **recommend** the case for change in product under product mix with a compliance of the following conditions:

1. PP shall submit undertaking stating that they will install CO₂ bottling plant within 6 months.
2. PP shall submit sugar production details after change in product mix.
3. Industry shall comply with all the conditions stipulated in Environmental Clearance and ensure display/upload of six-monthly compliance monitoring report on their official website.
4. Industry shall transmit OCEMS data directly to Board's server through the data logger.
5. Industry shall submit undertaking stating that, no new plant & machinery will be installed, and production activity will be carried out in existing plant & machinery only.
6. Industry should not manufacture any other product for which permission is not granted by the MPCB.
7. PP shall submit undertaking for installment of CO₂ bottling plant within 6 months.



MAHARASHTRA POLLUTION CONTROL BOARD

Agenda item No	9
Proposal No.	MPCB-CONSENT-0000151399
Project Details	M/s. Excel Industries Ltd. Plot No. D-9, MIDC Lote Parshuram, Tal. Khed, Dist.- Ratnagiri Maharashtra.
NIPL Certificate	NIPL certificate issued by Goldfinch Engineering Systems Pvt. Ltd.
Name of the Industry Representative present	Sh. V.R. Vaidya, Sr. Manager Technical

Introduction:

This has reference to the online proposal submitted vide No. MPCB-CONSENT-0000151399 along with the copies of documents seeking amendment in existing consent to operate under change in product mix under the provision of EIA Notification 2006 amended on 02.03.2021.

Exiting Clearances:

1. Environmental Clearance is granted to the industry vide SEIAA-EC-0000001910 dated 31.07.2019. The unit has valid consent to operate vide No. Format 1.0/CAC/UAN No. 0000092328/CO-2008000965 dated 26.08.2020.
2. Consent to Establish obtained vide No. Format 1.0/CAC/UAN No. 0000113005/CE-2108001154 dated 20/8/2021.
3. Industry has submitted proposal on PARIVESH portal on 21.11.2022. Single Window No (SW/2292/2022).

The industry has given the presentation regarding NIPL proposal before the committee and gist of the presentation is as follows:

Project details:

A. Production details:

Sr. No.	EXISTING CONSENTED PRODUCT	Production as per Environmental Clearance MT/A	Production as per existing CTO, MT/A	Production after product mix, MT/A
1	Sodium Penta Chloro Phenate And Its Formulation	2500	1800.0	1800.0
2	H.E.D.P. and its formulations (Codex 661 and its formulations) Acetyl Chloride Route	35000	9628.0	9628.0
	H.E.D.P. and its formulations (Codex 661 and its formulations) Direct Route	---	15372.0	15372.0
3	Acetyl Chloride	6500	6500.0	6500.0
4	Sodium Salt of 5-Sulphono Isothalic Dimethyl Ester (SiPM)	360	360.0	360.0




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Sr. No.	EXISTING CONSENTED PRODUCT	Production as per Environmental Clearance MT/A	Production as per existing CTO, MT/A	Production after product mix, MT/A
5	Amino Tri Methylene Phosphonic Acid and its formulations (ATMP)	12000	6000.0	6000.0
6	Codex-551	600	600.0	600.0
7	Dispercel (Poly Maleic Acid)	252	252.0	252.0
8	THPE [(1,1,1, TRIS (4-HYDROXY PHENYL) ETHANE)] AND /OR DMBPC (DI-METHYL BIS PHENOL CYCLOHEXANE(DMBPC) AND ITS DERIVATIVES	1500	1025.0	1025.0
9	Lauracel	30	30.0	30.0
10	4-Hydroxythiobenzamide (FEBUXOSTAT T1)	12	12.0	12.0
11	ETHYL-2-(4-HYDROXYPHENYL)-4-METHYLTHIAZOLE-5-CARBOXYLATE (FEBUXOSTAT T2)	18	18.0	18.0
12	ETHYL-2-(3-FORMYL-4-HYDROXYPHENYL)-4-METHYL-1,3THIAZOLE-5-CARBOXYLATE (FEBUXOSTAT T3)	120	120.0	120.0
13	Ethyl-2-(3-Formyl-4-isobutoxyphenyl)-4-Methyl-1,3Thiazole-5-Carboxylate) (FEBUXOSTAT T4)	14	14.0	14.0
14	Ethyl 2-(3- Cyano-4-Isobutoxy phenyl)-4-methylthiazole -5-carboxylate FEBUXOSTAT T-5	75	75.0	75.0
15	5-(BROMOMETHYL)-4-(4-FLUOROPHENYL)-6-(1-METHYLETHYL)-2-METHYL (METHYLSULFONY) AMINO] PYRIMIDINE Z 7 BR	48	48.0	48.0
16	PHOSPHONIUM, [[4-(4-FLUOROPHENYL)-6-(1-METHYLETHYL)-2-[METHYL METHYLSUFONYL) AMINO]-5 PYRIMIDINYL]MEHTYL] TRIPHENYL-BROMIDE(1:1) Z 8.2	60	60.0	60.0
17	N-[4-(4-FLUOROPHENYL)-5-FORMYL-6-(1-METHYLETHYL)-2-PYRIMIDINYL]-N-METHYL METHANE SULFONAMIDE. Z7 FORMYL	25	25.0	25.0
18	6-HYDROXY-3,4-DIHYDRO-1H-QUINOLINE-2-ONE 6HQ	20	20.0	20.0

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MAHARASHTRA POLLUTION CONTROL BOARD

Sr. No.	EXISTING CONSENTED PRODUCT	Production as per Environmental Clearance MT/A	Production as per existing CTO, MT/A	Production after product mix, MT/A
19	4-[4-(4-(HYDROXYDIPHENYLMETHYL)-1-PIPERIDINYL)-1-HYDROXYBUTYL]-AADIMETHYLPHENYLACETIC AND FEXOFENADINE N-1 AND/OR A,ADIMETHYL-4-(1-HYDROXY-4(4-(HYDROXYDIPHENYLMETHYL)-1-PIPERIDINYL)BUTYL)-BENZENEACETIC ACID HYDROCHLORIDE (FEXOFENADINE HYDROCHLORIDE) & ITS INTERMEDIATES	26	26.0	26.0
20	1,3;2,4-bis (3,4-dimethylbenzylidene)sorbitol Exclar	75	75.0	75.0
21	n-Octyl Phosphonic Acid (NOPA)	75	75.0	75.0
22	Pregabalin((S)-3-(aminomethyl)-5-methylhexanoicacid) and its intermediate	20	20.0	20.0
23	Sitagliptine Phosphate (3-(Trifluoromethyl)5,6,7,8-tetrahydro-[1,2,4]triazolo[4,3-a]pyrazine hydrochloride)intremediate	20	20.0	20.0
24	4-[5-(4-methylphenyl)-3-(Trifluoromethyl)pyrazol-1-yl]benzenesulfonamide and Celecoxib intermediate(4-hydrazinobenzne-1-sulfonamide hydrochloride)	10	10.0	10.0
25	Benfotamine Phosphate	20	20.0	20.0
26	Cetilistat	6	6.0	6.0
27	Silodosine	2	2.0	2.0
28	Ethyl 2-(3-cyno-4 Isobutoxyphenyl)-4-methyl-1, 3 thiazole-5carboxylic acid FEBUXOSTAT T-6	25	25.0	25.0
29	4 - ACETOXY STYRENE (4 - ACS)	100	100.0	100.0
30	Phenyl Hydrazine	600	600.0	600.0
31	Phenyl hydrazine HCl	500	500.0	500.0
32	4 Chloro PH HCL	200	100.0	100.0
33	3 - [(S) - 1 - TERTBUTOXYCARBONYL - 4 - OXOPYRROLIDIN - 2 - YL CARBONYL] THIAZOLIDINE (OXO)	25	25.0	25.0

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Sr. No.	EXISTING CONSENTED PRODUCT	Production as per Environmental Clearance MT/A	Production as per existing CTO, MT/A	Production after product mix, MT/A
34	Teneligliptin	40	40.0	40.0
35	PPZ - 1- (3 - METHYL -1 - PHENYL - 1 - PYRAZOL - 5 - YL) PIPERAZINE.	25	25.0	25.0
36	Solefinacin Base	25	3.0	3.0
37	Solefinacin Succinate	3	3.0	3.0
38	Sertaconazole	20	5.0	5.0
39	Nizatidine	25	5.0	5.0
40	Fluorobenzene and its derivatives	1000	300.0	300.0
41	Phoponates and its derivatives	500	500.0	500.0
42	Phosphates and its derivatives	500	250.0	250.0
43	Phosphites and its derivatives	500	250.0	250.0
44	R & D and pilot for industrial Chemicals and Intermediates	60	60.0	60.0
45	Hydrochloric Acid	75000	58000.0	58000.0
46	(R)-9-[2(PHOSPHONOMETHOXY) PROPYL]ADENINE (PMPA)	75	75.0	75.0
47	Phosphorous Tri chloride (PCI3)	0	0	20000.0
	TOTAL	--	103079.0	123079.0

B. Pollution load Details:

i) Water Consumption & Wastewater Aspect

Before Product Mix

Sr. No.	Particulars	Quantity in CMD	Effluent generation in CMD		COD				TDS			
			Strong	Weak	Strong		Weak		Strong		Weak	
					Kg/Day	Mg/l	Kg/Day	Mg/l	Kg/Day	Mg/l	Kg/Day	Mg/l
1	Water Consumption	923			Not Applicable							
2	Trade Effluent Generation											
A	Process & Washing Activity	216	--	--	--	--	--	--	--	--	--	--
B	Cooling Tower & Boiler	36	--	--	--	--	--	--	--	--	--	--
	Total	252	176	76	29333	166665	47.2	621	18284.5	103889	250.4	3295

MAHARASHTRA POLLUTION CONTROL BOARD

3	Domestic Effluent Generation, CMD	72	72	--	--	--	--
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Effluent Generation as per existing Consent to Operate: Domestic -72 CMD + Industrial – 252 CMD and as per Environmental Clearance Domestic -81 CMD + Industrial – 549 CMD

After Product Mix

Sr. No.	Particulars	Quantity in CMD	Effluent generation in CMD		COD				TDS			
			Strong	Weak	Strong		Weak		Strong		Weak	
					Kg/Day	Mg/l	Kg/Day	Mg/l	Kg/Day	Mg/l	Kg/Day	Mg/l
1	Water Consumption	923			Not Applicable							
2	Trade Effluent Generation											
A	Process & Washing Activity	216	--	--	--	--	--	--	--	--	--	--
B	Cooling Tower & Boiler	36	--	--	--	--	--	--	--	--	--	--
	Total	252	176	76	29333	166665	47.2	621	18284.5	103889	250.4	3295
3	Domestic Effluent Generation, CMD	72	72		--	--	--	--	--	--	--	--

Effluent Generation Domestic -72 CMD + Industrial – 252 CMD

- No Change in Water Consumption as compared to existing C to O
- No Change in Effluent generation as compared to existing C to O
- No Change in Average COD Load as compared to existing C to O

Treatment System

i) Trade Effluent:

- The generated waste water is being treated in full-fledged Effluent treatment System comprising of MEE, ATFD, ETP, RO & Spray Dryer.
- 252 CMD of total effluent from the plant is segregated in 3 streams
High TDS/High COD Stream: 86 CMD – (From Process),




MAHARASHTRA POLLUTION CONTROL BOARD

Low TDS/High COD Stream: 90 CMD - (From Process),

Low TDS/Low COD Stream: 76 CMD. - (From Utility, washing activity),

- c. Segregated concentrated stream 86 CMD (High TDS/High COD Stream) is fed to stripper. After treatment in Stripper it will fed to MEE & ATFD. MEE condensate along with primary treated Low TDS/High COD Stream 90 CMD from process is being treated in secondary and tertiary treatment of ETP.
- d. After tertiary treatment 176 CMD is fed to RO. 158.5 CMD RO permeate is being reused in the utilities. 17.5 RO reject is being treated in Spray Dryer to achieve Partial ZLD.
- e. Segregated Low TDS/Low COD Stream: 76 CMD is treated in ETP 2 comprising primary, secondary and tertiary treatment along with the domestic sewage 72 CMD. After tertiary treatment the treated effluent is sent to CETP for disposal as per valid CTO.
- f. Capacity of ETP 1 is 480 CMD
- g. Capacity of ETP 2 is 350 CMD

ii) Domestic Effluent:

Domestic sewage 72 CMD is treated in ETP 2 comprising primary, secondary and tertiary treatment along with the 76 CMD. After tertiary treatment the treated effluent is sent to CETP for disposal as per valid CTO.

ii) Air Emission Load:

Flue Gas Emissions

Sr. No.	Stack No.	Stack Attached to	Fuel	Existing Fuel Consumption	Fuel Consumption after Change in Product Mix	APC system	Stack Height
1	S-1	Boiler-1 (6 TPH)	Coal	72.5 TPD	72.5 TPD	Cyclone Separator, Baghouse & Stack	33 m
2		Boiler-2 (12 TPH)					
3	S-2	DG Set (1010 KVA)	HSD	2400 Lit/Hr	2400 Lit/Hr	Acoustic Enclosure & Stack	30 m
4	S-3	DG Set (500 KVA)	HSD	1200 Lit/Hr	1200 Lit/Hr	Acoustic Enclosure & Stack	16 m *

* In CTO stack height for DG set having capacity 500 KVA is given as 30 m. However, actual stack height is 16m which is as per CPCB guidelines for DG set stack height.

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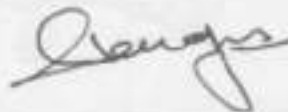
Process Emissions

Sr. No.	Stack No.	Stack Attached to	APC system	Stack Height	Pollutant
1	S-4	Codex (HCl Tail Gas Tower)	Dual Media Scrubber & Stack	15 m	HCl
2	S-5	Codex (Acetyl Chloride Packing)	Wet Scrubber & Stack	10 m	HCl
3	S-6	Codex (Acetic Acid Scrubbing)	Wet Scrubber & Stack	12 m	HCl
4	S-7	Codex (PCl ₃ Scrubber)	Wet Scrubber & Stack	12 m	HCl
5	S-8	Codex (Acetyl Chloride Scrubbing)	Wet Scrubber & Stack	12 m	HCl
6	S-9	SPCP (Drum Dryer)	Alkali Scrubber & Stack	25 m	HCl
7	S-10	SPCP (Packing Area)	Alkali Scrubber & Stack	25 m	HCl
8	S-11	SPCP (Reactor Neutralizer)	Alkali Scrubber & Stack	25 m	HCl
9	S-12	SPCP (HCl Scrubbing)	Dual Media Scrubber & Stack	25 m	HCl
10	S-13	PIP (HCl Scrubbing System)	Dual Media Scrubber & Stack	15 m	HCl
11	S-14	PIP (Common Vent)	Dual Media Scrubber & Stack	15 m	HCl
12	S-15	Pharma-1 (Process)	Alkali Scrubber & Stack	15 m	Solvents (VOC)
13	S-16	Pharma-2 (HCl Scrubbing System)	Alkali Scrubber & Stack	15 m	HCl
14	S-17	Spray Dryer (Fuel Coal: 350 Kg/Hr)	Wet Scrubber & Stack	30 m	SO ₂ (<84 Kg/Day) and TPM (<150 mg/Nm ³)
15	S-18	PH (Common Vent Scrubber)	Alkali Scrubber & Stack	15 m	SO _x
16	S-19	Solvent Recovery Unit	Stack	15 m	Solvents (VOC)
17	S-20	Emergency Scrubber (PCl ₃ Plant Chlorine Storage)	Alkali Scrubber & Stack	15 m	Chlorine
18	S-21	Emergency Disc Failure (PCl ₃ Plant Reactor)	Alkali Scrubber & Stack	15 m	Chlorine/ Acid Mist
19	S-22	Process Stack (PCl ₃ Plant)	Alkali Scrubber & Stack	15 m	Acid Mist

➤ Note: Stack No. 20, 21 & 22 are not mentioned in existing C to O which are installed after obtaining Consent to Establish.

Process Emission Parameters:

Sr. No.	Parameters	Before change in product-mix	After change in product-mix	MPCB Limit
1	HCl/Acid Mist	<35 mg/Nm ³	<35 mg/Nm ³	<35 mg/Nm ³

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		5-10 mg/Nm ³	5-10 mg/Nm ³	
2	SO ^x (Process)	--	--	Not Mentioned
3	Cl ²	--	--	Not Mentioned
4	HBr [*]	--	--	Not Mentioned
5	VOCS [*]	--	--	Not Mentioned

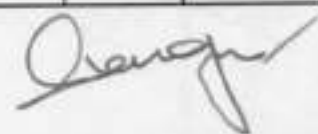
Note: Parameters were not mentioned in current valid CTO, but coming from existing products only, hence incorporated.

iii) Hazardous Waste Load

Sr. no.	Type of Waste	Cat. No.	As Per EC	As Per CTO.	Existing Qty.	After Change in Product Mix Qty.	UOM	Disposal
1	Used/ spent oil	5.1	6 KLPA	3	3	3	MT/A	Sale to Authorized party/Recycle/Re-processor/ CHWTSDF
2	Distillation residue	20.3	900	600	600	600	MT/A	CHWTSDF/Pre-Processor/Co-Processor
3	Spent catalyst	28.2	12	8	8	8	MT/A	CHWTSDF
4	Empty barrels/ containers/ liners contaminated with hazardous chemicals/ wastes	33.1	38130	30710	30710	30710	Nos./A	Sale to Authorized party/Recycle/ CHWTSDF
5	Spent ion exchange resin containing toxic metals	35.2	0.36	0.24	0.24	0.24	MT/A	Sale to Authorized party/Recycle/Re-processor/ CHWTSDF
6	Chemical sludge from waste water treatment (Dry Basis)	35.3	12500	3000	3000	3000	MT/A	CHWTSDF/Pre-Processor/Co-Processor
7	Concentration or evaporation residues (Dry Basis)	37.3		6000	6000	6000	MT/A	Sale to Authorized party/Recycle/Re-processor/ CHWTSDF
8	Filters and filter material which have organic	--	9	3	3	3	MT/A	CHWTSDF

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Sr. no.	Type of Waste	Cat. No.	As Per EC	As Per CTO.	Existing Qty.	After Change in Product Mix Qty.	UOM	Disposal
	liquid (Biocel Filter Cake)							
9	Process wastes/ residue (Dilute Methanol)	29.1	450	450	450	450	MT/A	Sale to Authorized party/Recycle/Re-processor/ CHWTSDF
10	Process waste / residue (Spent Acid)	29.1	1645	1645	1645	1645	MT/A	Sale to Authorized party/Recycle/Re-processor/ CHWTSDF
11	Process Wastes / residue (Dilute Acetic Acid)	29.1	1200	1200	1200	1200	MT/A	Sale to Authorized party/Recycle/Re-processor/ CHWTSDF
12	Spent Organic Solvent (Mixed Solvents)	28.6	600	600	600	600	MT/A	Sale to Authorized party/Recycle/Re-processor/ CHWTSDF
13	Process Wastes / residue (30% Sodium Sulphite)	29.1	936	936	936	936	MT/A	Sale to Authorized party/Recycle/Re-processor/ CHWTSDF
14	Process Wastes / residue (Spent Ethyl Bromide)	29.1	187.5	187.5	187.5	187.5	MT/A	Sale to Authorized party/Recycle/Re-processor/ CHWTSDF
15	Process Wastes / residue (Spent Magnesium Acetate)	29.1	75	75	75	75	MT/A	Sale to Authorized party/Recycle/Re-processor/ CHWTSDF
16	Process waste/residue (spent sodium bromide solution)	29.1	1424.5	1424.5	1424.5	1424.5	MT/A	Sale to Authorized party/Recycle/Re-processor/ CHWTSDF
17	Process waste/ residue (Dilute Thiophosphoric Acid)	29.1	11.75	11.75	11.75	11.75	MT/A	Sale to Authorized party/Recycle/Re-

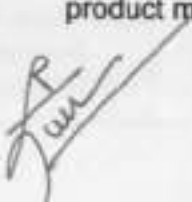
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Sr. no.	Type of Waste	Cat. No.	As Per EC	As Per CTO.	Existing Qty.	After Change in Product Mix Qty.	UOM	Disposal
								processor/ CHWTSDF
18	Process waste/ residue (Dilute Di methane sulphonic Acid)	29.1	195	195	195	195	MT/A	Sale to Authorized party/Recycle/Re- processor/ CHWTSDF
19	Process waste/ residue (Dilute Di methyl Formamide)	29.1	56	56	56	56	MT/A	Sale to Authorized party/Recycle/Re- processor/ CHWTSDF
20	Process waste/ residue (Dilute Bromide solution)	29.1	140	140	140	140	MT/A	Sale to Authorized party/Recycle/Re- processor/ CHWTSDF
21	Process waste/ residue (Formic Acid)	29.1	96	96	96	96	MT/M	Sale to Authorized party/Recycle/Re- processor/ CHWTSDF
22	Process Wastes / residue	29.1	12	4	4	4	MT/A	Sale to Authorized party/Recycle/Re- processor/ Pre- Processor/Co- Processor/ CHWTSDF

Note: There is no Change in hazardous waste.

Technical Committee Deliberations:

The proposed project was discussed on the basis of documents – NIPL Certificate and presentation made by the industry. Product wise load calculation in terms of wastewater, Air emissions & Hazardous waste generation were discussed. Existing consent to operate, Environmental Clearance, NIPL Certificate issued by Goldfinch Engineering Systems Pvt. Ltd and product mix Pro-forma are taken on the record.



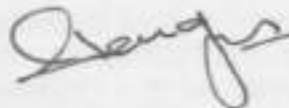

Committee after due deliberations noticed that:

- After product mix the total production capacity of the plant will be increased from 103079.0 MT/A to 123079.0 MT/A i.e. 20000 MT/A increase in production capacity.
- The water consumption, trade effluent generation & organic load will remain same.
- The overall Hazardous waste quantity after product mix will remain the same.
- The overall pollution load is not increased after change in product mix

Technical Committee Decision:

The Committee has decided to **recommend** the case for change in product under product mix with a compliance of the following conditions:

1. Industry shall comply with all the conditions stipulated in Environmental Clearance and ensure display/upload of six-monthly compliance monitoring report on their official website.
2. Industry should not manufacture any other product for which permission is not granted by the MPCB.
3. Industry shall ensure connectivity of OCEMS data to Boards server and transmit the data continuously for wastewater treatment.



MAHARASHTRA POLLUTION CONTROL BOARD

Agenda Item No.	10
Proposal No.	MPCB-CONSENT-0000151650
Project Details	Privi Speciality Chemicals Limited (Unit-I), Plot No. A-07, MIDC Mahad, Taluka Mahad, Dist. Raigad
NIPL Certificate	NIPL Certificate issued by M/s. Aditya Environmental Services Private Limited vide letter dated 11/10/2022
Name of the Industry Representative present	1. Sh. Sachin Rajurkar, Vice President 2. Sh. Naveen S.R., General Manager

Introduction:

This has reference to the online proposal submitted vide No. MPCB-CONSENT-0000151650 along with the copies of documents seeking amendment in existing Consent to Operate under change in product-mix under the provisions of EIA Notification 2006 amended on 23-Nov-16.

Existing Environment Clearances (EC):

1. EC was granted to Privi Specialty Chemicals Limited (Unit-I) by SEIAA vide SEAC-2013/CR-242/TC-2 dt. 08/10/2015.
2. MPCB granted Consent to Operate to Privi Specialty Chemicals Limited (Unit-I) vide CONSENT NO - Format 1.0/CC/UAN NO 0000095236/CR2011000997 Valid up to 30/08/ 2025.
3. The company was formerly known as Privi Organics India Ltd. Hence, CTO was amended on 03/12/2020 for name change vide amendment no. MPCB/UAN No. 0000004998/AS(T) /Amend-2012000008.

The industry has given the presentation before the committee and gist of the presentation is as follows:

Project Details:

A) Products with change in product mix as below:

sr.no.	Product	*As per EC	**Existing as per CTO	Proposed change	After Change in Product Mix	Remarks
		Qty MTPA	Qty MTPA	Qty MTPA	Qty MTPA	
Manufacture of Synthetic Organic Chemicals						
1	Citronellol (COL)	120	60	-60	0	Manufacturing to be stopped & include in trading/repacking
2	Styrallyl Acetate	6	6	-6	0	Product




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						deleted
3	Geranyl Nitrile	6	0	0	0	Product deleted
4	Citronellol Acetate (Citronellyl acetate)	4.8	6	-6	0	Product deleted
5	Geranyl /Neryl Acetate	6	6	-6	0	Product deleted
6	Dihydro Myrcenol (DHMOL)	12	12	-12	0	Product deleted
7	Alpha Camphenelic Aldehyde Derivatives	12	12	-12	0	Product deleted
8	Amber Fluor and its derivatives , Amber gamma ,Cedar ketol	5400	5640	480	6120	Increase
9	Rose Oxide	6	6	-6	0	Manufacturing to be stopped & included in trading/repacking
10	Indian Sandal Fleur	12	12	-12	0	Product deleted
11	Indian Sandal Core	108	300	-60	240	Decrease
12	Indian Sandal Touch	6	6	-6	0	Product deleted
13	Ionones	12	0	0	0	Product deleted
13.1	Gamma Methyl Ionone (GMI)					
13.2	Normal Methyl Ionone (NMI)	72	36	-36	0	Product deleted
13.3	Alpha Ionone (AI) & Ionone 100%				0	Product deleted
13.4	Beta Ionone (BI) (Technical /PG)				0	Product deleted
14	Geraniol/Nerol Extra Pure	6	6	-6	0	Product deleted
15	Para Tertiary Butyl Cyclohexyl acetate	6	6	-6	0	Product deleted

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(PTBCHA)						
16	Myrcene 90 /Myrcene Supra	600	396	-396	0	Product deleted
17	L-Limonene	300	300	121	421	Increase
18	Citral Extra Pure	360	240	-240	0	Manufacturing to be stopped & included in Trading/repacking
19	Aldehyde C11	144	144	-144	0	Product deleted
	Total	7198.8	7194.0	-413	6781	
FORMULATION BY BLENDING OF FRACTIONS						
1	PCM Fractions	0	0	1659	1659	New activity
2	Amber odour blend 5091	0	0	1175	1175	
3	Woody odour 5099	0	0	197	197	
4	Limonene -LP	0	0	953	953	
	Total	0	0	3984	3984	
Re-Packing /Trading Activity						
1	Citronellol (COL)	0	60	0	60	Shifted from Manufacturing to trading / re-packing activity
2	Rose Oxide	0	6	114	120	
3	Cedar Ketol	0	0	80	80	
4	Citral Extra Pure	0	240	-120	120	
	Total	0	306.0	74.0	380.0	
DISTILLATION						
1	Distillation of Aroma chemicals	0	0	468	468	New activity
	Total	0	0	468	468	
BY-PRODUCT (CO-PRODUCT)						
1	Aq. Fluoroboric acid OR	0	0	827	827	New addition
2	Potassium/Sodium/ Calcium Tetrafluoroborate	0	0	313	313	

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The highlights of the proposal are:

- a) Marginal decrease 5.74% in overall product quantity from 7194 MTPA to 6781 MTPA and change in product mix (existing and proposed).
- b) Increase of AmberFluer and its derivatives, Amber gamma, Cedarketol production quantity from 5640 MTPA to 6120 MTPA, L-Limonene quantity from 300 MTPA to 421 MTPA
- c) There is decrease in Indian Sandal Core quantity from 300 MTPA to 240 MTPA.
- d) Rest all other products listed in existing CTO are proposed to be deleted.
- e) Distillation of aroma chemicals is added as new product with proposed capacity of 468 MTPA.
- f) New activity of Formulation products prepared by blending of various fractions are proposed with proposed capacity of 3984 MTPA.
- g) By-products (co-products) Aqueous Fluoroboric acid (Fluoroboric acid) 827 MTPA OR Potassium/Sodium/Calcium Tetrafluoroborate is 313 MTPA are proposed.
- h) Repacking /Trading activity of 380 MTPA is also proposed to be included in the CTO.

B) Pollution load Details:

i) Water Consumption and Waste Water Aspect

Water consumption Aspect

Sr. No	Purpose	*Existing Water Consumption, as per CTO (CMD)	Proposed After Change in Product Mix, (CMD)	Proposed change in Water Consumption (CMD)
1	Domestic	12.5	12.5	0
2	Industrial			
2.1	Processing	88.82	82	-7
2.2	Cooling Tower	219.65	219.65	0
3	Gardening	0	0	0
	Grand Total	321	314	-7

Waste Water Aspect

No	Purpose	Existing Effluent Generation, as per CTO (*), cmd	Effluent Generation After Change in product Mix, cmd		Mode of Disposal & Ultimate Receiving Body
1	Domestic	10	10	No change	Effluent is sent to Privi-Unit-III & treated in common effluent treatment plant for Unit I and

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2	Industrial				Unit III, located at Unit III (Plot A-3) Part of the treated effluent is reused and balance is sent to CETP (As permitted in CTO of both units) ** Digital flow meters have been installed on low TDS and High TDS stream pipelines to record effluent quantity from/to Unit I to Unit III and vice versa as stipulated in CTO.
2.1	Processing	83.82	83	-1	
2.2	Cooling tower blowdown	28.42	28.42		
3	Gardening	0	0		
	Grand Total	122	121	-1	

COD and TDS loads

POLLUTION LOAD PARAMETER	EXISTING	POST CHANGE OF PRODUCT MIX	REMARKS
Total COD kg/day	597.04	332.72	Reduction by 264.32 Kg/day
*Total TDS kg/day	535.92	875.91	Increase by 340 kg/day (10.2 TPM)

After Product-mix:

- Fresh Water consumption will marginally reduce by 7CMD after proposed product mix.
- Effluent generation will remain unchanged after proposed change of product mix.
- COD load to ETP will get reduced by 44% after proposed change of product mix
- TDS—increase in TDS is because Unit is proposing to dispose off some by products by discharging them to ETP since they are unable to locate vendors having Rule 9 permission for recycling these despite taking steps to reduce quantity of by-products generation.
- The effluent is sent to Privi-Unit-III (as per existing CTO) for treatment in ETP and treated effluent is discharged to CETP as consented in Privi-Unit-III CTO.

Treatment System:

- **Sewage and Trade effluent**
 - Both domestic and trade effluents are sent to Privi Unit-III for treatment, as permitted in CTOs of both units.
 - PP has provided comprehensive ETP at Unit III comprising Primary- secondary (Extended aeration) followed by Tertiary treatment (comprising RO and MEE) for treating the effluent from Unit I and Unit III – the effluent quality at various stages are as below:

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Parameter	Unit I	Unit III	Weighted average load Inlet to ETP	Remarks
Low TDS stream				Treated in ETP at Unit III comprising Primary-secondary (Extended aeration) followed by Tertiary treatment (comprising RO)
Flow	116	136	252	
COD	4842	5000	4927	
BOD	1404	1400	1401	
TDS	5242	5100	5165	
High TDS stream				RO reject from ETP + High TDS stream Treated in MEE – condensate sent to aeration tank for further treatment
Flow	5	4	9	
COD	5000	108679	51080	
BOD	---	---	---	
TDS	148000	134000	141777	

Final Effluent from ETP after Change of Product Mix

Parameter	Weighted avg load	
	Inlet to ETP	ETP outlet
Low TDS stream		
Flow	252	252
COD	4927	< 229
BOD	1401	BDL
TDS	5165	< 2100
High TDS stream		
Flow	-	--
COD	-	--
BOD	-	--

From the above, it can be seen that there is no increase in effluent load at the outlet of ETP & ETP system is adequate to meet MPCB standards.




ii) Air Pollution Load:

Utility Stacks

Details of utility stacks, fuel consumptions & emissions in existing (as per CTO) & post product mix scenario are as below-

Stack no as per CTO.	Stack Attached To	Type of Fuel	Existing Fuel Consumption	Proposed Fuel Consumption	Stack Height in Mtrs
S2	D.G. Set (380 KVA)	HSD	200 Ltr/Hr	No change	4.0
S3	D.G. Set (380 KVA)	HSD	200 Ltr/Hr	No change	4.0

Privi Unit-I CTO lists one 3TPH boiler in Schedule-III under stack no S1. However, Privi- Unit-I has dismantled this boiler in the year 2017 and the same was intimated to MPCB on 20/06/2017 & CTO amendment application for this has been filed (MPCB-CONSENT-0000095236 dated 8th august 2022).

Boiler

Steam supply to Privi Unit-I is from boiler of Privi-Unit-III.

Steam Requirement

Unit-III at Plot no-3 is supplying steam requirement of unit. The existing steam requirement is 6.03 MT/hr which will be 6.03 MT/hr post change of product mix. Hence, there is no change in steam requirement.

Process Stacks

There are no process stacks existing & the same will continue post change of product mix. There is no additional utility and process stacks proposed. Thus, there is no change in the emissions from utility stacks. Thus, the emissions post change of product mix will be within the limits specified in CTO.

There is no change in overall fuel burning sources/ fuel consumption/ Air emissions due to proposed change in product mix.




MAHARASHTRA POLLUTION CONTROL BOARD

iii) Hazardous Waste Load:

CTO Sr. no.	By-Products	Category	UOM	Existing Quantity (TPA)	Proposed additional Quantity (TPA)	After Change in Product Mix Quantity (TPA)	Remarks	Disposal Method
1	Spent oil	5.1	TPA	7.2	0.00	7.20	No change	Sale to authorized process
2	Waste contaminated with oil (cotton/gaskets)	5.2	Kg/A	600	0.00	600	No change	CHWTSDP
3	Residues & Hydrocarbon (contaminated aromatic, aliphatic or naphthenic solvents may or may not be fit for reuse)	20.1	TPA	8.64	0.00	0	To be Removed since no generation	NA
4	Discarded containers/barrels	33.3	Nos/A	3120	0.00	3120	No change	Recycle/Sale to authorized party

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CTO Sr.no.	By-Products	Category	UOM	Existing Quantity (TPA)	Proposed additional Quantity(TPA)	After Change in Product Mix Quantity(TPA)	Remarks	Disposal Method
	liners							after decontamination
5	Chemical sludge form wastewater treatment	35.3	TPA	120	0.00	120.00	No change	Sale to authorized party/ CHWTSDF/Cement Industry
6	Any process or distillation residue	36.1	TPA	240	0.00	0	To be Removed since no generation	CHWTSDF or Sale to authorized party
7	Sludge from concentration technique (MEE)	36.1	TPA	10.8	0.00	10.80	To be included in CTO of Unit-III	Sale to authorized party/ CHWTSDF
8	Citronellol Column Tops	28.10	TPA	1.80	-1.80	0.00	Product Citronellol deleted	Sale to authorized party/ CHWTSDF
9	Citronellol Column Bottom Mass	28.10	TPA	0.78	-0.78	0.00	Product Citroellol deleted	Sale to authorized party/ CHWTSDF




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CTO Sr. no.	By-Products	Category	UOM	Existing Quantity (TPA)	Proposed additional Quantity (TPA)	After Change In Product Mix Quantity (TPA)	Remarks	Disposal Method
10	Styrallyl acetate Column Tops	28.10	TPA	0.26	-0.26	0.00	Product Styrallyl acetate deleted	Sale to authorized party/ CHWTSDF
11	Styrallyl acetate Column Bottom Mass	28.10	TPA	0.31	-0.31	0.00	Product Styrallyl acetate deleted	Sale to authorized party/ CHWTSDF
12	Citronellyl Acetate Column Tops	28.10	TPA	0.19	-0.19	0.00	Product Citronellol acetate deleted	Sale to authorized party/ CHWTSDF
13	Citronellyl Acetate Column Bottom Mass	28.10	TPA	0.26	-0.26	0.00	Product Citronellol acetate deleted	Sale to authorized party/ CHWTSDF
14	Geranyl Acetate Column Tops	28.10	TPA	0.23	-0.23	0.00	Product Geranyl Acetate deleted	Sale to authorized party/ CHWTSDF
15	Geranyl Acetate Column Bottom Mass	28.10	TPA	0.31	-0.31	0.00	Product Geranyl Acetate deleted	Sale to authorized party/ CHWTSDF
16	Dilute Sulphuric acid (30-40 %)	28.10	TPA	31.33	-31.33	0.00	Product DHMOL deleted	Sale to authorized party/ CHWTSDF
17	Dihydromyrcenol (DHMOL) Column Tops	28.10	TPA	1.90	-1.90	0.00	Product Dihydromyrcenol	Sale to authorized party/ CHWTSDF




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CTO Sr. no.	By-Products	Category	UOM	Existing Quantity (TPA)	Proposed additional Quantity (TPA)	After Change in Product Mix Quantity (TPA)	Remarks	Disposal Method
							(DHMOL) deleted	
18	Dihydromyrcenol (DHMOL) Column Bottom Mass	28.10	TPA	1.00	-1.00	0.00	Product Dihydromyrcenol (DHMOL) deleted	Sale to authorized party/ CHWTSDF
19	Alpha Camphenelic Aldehyde Derivatives Column Tops	28.10	TPA	0.86	-0.86	0.00	Product Alpha Camphenelic Aldehyde deleted	Sale to authorized party/ CHWTSDF
20	Alpha Camphenelic Aldehyde Derivatives Column Bottom Mass	28.10	TPA	1.46	-1.46	0.00	Product Alpha Camphenelic Aldehyde deleted	Sale to authorized party/ CHWTSDF
21	Aqueous Fluoroboric acid (Fluoroboric acid) Or	28.10	TPA	1139.28	-1139.28	0.00	The quantity has been reduced to 827 TPA and covered under by-product	By-product to Sale to authorized party
22	Spent Phosphoric acid	28.10	TPA	1500.24	-1500.24	0.00	Change in	Sent to Unit-III ETP




MAHARASHTRA POLLUTION CONTROL BOARD

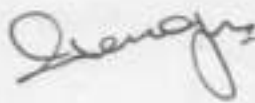
CTO Sr. no.	By-Products	Category	UOM	Existing Quantity (TPA)	Proposed additional Quantity (TPA)	After Change in Product Mix Quantity (TPA)	Remarks	Disposal Method
	Layer/Sodium Phosphate						process as described in sr. no.2.2 of this certificate.	for treatment. Separated along with MEE sludge to be disposed off at CHWTSDF
23	Sodium Phosphate wet	28.10	TPA	654.24	-654.24	0.00		Reuse/recycle /
24	Sodium Phosphate Solution	28.10	TPA	1827.36	-1827.36	0.00		Sale to authorized party/ CHWTSDF
25	Recovered Toluene	28.10	TPA	637.32	-607.33	29.99	Reduction due to decrease in product capacity	Recycle/reuse Sale to authorized party/ CHWTSDF
26	Amberfleur & its Derivatives Like Ammer gamma, Cedarketol Column Tops/ PCM Tops	28.10	TPA	1911.96	-1911.96	0.00	Proposed to use for making formulations by blending	Sale to authorized party/ CHWTSDF
27	Amberfleur & its Derivatives Like	28.10	TPA	1223.88	-1223.88	0.00	Proposed to use for making	Sale to authorized party/ CHWTSDF

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CTO Sr. no.	By-Products	Category	UOM	Existing Quantity (TPA)	Proposed additional Quantity (TPA)	After Change in Product Mix Quantity (TPA)	Remarks	Disposal Method
	Amber gamma, Cedarketol Column Bottom Mass						formulations by blending	
28	Rose Oxide Column Tops	28.10	TPA	0.44	-0.44	0.00	Product Rose Oxide deleted	Sale to authorized party/ CHWTSDF
29	Rose Oxide Column Bottom Mass	28.10	TPA	1.34	-1.34	0.00	Product Rose Oxide deleted	Sale to authorized party/ CHWTSDF
30	Catalyst A recovered (recycled)	28.10	TPA	1.12	-1.12	0.00	Product Indian Sandal Fleur deleted	Sale to authorized party/ CHWTSDF
31	Recovered Cyclohexane	28.10	TPA	2.86	-2.86	0.00	Product Indian Sandal Fleur deleted	Sale to authorized party/ CHWTSDF
32	Indian Sandal Fleur Column Tops	28.10	TPA	4.86	-4.86	0.00	Product Indian Sandal Fleur deleted	Sale to authorized party/ CHWTSDF
33	Indian Sandal Fleur Column Bottom Mass	28.10	TPA	3.12	-3.12	0.00	Product Indian Sandal Fleur	Sale to authorized party/ CHWTSDF

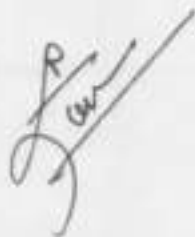
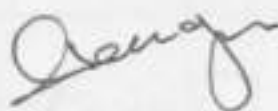
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CTO Sr. no.	By-Products	Category	UOM	Existing Quantity (TPA)	Proposed additional Quantity (TPA)	After Change in Product Mix Quantity (TPA)	Remarks	Disposal Method
							deleted	
34	Recovered Methanol	28.10	TPA	12.97	-12.97	0.00	Product Indian Sandal Fleur deleted	Sale to authorized party/ CHWTSDF
35	Sodium acetate Solution	28.10	TPA	8.32	-8.32	0.00	Product Indian Sandal Fleur deleted	Sent to Unit-III ETP for treatment. Separated along with MEE sludge to be disposed off at CHWTSDF
36	Sodium acetate Solution	28.10	TPA	177.90	-177.90	0.00	Change in process as described in sr. no. 2.2 of this certificate.	Sale to authorized party/ CHWTSDF
37	Rec. Catalyst A	28.10	TPA	27.90	-27.90	0.00	Product Indian Sandal core deleted	Sale to authorized party/ CHWTSDF




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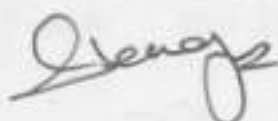
CTO Sr. no.	By-Products	Category	UOM	Existing Quantity (TPA)	Proposed additional Quantity (TPA)	After Change in Product Mix Quantity (TPA)	Remarks	Disposal Method
38	Recovered cyclohexane	28.10	TPA	101.70	-101.70	0.00	Product Indian Sandal Fleur deleted	Recycle/reuse Sale to authorized party/ CHWTSDF
39	Recovered Methanol	28.10	TPA	322.50	-8.10	314.40	Reduction of methanol usage in process	Recycle/reuse Sale to authorized party/ CHWTSDF
40	Indian Sandal Core Column Tops	28.10	TPA	112.80	-112.80	0.00	Proposed to use for making formulations by blending	Sale to authorized party/ CHWTSDF
41	Indian Sandal Core Column Bottom Mass	28.10	TPA	69.90	-69.90	0.00	Proposed to use for making formulations by blending	Sale to authorized party/ CHWTSDF
42	Indian Sandal Touch Column Tops	28.10	TPA	1.25	-1.25	0.00	Product Indian Sandal Fleur deleted	Sale to authorized party/ CHWTSDF

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CTO Sr. no.	By-Products	Category	UOM	Existing Quantity (TPA)	Proposed additional Quantity (TPA)	After Change in Product Mix Quantity (TPA)	Remarks	Disposal Method
43	Indian Sandal Touch Column Bottom Mass	28.10	TPA	1.64	-1.64	0.00	Product Indian Sandal Fleur deleted	Sale to authorized party/ CHWTSDF
44	Gamma Methyl Ionone Column Tops	28.10	TPA	2.92	-2.92	0.00	Product Gamma Methyl Ionone deleted	Sale to authorized party/ CHWTSDF
45	Gamma Methyl Ionone Column Bottom Mass	28.10	TPA	5.40	-5.40	0.00	Product Gamma Methyl Ionone deleted	Sale to authorized party/ CHWTSDF
46	Normal Methyl Ionone Column Tops	28.10	TPA	3.13	-3.13	0.00	Product Normal Methyl Ionone deleted	Sale to authorized party/ CHWTSDF
47	Normal Methyl Ionone Column Bottom Mass	28.10	TPA	4.18	-4.18	0.00	Product Normal Methyl Ionone deleted	Sale to authorized party/ CHWTSDF
48	Alpha Ionone (AI) &	28.10	TPA	1.22	-1.22	0.00	Product Alpha	Sale to authorized

CTO Sr. no.	By-Products	Category	UOM	Existing Quantity (TPA)	Proposed additional Quantity (TPA)	After Change in Product Mix Quantity (TPA)	Remarks	Disposal Method
	Ionone 100% Column Tops						Ionone (AI) & Ionone 100% deleted	party/ CHWTSDF

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49	Alpha Ionone (AI) & Ionone 100% Column Bottom Mass	28.10	TPA	2.09	-2.09	0.00	Product Alpha Ionone (AI) & Ionone 100% deleted	Sale to authorized party/ CHWTSDF
50	Dilute Sulphuric acid	28.10	TPA	92.05	-92.05	0.00	Product Dihydromyrcenol (DHMOL) deleted	Sale to authorized party/ CHWTSDF
51	Recovered Toluene	28.10	TPA	11.05	-11.05	0.00	Product Beta Ionone (BI) (Beta Ionone Technical /PG) deleted	Sale to authorized party/ CHWTSDF
52	Beta Ionone (BI) (Beta Ionone Technical /PG) Column Tops	28.10	TPA	1.66	-1.66	0.00	Product Beta Ionone (BI) (Beta Ionone Technical/PG) deleted	Sale to authorized party/ CHWTSDF

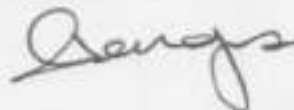
CTO Sr. no.	By-Products	Category	UOM	Existing Quantity (TPA)	Proposed additional Quantity (TPA)	After Change in Product Mix Quantity (TPA)	Remarks	Disposal Method
53	Beta Ionone (BI) (Beta Ionone Technical /PG) Column Bottom Mass	28.10	TPA	2.56	-2.56	0.00	Product Beta Ionone (BI) (Beta Ionone Technical/PG) deleted	Sale to authorized party/ CHWTSDF
54	Geraniol/Nerol Extra Pure Column Tops	28.10	TPA	0.11	-0.11	0.00	Product Geraniol/Nerol Extra Pure deleted	Sale to authorized party/ CHWTSDF
55	Geraniol/Nerol Extra Pure Column Bottom Mass	28.10	TPA	0.05	-0.05	0.00	Product Geraniol/Nerol Extra Pure deleted	Sale to authorized



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								party/ CHWTSDF
56	Para-Tertiary Butyl Cyclohexyl Acetate (PTBCHA) Column Tops	28.10	TPA	0.46	-0.46	0.00	Product Para-Tertiary Butyl Cyclohexyl Acetate (PTBCHA) deleted	Sale to authorized party/ CHWTSDF

CTO Sr. no.	By-Products	Category	UOM	Existing Quantity (TPA)	Proposed additional Quantity (TPA)	After Change in Product Mix Quantity (TPA)	Remarks	Disposal Method
57	Para-Tertiary Butyl Cyclohexyl Acetate (PTBCHA) Column Bottom Mass	28.10	TPA	0.14	-0.14	0.00	Product Para-Tertiary Butyl Cyclohexyl Acetate (PTBCHA) deleted	Sale to authorized party/ CHWTSDF
58	Myrcene 90 /Myrcene Supra Column Tops	28.10	TPA	109.30	-109.30	0.00	Product Myrcene 90 /Myrcene deleted	Sale to authorized party/ CHWTSDF
59	Myrcene 90 /Myrcene Supra Column Bottom Mass	28.10	TPA	65.74	-65.74	0.00	Product Myrcene 90 /Myrcene deleted	Sale to authorized party/ CHWTSDF
60	L-Limonene Column Tops	28.10	TPA	739.20	-739.20	0.00	Proposed to use for making formulations by blending	Sale to authorized party/ CHWTSDF
61	L-Limonene Column Bottom Mass	28.10	TPA	138.00	-138.00	0.00	Proposed to use for making	Sale to authorized party/ CHWTSDF

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CTO Sr. no.	By-Products	Category	UOM	Existing Quantity (TPA)	Proposed additional Quantity (TPA)	After Change in Product Mix Quantity (TPA)	Remarks	Disposal Method
							formulations by blending	
62	Aldehyde C11 Column Tops	28.10	TPA	21.02	-21.02	0.00	Product Aldehyde C11 deleted	Sale to authorized party/ CHWTSDF
63	Aldehyde C12 Column Bottom Mass	28.10	TPA	80.06	-80.06	0.00	Product Aldehyde C11 deleted	Sale to authorized party/ CHWTSDF
64	Aldehyde C13 Reaction Bottom mass	28.10	TPA	48.24	-48.24	0.00	Product Aldehyde C11 deleted	Sale to authorized party/ CHWTSDF
65	Spent Sulphuric acid	28.10	TPA	1860.00	-1860.00	0.00	Product Beta Ionone (BI) (Beta Ionone Technical /PG) deleted	Sale to authorized party
	TOTAL			17080.81	-12629.78	4202.39		
	E waste	--	Kg/A	360	0.00	360.00	No change	Sale to authorized party
	Lead acid batteries	--	Nos/A	5	0.00	5.00	No change	

- Post change of product mix, overall hazardous waste generation will be reduced by 70%.
- This is due to proposed deletion of several products as listed above, making of new formulations by blending some fractions (as listed in product list). Proposed process changes as stated in 2.2 section of this NIPL certificate. Thus, there is overall reduction in hazardous waste generation.

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Summary of HW Generation Post Change of Product Mix:

Head/ Activity	Existing Qty (As per EC)		After Change in Product Mix		Remarks
	Numbers	Quantity	Numbers	Quantity	
		(MTPA)		(MTPA)	
HW as identified in HOWM Rules 2016 (Sr No. 1- 7 in above Table)	7	4106.64	7	3858	Slight reduction from 4106.64 MTPA to 3858 MTPA due to reduction in manufacturing activities
Column Tops and Bottoms to use for making formulations by blending (Sr Nos 26-27,40-41, 60-61,in above Table)	6	4195.74	0	0.00	Column tops and bottoms having good odors will be blended and sold for use for low profile perfumery applications
By product drained to ETP and separated as ETP/MEE sludge(Sr Nos 22-24,36 in above Table)	3	2005.32	0	0.00	PP unable to find vendors with Rule 9 permission, hence decided to drain these to ETP and the same will be separated with MEE sludge and disposed off to MWML. Include MEE sludge qty in U-III
By products listed under HW schedule deleted since main product mfg will be discontinued (Sr Nos 8-20, 28-35,37-38, 42-59,62-65 In above Table)	45	2,519.59	0	0.00	These will be permanently deleted from consent to operate since the manufacturing activity of the products where these are generated is being discontinued
Reduction in by product quantity due process change (Sr Nos 39 in above Table)	1	322.50	1	314.40	Process improvements have resulted in reduction of by product generation
Reduction in by product quantity due reduction in generation (Sr Nos 25 in above table)	1	637.32	1	29.99	Process improvements have resulted in reduction of by product generation
Total		13787.1		4202.39	

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Technical Committee Deliberations:

The project proposal was discussed based on the presentation made and documents, NIPL Certificate, NIPL proforma submitted by the proponent. Product wise load calculation in terms of wastewater, Air Emissions & Hazardous Waste generations were discussed. Existing Consent to Operate, Environmental Clearance, No Increase in Pollution Load certificate issued by M/s. Aditya Environmental Services Private Limited vide letter dated 08th Feb. 2022 and product-mix proforma are taken on the record.

Committee after due deliberations noticed that:

- The PP has proposed change of product mix by deleting various existing manufactured products & increasing/decreasing tonnage of remaining products. The proposed tonnage reduction of manufactured products is from 7194 MTPA to 6781 MTPA. Thus, marginal reduction in production quantity. Unit has earlier EC and also production is in same category viz Aroma chemicals, thus it is permissible activity for grant of revised consent based on NIPL.
- The PP has proposed addition of new blending products which are mixing of various fractions from the manufactured products processing. The proposed tonnage of blending products is 3984 MTPA &
- The PP has proposed to include one byproduct in CTO & the proposed tonnage is 827 MTPA.
- The PP has proposed to include the Repacking & sale in CTO & the proposed tonnage is 380MTPA
- Post change of product mix, there is marginal reduction of 7 CMD in water consumption & no change in effluent generation
- The effluent is sent to Privi Unit-III for treatment as per existing CTOs of both Unit-I and Unit-III. Unit -III has well equipped ETP. Treated effluent is sent to CETP from Unit-III through the MIDC under drainage system,.
- Post change of product mix, there is no change in stack and air emission as there is no additional stack proposed.
- The hazardous waste generation will reduce from existing 17080 MTPA to 4202 MTPA due to deletion of several products, improvement in process & proposed blending products.

Technical Committee Decision:

1. The Board shall impose consent condition for Repacking activity while granting the consent.
2. Technical Committee decided to **recommend** the case for change in product mix based on "No Increase in Pollution Load" as per the provision of EIA notification 2006 and amendment thereto.

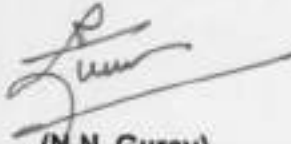


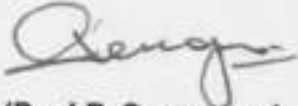
MAHARASHTRA POLLUTION CONTROL BOARD

Agenda item No	Item No. 11
Proposal No.	MPCB-CONSENT-0000154116
Project Details	M/s. Sumitomo Chemical India Ltd, MIDC Tarapur.
NIPL Certificate	NIPL Certificate issued by Ultratech Environmental Consultancy & Laboratory dtd. 18.04.2022
Name of the Industry Representative present	Sh. Ashish Ladu, Safety Incharge

1. As per the EIA notification published by MOEFCC, Delhi no. S.O. 980(E) dtd. 2nd March 2021 Appendix XIII 1.-"The project proponent is required to obtain a certificate of „no increase in the pollution load" from the environmental auditors or reputed institutions, to be empanelled by the State Pollution Control Board or Central Pollution Control Board or Ministry of Environment, Forest and Climate Change."
2. PP has NIPL certificate of "no increase in the pollution load" from the environmental auditor who is not accredited for the said specific sector (Pesticide).
3. Therefore, the case is **rejected** by the committee.

The meeting ended with vote of thanks to the chair.


(N.N. Gurav)
Regional Officer(BMW)
Member Convener


(Dr. J.B. Sangewaar)
Assistant Secretary(Technical)
Chairman of Product Mix
Committee