Minutes of 4th Technical Committee Meeting (2022-2023) 1st Sitting , for certification about "No Increase in Pollution Load" for getting exemption from going through the entire EIA process i.e for assessment of application of under change in Product-Mix.

Date 10th March, 2023
Venue: Hybrid Mode, 4th Floor, Conference Hall, Kalpataru Point, Sion, Mumbai.

Technical Committee Members present for the meeting:

1.	Dr.J.B.Sangewar, Assistant Secretary (Tech), MPCB	Chairman
2.	Dr. V. M. Motghare, Joint Director (APC)	Member
3.	Dr. Y.B. Sontakke, Joint Director (WPC)	Member
4.	Dr.B R. Naidu, Ex Zonal Officer, CPCB	Member
5.	Shri. N. N. Gurav, RO(BMW)	Member convener

At the outset, the request received from the members 1) Scientist-1, Environment department, GoM, 2) Regional Director, CPCB, 3) Representative nominated by director NEERI. 4) Mr. Anurag Garg, Associate Prof IIT, Mumbai and 5) Representative nominated by director NCL Pune for leave of absence from attending the meeting were placed before the committee meeting. The committee considered the same.

Shri.N.N Gurav , RO(BMW)MPCB, Member convener of the Committee, welcomed all the members of the Committee and requested , Dr.J.B.Sangewar, Assistant Secretary (Tech), MPCB & Chairman of the committee to permit proceedings of the meeting to start.

On the basis of request made by the industries, the members thereafter deliberated on the agenda items placed before the committee and following decisions were taken.

Agenda Item No.	**Item No.1**
Proposal No.	MPCB-CONSENT-0000114650
Project Details	**M/s. Crystal Crop Protection ltd.** Address: G 54, MIDC Industrial Area, Butibori, Maharashtra.
NIPL Certificate	NIPL certificate issued by M/s. Anacon laboratories Pvt ltd.

Introduction: This has reference to the online proposal submitted vide No. IA/MH/IND2/70618/2017along with the copies of documents seeking amendment in existing consent to operate under change in product-mix under the provision of EIA Notification 2006 amended on 06.10.2022.

Exiting Clearances:

1. Environmental Clearance is granted to the industry vide IA-J-11011/526/2017-IA-II(I); dated 05.04.2019.
2. Consent to Operate granted vide no. Format1.0/BO/AST/UAN NO. 0000076963/O/CC-1911000582; dated 15/11/2019. The validity of the existing consent is up to 31/10/2024.
3. Company has applied for amendment in existing CTO for hazardous waste vides UAN No. MPCB-CONSENT_AMMENDMENT-0000008897; dated 02.07.2022.

Project details:

A. Production Details;

Production Details: Sr. No.	Product Name	Existing Quantity (MT/A)	Proposed Quantity (MT/A)	Total Quantity (MT/A)	Remarks
A	**FUNGICIDE**				
1	Metiram Technical	850	-350	500	Reduced
2	Cymoxanil Technical	105	-105	0	Reduced
3	Propiconazole Technical	50	+150	200	Increased
4	Hexaconazole Technical	315	-265	50	Reduced
5	Tricyclazole Technical	420	-270	150	Reduced
6	Tebuconazole Technical	300	-100	200	Reduced
7	Azoxystrobin Technical	125	+75	200	Increased
8	Pyraclostrobin Technical	5	+15	20	Increased
9	Picoxystrobin Technical	105	-5	100	Reduced
10	Mandipropamid Technical	100	-50	50	Reduced
11	Epoxyconazole Technical	330	-280	50	Reduced
12	Bixafen Technical	30	-5	25	Reduced
13	Fluopyram Technical	50	-25	25	Reduced
14	Fluoxastrobin Technical	30	-30	0	Reduced
15	Fluxapyroxad Technical	50	0	50	No change
16	Prothiaconazole Technical	0	+200	200	Newly added
17	Difenoconazole Technical	0	+50	50	Newly added
B	**INSECTICIDE**				
18	Clothianidine	50	0	50	No change
19	Flonicamide Technical	105	+95	200	Increased
20	Imidacloprid Technical	400	-350	50	Reduced
21	Thiamethoxam Technical	480	+1020	1500	Increased

22	Acetamiprid Technical	180	-130	50	Reduced
23	Pyridaben Technical	50	+50	100	Increased
24	Chlorantraniliprole Technical	100	0	100	No change
25	Spirotetramat Technical	30	-30	0	Reduced
26	Sulfoxaflor Technical	50	-50	0	Reduced
27	Dinetofuron	100	-70	30	Reduced
28	Flubendamide	100	-100	0	Reduced
29	Lambda Cyhalothrin Technical	400	-350	50	Reduced
30	Cypermethrin Technical	250	-230	20	Reduced
31	Bifenthrin Technical	250	-200	50	Reduced
32	Thiachloprid Technical	0	+20	20	Newly added
33	Pymetrozine Technical	0	+200	200	Newly added
34	Chlorpyrifos 98% Technical	0	+50	50	Newly added
C	**HERBICIDE**				
35	Pyrazosulfuron Technical	20	+30	50	Increased
36	Tembotrione Technical	50	-50	0	Reduced
37	Penoxsulam Technical	30	-10	20	Reduced
38	Quizalofop Ethyl Technical	80	+20	100	Increased
39	Oxadiazon Technical	25	-25	0	Reduced
40	Clodinofop Propargyl Technical	100	0	100	No change
41	Metamifop Technical	50	-50	0	Reduced
42	Saflufenacil Technical	30	-30	0	Reduced
43	Bentazone Technical	360	-260	100	Reduced
44	Clomazone Technical	450	-350	100	Reduced
45	Sulfentrazone Technical	135	-135	0	Reduced
46	Propaquizafop Technical	100	-20	80	Reduced
47	Topramezone Technical	0	50	50	Newly added
48	Clethodim Technical	0	100	100	Newly added
D	**INTERMEDIATE**				
49.	Sodium Cyno Dithio formate Technical	0	+1250	1250	Newly added

50.	Cloquintocet-Mexyl Technical	0	+50	50	Newly added
51.	Dimethomorph (TCMSC) Technical	0	+500	500	Newly added
	Total	**6840**	**0**	**6840**	
	Note : Old Product quantity = 4370 TPA and Newly added product quantity = 2470 TPA				

There is no change in annual production capacity as per existing EC (6870 TPA) and CTO (6840 TPA). MPCB has not granted CTO for the manufacturing of BENZOVINDIFLUPYR TECHNICAL (30 MT/A) pesticide product. Thus, overall production capacities of existing plant will remain unchanged before and after the proposed change. The overall total production quantity will not exceed 6840 TPA.

B. Pollution load Details:

(i) Water & Wastewater Aspect;

Before Product Mix;

Sr. No.	Particular	Quantity in CMD	Effluent Segregation in CMD		COD (Strong)		COD (Weak)		TDS (Strong)		TDS (Weak)	
			Strong	Weak	mg/l	Kg/day	mg/l	Kg/day	mg/l	Kg/day	mg/l	Kg/day
1	Water Consumption	229.50	Not applicable									
2	**Trade Effluent Generation**											
A	Process Activity	25	16.4	8.6	18100	296.84	1340	11.52	13200	216.48	--	--
B	Cooling Tower & Boiler	16	--	16	--	--	980	15.68	--	--	2220	35.52
C	**Total**	**41**	**16.4**	**24.6**	**18100**	**296.84**	**2320**	**27.2**	**13200**	**216.48**	**2220**	**35.52**
3	Domestic Effluent Generation, CMD	15	---	15	---	---	700	10.5	--	---	500	7.5

After Product Mix:

Sr. No.	Particular	Quantity in CMD	Effluent Segregation in CMD		COD (Strong)		COD (Weak)		TDS (Strong)		TDS (Weak)	
			Strong	Weak	mg/l	Kg/day	mg/l	Kg/day	mg/l	Kg/day	mg/l	Kg/day
1	Water Consumption	229.5	Not applicable									
2	**Trade Effluent Generation**											
A	Process Activity	25	16.1	8.9	18500	297	1310	11.65	13180	212.19	--	--
B	Cooling Tower & Boiler	16	--	16	--	--	980	15.68	--	--	2220	35.52
C	**Total**	**41**	**16.1**	**24.9**	**18500**	**297**	**2290**	**27.33**	**13200**	**212.19**	**2220**	**35.52**
3	Domestic Effluent Generation, CMD	15	---	15	---	---	700	10.5	--	---	500	7.5

- Water Consumption will remain same 229.5 CMD
- Hydraulic Load will remain same 41 CMD
- COD load of trade effluent will remain same 297 Kg/day
- TDS load for trade effluent will remain same 213 Kg/day

There is no change in process & technology before and after proposed changes. Therefore, No additional wastewater will be generated before and after proposed change in product mix. Thus, the trade effluent generations as per valid CTO issued is 41 CMD, remains unchanged before and after the change in product mix. Zero Liquid Discharge (ZLD) is being/ will be maintained by reuse the recycle water in process and cooling tower.

Treatment System

a) **Trade Effluent:**
Provided ETP (Capacity_100 KLD)

b) **Domestic Effluent: Provided** STP (Capacity_15 KLD)

(ii) Air Emission Load;

Sl. No.	Stack attached to	APC System	Height in Meters	Stack Diameter In MM	Type of Fuel	Quantity & UoM Before Product Mix	Quantity & UoM After Product Mix	Any change after desired product quantity
1	Boiler 5 TPH	Cyclone Separator for Dust collection, Bag Filter	30	800	Biomass Briquette	6000 Kg/hr	6000 Kg/hr	No Change
2	Thermopack	stack	30	450	LDO	15 lit/hr	15 lit /hr	No Change
2	DG Set 180 kVA	Acoustic enclosure	3	120	HSD	28 Kg/hr	28 Kg/hr	No Change
3	DG Set 750 kVA	Acoustic enclosure	6	200	HSD	80 Kg/hr	80 Kg/hr	No Change
Process Reactor								
4	Process Stack	Packed column Scrubber	12	150	-	-	-	No Change

(iii) Hazardous Waste Load

Sl. No.	Hazardous Waste Type	Category (As per schedule under hazardous & other waste management Rules, 2016)	Maximum Quantity Before Change in product mix. (MT/D)	Maximum Quantity After Change in product mix. (MT/D)
1.	ETP Sludge	35.3	0.3	0.3

Sl. No.	Hazardous Waste Type	Source of Generation	Mode of Storage	Mode of Treatment Method	Mode of Disposal method	Action
1.	ETP Sludge	ETP	Stored in dedicated area	Landfill	CHWTSDF	No change

- As per existing EC number - IA-J-11011/526/2017-IA-II(I); dated 05.04.2019, Condition No. 10 (XII)- Process organic residue and spent carbon, if any, shall be sent to cement industries, ETP sludge, process inorganic & evaporation salt shall be disposed off to TSDF.
- EIA report page no. 48 following hazardous categories given to add but not added in CTO hence separate application was done on CTO Amendment Application dated 02.07.2022 vide application UAN number MPCB-CONSENT_AMMENDMENT-0000008897; dtd. 02.07.2022.

Sr.No	Haz.waste	Cat	Haz.waste	Before product Mix MT/day	After Product mix	
1.	Process wastes or residues	29.1	Process wastes or residues	-	1.0	TSDF/pre-processing/co-processing
2.	Residue from Distillation	29.1	Residue from Distillation	-	0.5	TSDF/pre-processing/co-processing
3.	Sludge from ATFD ETP	35.3	Sludge from ATFD ETP	-	0.5	TSDF/pre-processing/co-processing
4.	Sludge from STP	35.3	Sludge from STP	-	0.05	TSDF/pre-processing/co-processing

Technical Committee Deliberations:

The proposed project was discussed on the basis of documents – NIPL Certificate and presentation made by the industry. Product wise load calculation in terms of Wastewater, Air emissions & Hazardous waste generation was discussed. Existing Consent to Operate, Environmental Clearance, NIPL Certificate issued by M/s. Anacon laboratories Pvt ltd and Product – Mix Proforma are taken on the record.

After due deliberations, Committee noticed that:

i. Industry has applied for Change in Product Mix with no increase in the pollution load.

ii. There is no change in annual production capacity as per existing EC (6870 TPA) and CTO (6840 TPA). MPCB has not granted CTO for the manufacturing of BENZOVINDIFLUPYR TECHNICAL (30 MT/A) pesticide product. Thus, overall production capacities of existing plant will remain unchanged before and after the proposed change. The overall total production quantity will not exceed 6840 TPA.

iii. There is no change in process & technology before and after proposed changes. Therefore, No additional wastewater will be generated before and after proposed change in product mix. Thus, the trade effluent generations as per valid CTO issued is 41 CMD, remains unchanged before and after the change in product mix. Zero Liquid Discharge (ZLD) is being/ will be maintained by reuse the recycle water in process and cooling tower.

iv. As per existing EC number - IA-J-11011/526/2017-IA-II(I); dated 05.04.2019, Condition No. 10 (XII)- Process organic residue and spent carbon, if any, shall be sent to cement industries, ETP sludge, process inorganic & evaporation salt shall be disposed off to TSDF.

v. The PP has presented the EIA report submitted to SEIAA wherein, on page no. 48 hazardous quantities and categories were mentioned however in the EC the hazardous waste quantity has not mentioned. While applying for CTE & CTO inadvertently it was not mentioned therefore it was not reflected in the consent, now they have applied with the corrected categories and quantities. Hence it seems that, there is no increase in hazardous waste.

Technical Committee Decision:

Technical Committee decided to recommend the case for change in product under product mix with a compliance of the following conditions.

(i) Industry shall comply with all the conditions stipulated in Environmental Clearance and ensure display/upload of six-monthly compliance monitoring report on their official website.

(ii) Industry should not manufacture any other product for which permission is not granted by the Board.

(iii) Industry shall ensure connectivity of OCEMS to Board server.

Agenda Item No.	**Item No.2**
Proposal No.	MPCB-CONSENT-0000138247
Project Details	**M/s. Astec Lifesciences Ltd.** Address: Plot No. K-2/1/1, Additional MIDC Area, Mahad, Dist Raigad, Maharashtra.
NIPL Certificate	NIPL certificate issued by M/s. Sadekar Enviro Engineers Pvt. Ltd.

Introduction:

This has reference to the online proposal submitted vide No. MPCB-CONSENT-0000138247 along with the copies of documents seeking amendment in existing consent to operate under change in product-mix under the provision of EIA Notification 2006 as amended on 23/11/2016 & 02/03/2021.

Exiting Clearances:

1. Environmental Clearance is granted to the industry vide J-11011/111/2011-IA-11(I) dated 22.03.2013.
2. Consent to Operate granted vide no. 1.0/BO/AST/UAN No. 0000074199/0/CC-1908000498 dated 19/08/2019. The validity of the existing consent is up to 31/7/2022.
3. Company has applied for change in product mix along with the renewal of CTO to the Board vide no MPCB-CONSENT-0000138247 dated 03.05.2022.

Project details:

A. Production Details:

Sr. No.	Product Name	Existing Quantity (MT/M)	Proposed Quantity (MT/M)	Total Quantity (MT/M)	Remarks
1	4-BAT	0	2	2	Newly added
2	Diniconazole	0	2	2	Newly added
3	Uniconazole	0	2	2	Newly added
4	Mapiquat	0	1	1	Newly added
5	Silthiofam	0	2	2	Newly added
6	MXL-M	0	5	5	Newly added
7	Transfluthrin	25	16	41	Increased
8	Tebuconazole	120	40	160	Increased
9	Propiconazole	120	-70	50	Reduced
10	Dichlorophenyl oxirane	18	0	18	No change

11	3 -Aminotriazole	20	0	20	No change
12	Siduron	20	0	20	No change
13	2-Ethyl 2-methyl butanoic acid	25	0	25	No change
14	Metalaxyl	20	0	20	No change
15	Simeconazole	20	0	20	No change
16	Cyproconazole	20	0	20	No change
17	Imazethapyr (IMZPR)	35	0	35	No change
18	DTX, Dextrinol	5	0	5	No change
19	Imibenconazole	10	0	10	No change
20	Difenoconazole (CCPV)	40	0	40	No change
21	F69 (2-(2,4-diflurophenyl)-1-(1H-1,2,4 triazol-1-yl)-3-(trimethylsilyl) propan 2-ol)	5	0	5	No change
	Total	**503**	**0**	**503**	

The overall production quantity will remain same. Maximum 21 Nos. of products shall be manufactured at any given point of time. The overall total production quantity will not exceed 503 MT/M.

B. Pollution load Details:

(i) Water & Wastewater Aspect;

Before Product Mix;

Sr. No.	Particular	Quantity in CMD	Effluent Segregation in CMD		COD (Strong)		COD (Weak)		TDS (Strong)		TDS (Weak)	
			Strong	Weak	mg/l	Kg/day	mg/l	Kg/day	mg/l	Kg/day	mg/l	Kg/day
1	Water Consumption	307	Not applicable									
2	**Trade Effluent Generation**											
A	Process Activity	53	76.5	--	11320	866.5	--	--	101580	7771.1	--	--
B	Cooling Tower & Boiler	234	--	33.5	--	--	2800	93.8	--	--	900	30.15

C	**Total**	**287**	**76.5**	**33.5**	--	**866.5**		**93.8**	--	**7771.1**		**30.15**
3	Domestic Effluent Generation, CMD	20	---	15	---	---	700	10.5	--	---	500	7.5

After Product Mix;

Sr. No.	Particular	Quantity in CMD	Effluent Segregation in CMD		COD (Strong)		COD (Weak)		TDS (Strong)		TDS (Weak)	
			Strong	Weak	mg/l	Kg/day	mg/l	Kg/day	mg/l	Kg/day	mg/l	Kg/day
1	Water Consumption	307	Not applicable									
2	**Trade Effluent Generation**											
A	Process Activity	53	76.1	--	11300	866	--	--	97000	7386	--	--
B	Cooling Tower & Boiler	234	--	33.5	--	--	2800	93.8	--	--	900	30.15
C	**Total**	**287**	**76.1**	**33.5**		**866**		**93.8**	--	**7386**		**30.15**
3	Domestic Effluent Generation, CMD	20	---	15	---	---	700	10.5	--	---	500	7.5

- Water Consumption will remain same 307 CMD
- Hydraulic Load will reduce to 109.6 CMD
- COD load for trade effluent will reduce by 0.5 Kg/day
- TDS load for trade effluent will reduce by 385 Kg/day

Treatment System

Trade Effluent:

Industry has segregated trade effluent into weak stream & strong stream and provided Effluent Treatment Plant (ETP) comprising of;

i) **Strong COD/TDS stream of 76.1 CMD:** Treatment system comprising of collection tank neutralization, stripper, In-plant evaporation system, Multiple effect Evaporator, ATFD. The distillate is recycled to process.

ii) **Weak COD/TDS stream of 33.5 CMD:** Treatment system comprising of collection tank and psychometric evaporator.

Domestic Effluent: The domestic effluent is treated in sewage treatment plant of capacity 20 CMD.

(ii) Air Emission Load;

Sr. No.	Source	Fuel	Before Product Mix	After Product Mix	Remark
1	Boiler- 6 TPH	Coal	22 MT/D	22 MT/D	No change
2	Thermic Fluid Heater 15 Lac Kcal/Hr				
3	DG Set- 500 KVA & 250 KVA	HSD	1000 Lit/Hr	1000 Lit/Hr	No change

(iii) Hazardous Waste Load;

Sr. No.	Description	Category No.	UOM	Before Product Mix	After Product mix	Remark
1	Used or spent oil	5.1	Lit/M	50	50	No change
2	Residue & Wastes	29.1	MT/M	50	50	No change
3	Chemical sludge residue containing pesticide	29.2	MT/M	18	15	Reduced
4	Discarded containers	33.1	Nos./M	1245	1245	No change
5	Filter & filter material having organic liquid	36.2	Kg/M	50	50	No change
6	Spent carbon	36.2	MT/M	2.5	2.5	No change
7	Concentration or evaporation residues	37.3	MT/M	5	5	No change
8	Inorganic Salts K/Na/Zn of Sulphate, Phosphate, Chloride, Bromide	29.1	MT/M	146	146	No change
9	Mg Salts (Sulphate/Chloride/Carbonate)	29.1	MT/M	142.5	142.2	Reduced
10	Aliphatic Hydrocarbon	29.1	MT/M	20	20	No change
11	Hydrochloric acid	29.1	MT/M	6	6	No change

Out of 11 nos. of category of Hazardous wastes, 9 nos. of category of HW remains unchanged and quantity of 2 category waste will be reduced.

Technical Committee Deliberations:

The proposed project was discussed on the basis of documents – NIPL Certificate and power point presentation made by the industry. Product wise load calculation in terms of Wastewater, Air emissions & Hazardous waste generation was discussed. Existing Consent to Operate, Environmental Clearance, NIPL Certificate issued by M/s. Sadekar Enviro Engineers Pvt. Ltd. and Product – Mix Proforma are taken on the record.

After due deliberations, Committee noticed that:

i. Industry has applied for Change in Product Mix with no increase in the production quantity. The total production quantity will be remaining same after product mix i.e. 503 MT/ M.
ii. The water consumption, trade effluent generation will remain same after product mix.
iii. COD load will reduce by 0.5 Kg/day and TDS load will reduce by 385 Kg/day
iv. Committee noticed that, industry have segregated effluent into strong and weak stream and not provided separate treatment for segregated trade effluent.
v. The overall hazardous waste quantity after product mix will remain same.
vi. The by-products generated which shall be shifted to Hazardous Waste and dispose as per the provision of H&OW Rule and PP agreed for the same.
vii. The overall pollution load is not increased after change in product – mix.

Technical Committee Decision:

Technical Committee decided to recommend the case for change in product under product mix with a compliance of the following conditions.

(i) Industry shall comply with all the conditions stipulated in Environmental Clearance and ensure display/upload of six-monthly compliance monitoring report on their official website.
(ii) Industry should not manufacture any other product for which permission is not granted by the Board.
(iii) Industry shall ensure connectivity of OCEMS to Board server.

Agenda Item No.	**Item No.3**
Proposal No.	MPCB-CONSENT-0000138688
Project Details	**M/s. Atul Bioscience ltd.** Address: Plot no N-37, MIDC Anandnagar, Additional Ambarnath, Industrial Area, Tal Ambarnath, Dist. Thane Maharashtra.
NIPL Certificate	NIPL certificate issued by Institute of Chemical Technology, Matunga, Mumbai-400019

Introduction:

This has reference to the online proposal submitted vide No. MPCB-CONSENT-0000138688 along with the copies of documents seeking amendment in existing consent to operate under change in product-mix under the provision of EIA Notification 2006 amended on 02.03.2021.

Exiting Clearances:

1. Environmental Clearance is granted to the industry by SEIAA vide No. SIA/MH/IND2/152225/2020 dated 26.06.2020.
2. 1st Consent to Operate (Expansion) granted with change in product mix with renewal of existing consent to operate obtained vide no. Format 1.0/CC/UAN No. 0000099414/CO-2107000147, Date: 02.07.2021 valid upto 31.12.2025

Project details:

A. Production Details:

S. No	Name of the products, Unit	Existing, MTA	Proposed, MTA	Total, MTA	Remarks
1	(1R)-2-{[2-(4-aminophenyl)ethyl]amino}-1-phenylethanol Hydrochloride	22	0	22	No change
2	(1R)-2-{[2-(4-nitrophenyl)ethyl]amino}-1-phenylethanol Hydrochloride	25.74	0	25.74	No change
3	(2R)-2-hydroxy-N-[2-(4-nitrophenyl)ethyl]-2-phenylethanamide	26.51	0	26.51	No change
4	(S) - Metoprolol Succinate	10	-5	5	Reduced
5	(S)-1-(2-Chloroacetyl)pyrrolidine-2-carbonitrile (CACP)	62.62	0	62.62	No change
6	(S)-Metoprolol Base	9.61	0	9.61	No change
7	1-(4-methoxyphenyl)-propan-2-one	36.72	0	36.72	No change

S. No	Name of the products, Unit	Existing, MTA	Proposed, MTA	Total, MTA	Remarks
8	2-(acetylamino)-9-{[2-(acetyloxy)ethoxy]methyl}-9H-purin-6-yl acetate	238.5	0	238.5	No change
9	3,4-dimethoxy-benzoic acid	31.02	0	31.02	No change
10	3,4-dimethoxy-benzoic acid-4-bromo-butulylester	51.75	0	51.75	No change
11	Acyclovir	150	-100	50	Reduced
12	Atazanavir	50	-50	0	Reduced
13	Benzyl chloride	250	-250	0	Reduced
14	Carvidilol	25	-25	0	Reduced
15	CBZ-L-Valine	157.95	-132.95	25	Reduced
16	CBZ-Valacyclovir	202.5	-152.5	50	Reduced
17	Chlorobutanol	50	-25	25	Reduced
18	CLVM	360	-360	0	Reduced
19	Dapsone	40	-40	0	Reduced
20	DCHU	150	0	150	No change
21	Desvenlafaxine	25	10	35	Increased
22	Ethyl-[2-(-methoxy-phenyl)-1-methylethyl]amine	31.5	0	31.5	No change
23	Fluconazole	75	25	100	Increased
24	Fluconazole Crude (FCZ-III)	86.47	35.53	122	Increased
25	Guanine diacetate	200.34	0	200.34	No change
26	L-PBE. HCl.	200	-140	60	Reduced
27	L-Prolinamide	62.62	0	62.62	No change
28	Losartan Potassium	60	40	100	Increased
29	Losartan-I	60	0	60	No change
30	Losartan-II	60	0	60	No change
31	Mebeverine	75	0	75	No change
32	Metoprolol Base	112.94	0	112.94	No change
33	Metoprolol Epoxide	96.78	0	96.78	No change

S. No	Name of the products, Unit	Existing, MTA	Proposed, MTA	Total, MTA	Remarks
34	Metoprolol Succinate	50	0	50	No change
35	Metoprolol Tartrate	80	-30	50	Reduced
36	Mirabegron	25	-15	10	Reduced
37	Nebivolol HCL	25	-25	0	Reduced
38	Quetiapine Fumerate	75	-75	0	Reduced
39	Ritonavir	50	10	60	Increased
40	Sodium veratroate	39.17	0	39.17	No change
41	Tert.butyl N[(1S,3S,4S)-1-benzyl-4-amino-3 hydroxy-5- phenyl pentyl]carbamate	35	0	35	No change
42	Thiazol-5-yl-methyl N[(1S,3S,4S)-1-benzyl-4-amino-2 hydroxy-5- phenyl pentyl]carbamate	35	0	35	No change
43	TMSI	70	-20	50	Reduced
44	Topiramate HCL	50	-50	0	Reduced
45	Valacyclovir hydrochloride	150	-25	125	Reduced
46	Venlafaxine Acetate	154.5	0	154.5	No change
47	Venlafaxine Hydrochloride	150	-50	100	Reduced
48	Veratraldehyde	29.53	0	29.53	No change
49	Vildagliptin	75	-55	20	Reduced
50	1-BOC PIPERAZINE	0	10	10	Newly added
51	1-Chloroethyl methyl carbonate (1-CEMC)	0	100	100	Newly added
52	10-Methoxy Iminostilbene	0	100	100	Newly added
53	2,2'-DITHIOBISBENZOTHIAZOLE DISULPHIDE	0	25	25	Newly added
54	ATAA.HCl	0	10	10	Newly added
55	BDH Salt	0	10	10	Newly added
56	Boc-L-Proline	0	5	5	Newly added
57	Boc-L-Valine	0	5	5	Newly added
58	BPBH	0	5	5	Newly added

S. No	Name of the products, Unit	Existing, MTA	Proposed, MTA	Total, MTA	Remarks
59	CLBL Anhydrous	0	1	1	Newly added
60	CLVM HCl	0	120	120	Newly added
61	CLVM Oxalate	0	120	120	Newly added
62	DFTA	0	75	75	Newly added
63	EDP	0	100	100	Newly added
64	FCZ-III aqueous layer	0	600	600	Newly added
65	ITVM	0	25	25	Newly added
66	MAEM	0	100	100	Newly added
67	MAEM ESTER	0	68	68	Newly added
68	MAEM ESTER Stage-1	0	158	158	Newly added
69	MAEM ESTER Stage-2	0	188	188	Newly added
70	MAEM ESTER Stage-3	0	98	98	Newly added
71	METHOXYAMINE. HYDROCHLORIDE (MA. HCl)	0	25	25	Newly added
72	MICA ESTER	0	75	75	Newly added
73	MICA ESTER- Step-1	0	45	45	Newly added
74	MICA ESTER- Step-2	0	60	60	Newly added
75	MICA ESTER- Step-3	0	100	100	Newly added
76	Moc-L-Valine	0	5	5	Newly added
77	N-BOC-4-Piperidone	0	10	10	Newly added
78	NEED	0	100	100	Newly added
79	NPEA HCL	0	10	10	Newly added
80	NPTC	0	10	10	Newly added
81	SMIA	0	100	100	Newly added
82	SMIA -stage 1	0	45	45	Newly added
83	SMIA -stage 2	0	45	45	Newly added
84	SUCCINATE SALT STAGE 5	0	10	10	Newly added
85	TBC	0	25	25	Newly added

S. No	Name of the products, Unit	Existing, MTA	Proposed, MTA	Total, MTA	Remarks
86	TMU	0	5	5	Newly added
87	VALSARTAN	0	120	120	Newly added
88	VALSARTAN Stage-1	0	120	120	Newly added
89	VALSARTAN Stage-2	0	120	120	Newly added
90	Venla free base	0	25	25	Newly added
		4188.77	**1473.08**	**5661.85**	

The overall production quantity will increase from 4189 MTA to 5662 MTA.

B. Pollution load Details:

i) Water & Wastewater Aspect

Before Product Mix

Sr. No.	Particular	Quantity in CMD	Effluent Segregation in CMD		COD (Strong)		COD (Weak)		TDS (Strong)		TDS (Weak)	
			Strong	Weak	mg/l	Kg/day	mg/l	Kg/day	mg/l	Kg/day	mg/l	Kg/day
1	Water Consumption	275	Not applicable									
2	**Trade Effluent Generation**											
A	Process Activity	60	10	67	15000	150	4474	299.75	2710	181.57	2850	190
B	Cooling Tower & Boiler	185	0	15	--	--	300	4.5	--	--	700	10.5
C	**Total**	**245**	**10**	**82**	--	**150**	--	**304.25**	--	**181.57**	--	**200.5**
3	Domestic Effluent Generation, CMD	30	0	22	--	--	700	15.4	--	--	500	11

After Product Mix:

Sr. No.	Particular	Quantity in CMD	Effluent Segregation in CMD		COD (Strong)		COD (Weak)		TDS (Strong)		TDS (Weak)	
			Strong	Weak	mg/l	Kg/day	mg/l	Kg/day	mg/l	Kg/day	mg/l	Kg/day
1	Water Consumption	272	Not applicable									
2	**Trade Effluent Generation**											
A	Process Activity	57	9.5	64.5	14800	139.65	4340	279.93	2400	154.8	3350	216.07
B	Cooling Tower & Boiler	185	--	15	--	--	300	4.5	--	--	700	10.5
C	**Total**	**242**	**9.5**	**79.5**	**--**	**139.65**	**--**	**284.43**	**--**	**154.8**	**--**	**226.57**
3	Domestic Effluent Generation, CMD	30	0	22	--	--	700	15.4	--	--	500	11

- Water Consumption will reduce from 275 CMD to 272 CMD
- Effluent generation will reduce from 114 CMD to 111 CMD
- COD load for trade effluent will reduce from 454.25 Kg/day to 424.08 Kg/day
- TDS load for trade effluent will reduce from 382.07 Kg/day to 381.37 Kg/day

Treatment System

a) **Trade Effluent:**

Industry has segregated trade effluent into weak stream & strong stream and provided Effluent Treatment Plant (ETP) comprising of:

- **Strong COD/TDS stream of 9 CMD:** Treatment system comprising of collection tank neutralization, stripper, In-Plant Evaporation System, Multiple Effect Evaporator, ATFD. The distillate is recycled to process.
- **Weak COD/TDS stream of 65 CMD:** Treatment system comprising of collection tank and psychometric evaporator.

b) **Domestic Effluent:**

The domestic effluent is treated in sewage treatment plant of capacity 22 CMD.

ii) **Air Emission Load**

Sr. No.	Source	Fuel	Before Product Mix	After Product Mix	Remark
1	Boiler-1 (3TPH)	Coal	400 kg/hr	400 kg/hr	No change
2	Boiler-2 (0.85 TPH)	FO	40 kg/hr	40 kg/hr	No change
	Boiler-3 (0.85 TPH)	FO	40 kg/hr	40 kg/hr	No change
	Boiler-4 (0.65 TPH)	FO	30 kg/hr	30 kg/hr	No change
3	DG set (500 KVA)	HSD	70 Lits/hr	70 Lits/hr	No change
4	DG set (125 KVA)	HSD	40 Lits/hr	40 Lits/hr	No change
5	Process Vent-1	--			No change
6	Process Vent-2	--			No change
7	Process Vent-3	--			No change

iii) **Hazardous Waste Load**

Sr. No.	Description	Category No.	UOM	Before Product Mix	After Product mix	Remark
1	Any Process or distillation residue	36.1	MT/A	1137.6	1340	Increased
2	Spent Carbon	28.3	MT/A	97	120	Increased
3	Spent Catalyst	28.2	MT/A	83	58	Decreased
4	Process Residue and waste	28.1	MT/A	185	285	Increased
5	Chemical sludge from wastewater treatment	35.3	MT/A	408	408	No change
6	Used or spent oil	5.1	MT/A	5	5	No change
7	Date expired products	28.5	MT/A	5	5	No change

8	Empty barrels/ containers/ liners/ contaminated with hazardous chemicals/ wastes	33.1	MT/A	12	12	No change
9	Spent solvents	28.6	MT/A	38912	38221	Decreased
10	Waste or residues containing oil	5.2	MT/A	12	12	No change
				40856.6	**40466**	

Technical Committee Deliberations:

The proposed project was discussed on the basis of documents – NIPL Certificate and presentation made by the industry. Product wise load calculation in terms of Wastewater, Air emissions & Hazardous waste generation was discussed. Existing Consent to Operate, Environmental Clearance, NIPL Certificate issued by Institute of Chemical Technology, Matunga, Mumbai- 400019 and Product – Mix Proforma are taken on the record.

After due deliberations, Committee noticed that:

i. Industry has applied for Change in Product Mix with no increase in the pollution load. The total production quantity will increase 4189.0 TPA to 5662 TPA (35.16% above existing capacity)
ii. The water consumption decreased from 275 KLD to 272 KLD and effluent generation decreased from 114 KLD to 111 KLD after product mix.
iii. COD load for process effluent will decrease from 449.76 Kg/day to 419.74 Kg/day and TDS load will decrease from 371.76 Kg/day to 370.94 Kg/day
iv. Committee noticed that, industry is ZLD unit.
v. The overall hazardous waste quantity after product mix will decrease from **40856.6** MTA to **40466** MTA
vi. Hazardous waste details showing specific hazardous waste quantities are increasing for
   - Any Process or distillation residue: 1137.6 MTA to 1340 MTA
   - Spent Carbon: 97 MTA to 120 MTA
   - Process Residue and waste: 185 MTA to 285 MTA

Technical Committee Decision:

Technical Committee decided that, the hazardous waste quantity to be reviewed and resubmit the case in the next meeting.

Agenda Item No.	**Item No.4**
Proposal No.	MPCB-CONSENT-0000132386.
Project Details	M/s. Aarti Pharmalab Ltd. (APL)-(SPACK Division), (formerly known as Aarti Industries limited)-(SPACK Division), Plot No. D-18 MIDC Tarapur, Tal & Dist. Palghar.
NIPL Certificate	NIPL Certificate issued by M/s. Aditya Environmental Services Private Limited vide No. AESPL/22-23/Arti/R-01 letter dated 04/03/2023

Introduction:

This has reference to the online proposal submitted the aforesaid industry vide No. MPCB-CONSENT-0000132386 along with the copies of documents seeking amendment in existing consent to operate under change in product-mix under the provision of EIA Notification 2006 as amended on 23/11/2016 & 02/03/2021.

Exiting Clearances:

1. EC was granted to M/s.Aarti Industries Ltd by SEIAA-EC-0000000258 dt 26-04-2018 valid upto April 25, 2025
2. Consent to operate granted to M/s.Aarti Industries Ltd by MPCB vide No. Format 1.0/AS(T) /UAN No. 0000124079/CR/2204001256 19/04/2022 valid upto 31.12.2024
3. Amendment for Consent to Operate by MPCB vide No. Format 1.0/AS(T)/UAN No. 0000009443 /AMEND/2211000021 dt 10/11/2022 valid up to 31.12.2024 transferred on Arti Pharmalabs Ltd (unit VI) .

The existing product quantities as per EC and as per CTO granted by MPCB are as below :

Sr.N.	Product	EC Quantity (MTPM) (*)	Existing CTO(#) quantity (MTPM)
1	Sulphuric acid/ Oleum 25%/ Oleum 65%/ Liquid SO3 (Sulphuric anhydride)	6000	6000
2	**Di Methyl Sulphate (DMS)**	**2000**	**2500**
3	**Di Ethyl Sulphate (DES)**	**1200**	**700**
4	Di Methyl Urea (DMU)	600	600

5	Monomethyl Urea (MMU)	100	100
6	Sodium Vinyl Sulphonate (SVS)	300	300
7	**Cyano Acetic Acid (CAA)**	**500**	**250**
8	**Cyano Acetyl Methyl Urea (CAMU)**	**300**	**50**
9	Nitrosourasil	300	300
10	**Di Methyl Aniline**	**18**	**518**
	Total	**11318**	**11318**
11	Captive power plant (KW)	500	500

Thus, it is seen that overall production is within the EC sanctioned limit. Aforesaid industry had opted for Change in Product Mix earlier which was approved by Committee on 31.07.21 and CTO granted on 25th Nov 21- thus some product quantities differ from EC quantities.

This case of Change of Product Mix with No Increase in Pollution Load was considered in 2nd Technical meeting dt 25.08.22 where the project was deferred by Committee. The Minutes of 2nd Technical Committee meeting are as below:

- PP has proposed to switch the manufacturing process of product CAA from distillation of crude to manufacturing from raw material. However, the presentation was lacking in the proposed new plant and machinery along with the proposed pollution control system
- The industry has proposed to manufacture CAA from an increase in quantity instead of the existing process of distillation of crude and there will be an increase in pollution load. The presentation and NIPL certificate is lacking with respect to the same.
- The NIPL is calculated for the manufacturing CAA from 250 MT/M to 500 MT/M. However, the PP has proposed to change the manufacturing process of CAA from distillation of crude to manufacturing using raw material. Therefore, the NIPL should be in accordance with the manufacture of CAA for a total 500 MT/M and presentation is lacking for this.
- The presentation was lacking with respect to present effluent characteristics and proposed effluent characteristics due to change in manufacturing process
- The presentation was lacking with respect to the present emissions and proposed emissions along with comparison in pollution load due to changing manufacturing process.
- Proposal was deferred on above account

Changes in Proposal by aforesaid industry:

Originally, the unit had proposed: Manufacturing of CAA from starting raw material (instead of distillation of impure CAA)+ new product PHE (25 TPM) with reduction of Nitroso uracil from 300 TPM to 25 TPM.

The aforesaid industry now intends to propose the following changes in their proposal for Change of Product Mix :

Chemical Name	Existing Qty (MTPM)	Earlier Proposal for product mix (as submitted to MPCB) (MTPM)	Proposed Qty now (MTPM)	Remarks
Nitroso Urasil	300	25	0	Product to be discontinued
Phenylephrine (PHE-II)	0	25	0	Not to be taken up at this site

Hence, industry re-submitted computations based on above and have submitted Fresh NIPL Certificate

Project Details:

Aforesaid industry manufactures Etophylline, Theophylline at its neighbouring unit. CAA is vital raw material for both these lifesaving drugs. Currently, APL is importing crude CAA & purifying to desired concentration. Due to pandemic situation, supply from China is very irregular and of varying grade. Since, the above drugs are vital (life saving) and in great demand during current pandemic situation, APL has decided to start manufacture of CAA from basic raw materials.

A) Products with change in product mix as below:

APL (Unit VI), proposes Change of Product Mix as per below:

Sr. No.	Product	EC Quantity (MTPM) (*)	Quantity MTPM		Remarks
			Existing CTO(*)	Proposed	

1	Sulphuric acid/ Oleum 25%/ Oleum 65%/ Liquid SO3 (Sulphuric anhydride)	6000	6000	6000	
2	Di Methyl Sulphate (DMS)	2000	2500	2500	
3	Di Ethyl Sulphate (DES)	1200	700	700	
4	Di Methyl Urea (DMU)	600	600	600	
5	Monomethyl Urea (MMU)	100	100	100	
6	Sodium Vinyl Sulphonate (SVS)	300	300	300	
7	Cyano Acetic Acid (CAA)- Purification	500	250	0	-250
	Cyano Acetic Acid (CAA)- New Process	**0**	**0**	**500**	**500**
8	Cyano Acetyl Methyl Urea (CAMU)	300	50	50	
9	Nitroso Urasil	300	300	0	-300
10	Di Methyl Aniline	18	518	518	
	Total (A)	**11318**	**11318**	**11268**	**-50**
11	Captive Power (KW)	500	500	500	

Note :- (*) CTO No. Format 1.0/AS(T)/UAN No. 0000124079/CR/2204001256 Dt 19-04-2022

The highlights of the proposal are as below;

a) Manufacture of 500 MT/M of 70% CAA from starting raw materials mono chloro acetic acid & sodium cyanide (reaction + distillation)
b) Discontinuing distillation/purification of CAA 250 MT/M
c) Total Product quantity reduced by 50 MT/M
d) Reduction in Nitrosourasil & CAA (Distillation) Production Capacity.
e) Thus, there is no increase in overall product quantity and product range (existing and proposed) covered under Synthetic Organic Chemicals Manufacturing category 5(f) as per EIA Notification 14.09.2006. Thus, the proposal qualifies for consideration under Change of Product Mix as per Amendment dated 23rd November 2016 of the said Notification.

Summary of proposed changes:

Product	Proposed change	Remark
Cyano Acetic Acid (CAA)	Increase in capacity with process change	Process change- Existing process--Currently crude CAA is bought and distilled. Proposed process – To manufacture from starting RM Mono Chloro Acetic Acid
Nitroso urasil	Discontinuation of manufacturing	
By Product – Sodium Chloride	**New by-product**	**From CAA**

B. Pollution load Details:

i) Water and waste water Aspect

(a) Water Consumption aspect

- Water requirement is for Domestic, Process, Cooling / Boiler & Green belt. Total water requirement for the existing facility is 1234 cmd.
- The water requirement after change in product mix has been calculated from the material balances and is found to be 1144 cmd.
- The detailed breakup of water requirement is as below:

Sr. No.	Purpose	Existing Water Consumption (cmd)	After Change in product Mix (cmd)	Remark
1	Domestic	9	9	
2	Industrial			
2.1	Processing	80	90	Preparation of Soda Ash solution in CAA- This will be met primarily by use of recycle water.
2.2	Boiler feed	407	402	Installation of RO will reduce DM regeneration
2.2	Cooling	738	642	Proposed replacement of Cooling tower natural to induce draft
	Total	**1234**	**1144**	Overall Water consumption will be reduced by 90 cmd

The total water requirement as per Environmental clearance no. SEIAA-EC-0000000258 dated 26/04/2018 is 1281 cmd. Thus, the water requirement is within the EC quantity. Total water consumption in process is increasing from 80 cmd to 90 cmd, however this will be met from recycled water (post change in product mix, fresh water consumption is reduced by 2 cmd, from existing 63.8 cmd to 62.4 cmd whereas Recycled water consumption is increased by 12 cmd, existing 16.3 cmd, to proposed 27.9 cmd). Thus, there is Overall Water consumption will be reduced by 90 cmd from existing Consented quantity.

(b) Effluent Generation & Its disposal

Total Effluent generation in existing facility from Domestic, Process, Cooling / Boiler & proposed effluent generation is tabulated below:

No	Purpose	Existing Effluent Generation, m^3/day	After Change in product Mix, m^3/day	Mode of treatment
1	**Domestic**	7	7	STP
2	**Industrial**			
2.1	Processing	8	8	MEE
2.2	Boiler & DM Plant	42	36	33 RO + 3 MEE
2.3	Cooling Tower BLD	78	78	72 RO + 6 ETP
	RO reject	17	13	MEE
	Grand Total	**145**	**135**	

Overall reduction by 10 m^3/day in effluent generation

To reduce DM regeneration & backwash RO will be installed as pretreatment for treating MIDC raw water.

To increase treated effluent recycle planned to install 3rd stage RO.

(c) Effluent Quality:

Product wise pollution load in existing and proposed operations due to effluent generation in process is presented is as below;

Pollution Load Existing and Proposed (Effluents)

Sr. No.	Stream	Existing Effluent load			Total Load		Proposed Effluent load			Total Load	
		Effluent Qty.	COD	TDS	COD	TDS	Effluent Qty.	COD	TDS	COD	TDS
	Unit	cmd	ppm	ppm	kg/day	kg/day	cmd	ppm	ppm	kg/day	kg/day
1	Cooling tower blowdown	72	250	1100	18	79	72	250	1100	18	79
2	Boiler blowdown	31	250	250	8	8	31	250	250	8	8
3	DM Plant	5	300	3500	2	18	2	300	3500	1	7
4	DM Plant regeneration	6	2500	50000	15	300	3	2500	50000	8	150
5	RO reject	17	3014	11000	51	187	13	3813	12000	50	156
	Total -A (Utilities)	131			93	591	121			83	400
6	Cyano Acetyl Methyl Urea (CAMU)	1	7000	50000	7	48	1	7000	50000	7	48
7	Di Methyl Aniline	1	15000	55479	14	52	1	15000	55479	14	52
8	Cyno Acetic Acid (CAA)										
a	Cyno Acetic Acid (CAA) (Purification)	0	0	0	0	0	0	0	0	0	0
b	Cyno Acetic Acid (CAA) (New Process)	0	0	0	0	0	2	5000	60000	8	96
9	Nitroso Urasil	2	5500	90000	11	179	0	0	0	0	0
10	Acid Plant / CAMU / Nitroso Scrubber	4	3500	50000	14	200	4	3500	50000	14	200
11	DMS / DES Ejector cooling tower	6	4000	5500	24	33	6	4000	5500	24	33
	Total -B (Process)	14			81	700	14			78	498
	Total A+B	145			163	1103	135			150	829

From the same it can be seen that the effluent hydraulic load will reduce from 145cmd to 135cmd, COD load from 163 kg/d to 150 kg/d and TDS load from 1103 kg/d to 829 kg/d.

Thus, there is reduction in effluent generation and pollution load post proposal.
The company has a fully functional effluent treatment plant consisting of primary, secondary & tertiary treatment of capacity 159 cmd with RO and Evaporator. Treated effluent is fully recycled within the site, thereby achieving Zero Liquid discharge.

Domestic sewage (8cmd) is treated in STP plant and treated sewage water used for gardening.

ii) Air emissions Load:-

Details of Fuel Burning emissions

Major heat requirement for process is met by way of steam. The product wise steam requirement in existing and proposed operations is presented, it can be seen that the existing steam requirement is 13.3TPH whereas it is 12.5TPH in proposed operations. Most of the plant steam requirement fulfilled from Waste Heat Recovery (from sulfuric acid plant). No additional Steam is required after proposal. Heat recovery proposed in DMS (for use of waste heat from distillation system + pre- heating of Raw materials), Flash steam recovery system, MVR proposed for steam conservation / recovery in CAA plant. There will not be any additional fuel burning sources installed for proposed change in product mix.

Sr. No.	Product	Steam requirement TPH	
		Existing	After product mix
1	Sulphuric acid/ Oleum 25%/ Oleum 65%/ Liquid SO3 (Sulphuric anhydride)	1.2	1.2
2	Di Methyl Sulphate (DMS)	5.5	4.1
3	Di Ethyl Sulphate (DES)	1.0	1.0
4	Di Methyl Urea (DMU)	1.2	1.2
5	Monomethyl Urea (MMU)	0.5	0.5
6	Sodium Vinyl Sulphonate (SVS)	0.5	0.5
7	Cyno Acetic Acid (CAA)		
7a	**Cyno Acetic Acid (CAA) (Purification)**	**0.4**	**0.0**
7b	**Cyno Acetic Acid (CAA) (RM)**	**0.0**	**2.0**

8	Cyano Acetyl Methyl Urea (CAMU)	0.0	0.0
9	Nitroso Urasil	1.0	0.0
10	Di Methyl Aniline	1.0	1.0
11	MEE	1.0	1.0
	Total	**13.3**	**12.5**

Fuel burning sources in existing & proposed facility is unchanged as tabulated below:

S. N.	Source	Fuel	Fuel Consumption	APC	Stack Height	After Proposal
1.	6 TPH Boiler	Coal	1200 Kg/hr	Bag Filter	34	No change envisaged
2.	4 Lakh Kcal/Hr Thermic fluid heater	LDO	21 kg/hr	Scrubber	22	No change envisaged
3.	500 KVA DG set	HSD	30 Lit/Hr	Acoustic Enclosure Stack	5 m above building	No change envisaged
4.	1500 KVA DG set	HSD	60 Lit/Hr	Acoustic Enclosure Stack	8 m above building	No change envisaged

Thus, post proposal the emissions from utilities will be reduced on account of reduce steam requirement & will be within consented limits. Continuous online emission monitoring installed & connected to MPCB, CPCB The industry is self-monitoring the emissions from stacks from MOEF & CC approves laboratory & the emissions are within the limits stipulated in CTO. There is no change in overall fuel burning sources/ fuel consumption/ Air emissions due to proposed change in product mix.

Details of Process Emission Load;

The process emissions are controlled by adequate size scrubbers. There will be one additional scrubber added in CAA plant due to change in process for the proposed change in product mix. Details of existing plus proposed one new (sr no 7) process scrubbers are as below-

Details of Existing Process Vents and APCM;

Sr no	Stack attached to	Stack height (m)	APCM	Parameter	Permissible Limit
				Existing	
1	Process reactor (H2SO4 plant)	45	Wet scrubber	Acid Mist	20 mg/Nm^3
2	Sulphonation Reactor (DMS Plant)	9	Wet scrubber	Acid Mist	20 mg/Nm^3
				SO2	50 ppm
3	DES Reactor	9	Scrubber	Acid Mist	20 mg/Nm^3
				SO2	50 ppm
4	SVS Plant	9	Scrubber	Acid Mist	20 mg/Nm^3
				SO2	50 ppm
5	DMU/MMU Plant	9	Scrubber	Acid Mist	20 mg/Nm^3
				SO2	50 ppm
6	Ammonium Sulphate Plant	9	Scrubber	NH3	50 ppm

DES/SVS has same first stage reaction and hence APL will carry out reaction in one reactor and connect to scrubber, thereby reducing one process vent.

Process vents (post change in product mix):

Sr. no	Stack attached to	Stack height (m)	APCM	Parameter	Permissible Limit
				After change in product mix	
1	Process reactor (H2SO4 plant)	45	Wet scrubber	Acid Mist	20 mg/Nm3
2	Sulphonation Reactor (DMS Plant)	9	Wet scrubber	Acid Mist	20 mg/Nm3
				SO2	50 ppm
3	DES Reactor/ SVS reactor	9	Scrubber	Acid Mist	20 mg/Nm3

				SO2	50 ppm
4	DMU/MMU Plant	9	Scrubber	Acid Mist	20 mg/Nm3
				SO2	50 ppm
5	Ammonium Sulphate Plant	9	Scrubber	NH3	50 ppm
6	CAA	9	Alkali Scrubber	HCl	35 mg/Nm3
				HCN	10 ppm

There will be one additional scrubber added in CAA plant for the proposed change in product mix .Continuous online emission monitoring installed & connected to MPCB, CPCB

The pollution load from process vents in existing and proposed operations is computed and presented below:

Pollution Load from Process (Existing and Proposed)

Product	Parameter	Limit	Unit	Gas flow m^3/Hr	Existing		Proposed	
					mg/Nm^3	kg/d	mg/Nm^3	kg/d
Di Methyl Sulphate (DMS)	SO_2	50	ppm	150	143	0.5	143	0.5
Di Ethyl Sulphate (DES)	SO_2	50	ppm	150	143	0.5	143	0.5
Di-Methyl Urea (DMU)/ Monomethyl urea (MMU)	Ammonia	20	mg/Nm^3	200	20	0.1	20	0.1
Sodium Vinyl Sulphonate (SVS)	SO_2	50	ppm	150	143	0.5	0	0.0
Cyano Acetic Acid (CAA)						0.0		
Cyano Acetic Acid (CAA)-Purification								

Cyno Acetic Acid (CAA)-Process	HCN	10	ppm	150	--	--	12	0.04
	HCl	35	mg/Nm^3	150	0	0.0	35	0.13
Ammonium Sulphate	Ammonia	20	mg/Nm^3	150	20	0.1	20	0.1
						1.7		**1.4**

From the above it can be seen that the load in existing operations is 1.7kg/d which reduces to 1.4kg/d in proposed operations.

iii) Hazardous Waste Generation and its Disposal:

The existing & proposed hazardous waste generation is tabulated below:

Sr. No	Type of Waste	Category	Generation			Source Of Generation	Disposal
			Existing	Proposed	Remarks	Treatment	
1	Distillation	17.1	6 MT/A	6 MT/A	From Acid Plant	Preprocessing / Co-processing / Incineration	Sale to authorized party/ CHWTSDF
2	Residue	17.2	255 Lit/A	255 Lit/A	From DMS / DES	Recycle	Sale to authorized party/ CHWTSDF
3	Discarded containers/barrels/ liners	33.1	1 MT/A	1 MT/A	From Plant	Recycle	CHWTSDF/ Sale to authorized party after decontamination
4	Chemical sludge from waste water treatment	35.3	100 KG/M	100 KG/M	From ETP	Landfill after treatment	CHWTSDF
5	Spent carbon	28.3	25 MT/A	25 MT/A	From Plant/ETP	Preprocessing / Co-processing / Incineration	Sale to authorized party/ CHWTSDF

6	Sludge from concentration technique (MEE)	37.3	330 MT/A	250 MT/A	From MEE	Landfill after treatment	Sale to authorized party/ CHWTSDF
7	Distillation	20.3	14.4 MT/A	14.4 MT/A	From DMA Plant	Preprocessing / Co-processing / Incineration	Sale to authorized party/ CHWTSDF

Thus, there is reduction in sludge from MEE post change in product mix due to reduction in effluent quantity and TDS load to ETP. Thus the Hazardous waste generation post product mix change and generation will be as per the limits of CTO.

During grant of CTO, MPCB has transferred some of the byproducts to HW schedule and asked industry to obtain permission under Rule 9 of HOWM Rules 2016. From the material balance, the byproduct generation was computed in post project scenario and same is presented below.

Byproduct (Hazardous Waste) Generation

Sr No.	Product	Catagory	Existing MT/M	Proposed MT/M	Remarks	Source Of Generation	Disposal
1	Spent acid (from DMS)	26.3	53	53	0	DMS	Sale to Authorised party /CHWTSDF
2	Spent acid (from DES)	26.3	1199	1199	0	DES	Sale to Authorised party /CHWTSDF
3	Liquor Ammonia (20 %)	28.1	1305	1305	0	DMU / MMU	Sale to Authorised party /CHWTSDF
4	Ammonium sulphate	28.1	1488	1119	-369	Rxn of Spent + Ammonia	Sale to Authorised party /CHWTSDF
5	Sodium sulphate	28.1	110	110	0	SVS	Sale to Authorised party /CHWTSDF
6	Acetic Acid (95%)	26.3	138	45	-93	Nitroso / CAMU	Sale to Authorised party /CHWTSDF
7	Acetic Acid (35%)	26.3	64	14	-50	Nitroso / CAMU	Sale to Authorised party /CHWTSDF
8	Sodium Chloride		0	457	457	CAA	Sale to Authorised party /CHWTSDF
	Total (B)		4357	4302	-55		
	Total (A+B)		16175	16070	-105		

Technical Committee Deliberations:

Minutes of 4th Technical Committee Meeting (2023-2024), for certification about "No Increase in Pollution Load" dtd. 10th March 2023

The project proposal was discussed on the basis of presentation made by Consultant and documents- NIPL Certificate submitted by the proponent. Product wise load calculation in terms of wastewater, Air Emissions & Hazardous Waste generations were discussed. Existing Consent to Operate, Environmental Clearance, No Increase in Pollution Load certificate issued by M/s. Aditya Environmental Services Private Limited vide letter dated 17th Aug. 2022 are taken on record.

Committee after due deliberations noticed that:

i. It is seen that there is reduction in water consumption post expansion project.
ii. There is reduction in pollution load in respect of effluent quantity, effluent quality (organic load and TDS), air pollution load due to fuel burning, process emission load and hazardous waste generation

Technical Committee Decision:

Technical Committee decided to recommend the case for change in product under product mix with a compliance of the following conditions.

(i) Industry shall comply with all the conditions stipulated in Environmental Clearance and ensure display/upload of six-monthly compliance monitoring report on their official website.
(ii) Industry should not manufacture any other product for which permission is not granted by the Board.
(iii) Industry shall ensure connectivity of OCEMS to Board server.

Agenda Item No.	**Item No. 5**
Proposal No.	MPCB-CONSENT-0000139385
Project Details	**M/s. Curia India Private Limited** Plot no. G-1/1, 1/2, MIDC Waluj, Aurangabad
NIPL Certificate	NIPL certificate issued by M/s. SD Engineering services pvt. ltd., Aurangabad

Introduction:

This has reference to the online proposal submitted vide No. MPCB-CONSENT-0000139385 along with the copies of documents seeking amendment in existing consent to operate under change in product-mix under the provision of EIA Notification 2006 as amended on 23/11/2016 & 02/03/2021.

Exiting Clearances:

1. Environmental Clearance is granted to the industry for expansion vide SEAC-2015/CR-152/TC-2 dated 18/7/2016 and amended vide No. SEAC/CR-152/TC-2 dated 02/03/2017.
2. Change in Name in Environmental clearance issues by SEAC vide dtd. 14/05/2019.
3. Consent to Operate accorded by the Board vide Consent Order No. BO/AST/ UAN No. MPCB-CONSENT-0000033034/A/CC-1808000034, Dated 01/08/2018 valid up to 30/04/2020.
4. Corrigendum in the Consent to Operate issued vide no. BO/AST/RO-AD/ MPCB-CONSENT_Ammend-00000001122/R/CC-1811000044, dated 27/11/2018.
5. Change in name in Company of M/s Amri India Pvt. Ltd. to M/s. Albany Molecular Research Hyderabad Research Centre Pvt. Ltd. vide MPCB/AS(T)/Amendment/TB-1905000030, Date 17/05/2019.
6. Minutes of 4th meeting of Technical Committee (2020-21) & Minutes of 6th meeting of Technical Committee (2020-21) for assessment of application of under change In product-mix held on dated 20/06/2020 & 31/10/2020 respectively.
7. Minutes of 6th Consent Committee Meeting of 2019 2020, held on dated 02/07/2020.
8. Industry's Request letter vide dtd. 22/07/2020 for resubmission of revised Presentation before Technical Committee under Change in Product- Mix dtd 31.10,2020.
9. Minutes of 13th Consent Committee Meeting of 202G-21, held on 01/0212021, 12/02/2021 & 25/02/2021
10. Amendment in consent to operate for change in name from M/s Albany Molecular Research Hyderabad Research Centre Pvt. Ltd. to M/s. Curia India Private Limited. Vide dated 15.06.2022

Project details:

A. Production Details:

Sr. No.	New Product Name	Existing Quantity (MT/M)	Proposed Quantity (MT/M)	Total Quantity (MT/M)	Remarks
1.	Furosemide	15	-	15	No change
2.	Isosorbide-5-mononitrate	6	-	6	No change
3.	Dilute Isosorbide-5-mononitrate (10% to 90%)	10	-	10	No change
4.	4-isothiocyanato-2-(trifluoromethyl) benzonitrile (MDV3100-6) [MDV-6]	4.5	-	4.5	No change
5.	Diatrizoate Sodium	6	-	6	No change
6.	Diatrizoate Meglumine	6	-	6	No change
7.	Propranolol Hydrochloride	2	-	2	No change
8.	7-acetyl-1,2,4,6,7,8,12,13,14,15,16,17-dodecahydrospiro [cyclopenta[a]phenanthrene-3,2'-[1,3]dioxolan]-17-yl acetate (Ketal Acetate)	3	-	3	No change
9.	Anecortave (5HC) Hydrocortisone Base (HC) or Tetraene Acetate (2TR)	3	-	3	No change
10.	(R)-2,7,8-trimethyl-2-((4R,8R)-4,8,12-trimethyltridecyl) chroman-6-01 or D-α-Tocopheryl polyethylene glycol succinate Vitamin-E TPGS	3	-	3	No change
11.	Solifenacin Succinate	2	-	2	No change
12.	Fesoterodine	1	-	1	No change
13.	Deferasirox	2	-	2	No change
14.	Fluticasone Furoate	2	-	2	No change
15.	Indacaterol	2	-	2	No change
16.	2-Acetate	6	-	6	No change

17.	Ethyl 2,4-dihydroxy-6-pentylbenzoate (Ethyl Olivetolate)	2	-	2	No change
18.	(1S,4R)-1-methyl-4-(prop-1-en-2-yl)cyclohex-2-enol (Menthadienol)	2	-	2	No change
19.	2-(4-chloro-3-(chlorosulfonyl)benzoyl)benzoic acid (Chlorthalidone Intermediate-1/ intermediates	15	-	15	No change
20.	(4S-trans)-4-(N-acetyl-N-ethylamino)-5,6-dihydro-6-methyl-4H-thien-(2,3-b)-thiopyran-7,7-dioxide (Chiral Acetamide)	5	-	5	No change
21.	2-(Formamido-1,3-thiazol-4-yl) glyoxylic acid AZTH3 intermediate	3	-	3	No change
22.	2-Mercapto-N-methylbenzamide	3	-	3	No change
23.	Citarabine intermediate	5	-	5	No change
24.	2-3((3-Fluoro-4-(methylcarbamoyl) phenyl) amino)-2-methylpropanoic acid (MDV 4)	6	-	6	No change
25.	4-Bromo-2-fluro-N-methyl benzamide MDV-2	8	-	8	No change
26.	6-Chloro 3 methyl Uracil (CMU)	2.5	-	2.5	No change
27.	5-Bromo-2-(2-methyl-2H-tetrazol-5-yl)pyridine (DA-3)	3	-	3	No change
28.	Acetyl Benzyl Amine	15	-	15	No change
29.	Sodium benzofuran-6-carboxylate (Synthon A)	4	-	4	No change
30.	2-(tert-Butoxycarbonyl)-5,7-dichloro-1,2,3,4-tetrahydroisoquinoline-6-carboxylic acid (Synthon B)	4	-	4	No change
31.	Benzyl 2-amino-3-(3-methylsulfonyl)phenyl) propanoate Hydrochloride (Synthon C)	4	-	4	No change
32.	(S)-methyl 2-methylpyrrolidine-2-carboxylate Neuren-4	3	-	3	No change

33.	(S)-dibenzyl 2-((S)-1-(2-(benzyloxy) carbonyl) amino) acetyl)-2-methylpyrrolidine-2-carboxamido) pentanedioate Neuren-7	3	-	3	No change
34.	Propionyl Chloride	15	-	15	No change
35.	2-Amino-5-bromo Benzoxazole [ML 737] OR tert-butyl (5-bromobenzo[d]oxazol-2-yl) carbamate or (BOC-ML737)	4	-	4	No change
36.	4-Amino pyrazolopyrimidine [ML739]	6	-	6	No change
37.	Bromofluro methane (BFM)	0.5	-	0.5	No change
38.	Benzyl 2-bromo ethyl ether (BBEE)	0.75	-	0.75	No change
39.	1,6-Di Bromo hexane	5.40	-	5.40	No change
40.	5-bromo-3-methyl-6-oxo-1,6-dihydropyridine-2-carboxamide (Methyl analogue of pyridine der) (eFT000776) OR N-(6-aminopyrimidin-4-yl) cyclopropanecarboxamide (eFT000775)	1	-	1	No change
41.	**1-(benzyloxy)-4-bromo-2,5 dimethoxybenzene Compound 4 (SGL Chemistry)**	**2**	**0**	**0**	**Deleted**
42.	N,N-bis(2.4-dichlorobenzyl) hydroxylamine (Compound 1534 Water villie)	6.5	-	6.5	No change
43.	tert-butyl((1s,4s)-4-aminocyclohexyl)carbamate [BOC - CIS -Diamine]	3	-	3	No change
44.	2-(4-(benzyloxy)-3-nitrophenyl)oxirane [Borregaard NSO]	3	-	3	No change
45.	6-((2-(3,4- dihydroxyphentl1)-4-oxo-4H-chromen-3-yl)oxy)-6-oxohexanoic acid [NP-202]	3	-	3	No change
46.	Miconazole Nitrate	1	-	1	No change
47.	Timolol Maleate (Timolol)	1	-	1	No change
48.	**Warfarin Sodium Clathrate [Warfarin]**	**1**	**0**	**0**	**Deleted**
49.	1,2-Di-P-tolylethane-1,2-dione dioxime	3	-	3	No change

50.	Ethyl 2,4,6-tri-O-benzoyl-β-D-thiogalactopyranoside (PF-06460245)	3	-	3	No change
51.	**Amine HCl salt 090602**	**3**	**0**	**0**	**Deleted**
52.	N-(3,5-dichloro-4-((6-oxo-1,6-dihydropyridazine-3-yl) oxy) phenyl) benzamide (Intermediate-C)	2	-	2	No change
53.	N-cyanoacetylurethane (NCAU)	2	-	2	No change
54.	4-acetyle-4'-(benzyloxy)-2',5'-dimethoxy-[1,1'-biphenyl]-2-carboxylic acid Compound 7 (SGL Chemistry)	2	-	2	No change
55.	(R)-2-(2-(3-(((benzyloxy)carbonyl)amino)propyl)phenoxy) propyl 4-methylbenzenesulfonate (LP101-9c)	1	-	1	No change
56.	Adrenalone HCl	5	-	5	No change
57.	Dibenzyl Artereone	5	-	5	No change
58.	2-(5-((3-Methyloxetan-3-yl)methoxy)-1H-benzo[d] imidazol-1-yl) quinolin-8-ol (ASP-187)	3	-	3	No change
59.	Apalutamide	1	-	1	No change
60.	Ziprasidone Nucleus	2.5	-	2.5	No change
61.	BG-4 (5-amino-3-(4-phenoxyphenyl)-1H-pyrazole-4-carbonitrile)	2.5	-	2.5	No change
62.	BG-8 (tert-butyl (E)-4-(3-(dimethyl amino) acryloyl) piperidine-1 -carboxylate)	2	-	2	No change
63.	PF -06850062 (((1R,5S,6r)-3-benzyl-3-azabicyclo[3.1.0]hexan-6-yl)methanol)	1.5	-	1.5	No change
64.	1H-Pyrrolo[2,3-D] Pyrimidine -2, 4(3H, 7H)-Dione	2.5	-	2.5	No change
65.	2,4-Dichloro Pyrimidine	2.5	-	2.5	No change
66.	3-Cyano-5-Hydroxy Pyridine	2.5	-	2.5	No change

67.	Bay-28288113 (N-((R)-chroman-4-yl)-7-fluoro-4-(3-fluoroazetidin-1-yl)-8-(2,3,5-trifluorophenyl) quinoline-3 -carboxamide)	1.5	-	1.5	No change
68.	R & D Products	0.5	-	0.5	No change
69.	Distillation of spent solvent	20	-	20	No change
70.	Tolazoline HCl	2	-	2	No change
71.	Potassium 6-(4-amino-2,6-dichlorophenoxy)-4-isopropylpyridazin-3-olate [Intermediate F]	1	-	1	No change
72.	Pravibismane- API	1	-	1	No change
73.	**SNDX-5613-5 OR (N-Ethyl-5-fluoro-N-isopropyl-2-(pyrimidin-5-yloxy) benzamide)**	**0**	**1.5**	**1.5**	**Newly added**
74.	**SNDX-5613-8 OR (Tert-butyl 2- (5- (2- (ethyl (isopropyl) carbamoyl) -4-fluorophenoxy) -pyrimidin-4-yl) -2,7-diazaspiro [3.5] nonane-7-carboxylate)**	**0**	**1.5**	**1.5**	**Newly added**
75.	**SNDX-5613-10A OR (trans-4-((ethylsulfonamido)cyclohexyl) methyl-4-methylbenzene sulfonate)**	**0**	**1.5**	**1.5**	**Newly added**
76.	**Ligand OR (TBUPDI)**	**0**	**1.5**	**1.5**	**Newly added**

The overall production quantity will remain same. Total Production capacity of above mentioned products shall not exceed 65 MT/M

B. Pollution load Details:

(i) Water & Wastewater Aspect

Before Product Mix

Sr. No.	Particular	Quantity in CMD	Effluent Segregation in CMD	COD (Strong)	COD (Weak)	TDS (Strong)	TDS (Weak)

			Strong	Weak	mg/l	Kg/day	mg/l	Kg/day	mg/l	Kg/day	mg/l	Kg/day
1	Water Consumption	80.40	Not applicable									
2	**Trade Effluent Generation**											
A	Process Activity	**39.40**	14.73	19.70	50000	736.5	5000	98.5	60000	883.8	2800	41.24
B	Cooling Tower & Boiler	**26**	--	2.3	--	--	5000	11.5	--	--	2800	6.44
C	**Total**	**65.40**		36.73	--	736.5		**110**	--	883.8		47.68
3	Domestic Effluent Generation, CMD	**10**	---	7	---	---	500	3.5	--	---	900	6.3
4	Other (Gardening)	**5**	--	--	--	--	--	--	--	--	--	--

After Product Mix:

Sr. No.	Particular	Quantity in CMD	Effluent Segregation in CMD		COD (Strong)		COD (Weak)		TDS (Strong)		TDS (Weak)	
			Strong	Weak	mg/l	Kg/day	mg/l	Kg/day	mg/l	Kg/day	mg/l	Kg/day
1	Water Consumption	79.95	Not applicable									
2	**Trade Effluent Generation**											
A	Process Activity	**38.95**	14.16	19.70	50000	708	5000	98.5	60000	849.6	2800	41.24
B	Cooling Tower & Boiler	**26**	--	2.3	--	--	5000	11.5	--	--	2800	6.44
C	**Total**	**64.95**		36.16	--	708		110	--	849.6		47.68

3	Domestic Effluent Generation, CMD	10	---	7	---	---	500	3.5	--	---	900	6.3
4	Other (Gardening)	5	--	--	--	--	--	--	--	--	--	--

- Water Consumption will reduce by 0.45 CMD
- Effluent Generation will reduce by 0.57 CMD
- COD load for trade effluent will reduce by 28.5 Kg/day
- TDS load for trade effluent will reduce by 34.2 Kg/day

Treatment System

a) Trade Effluent:

Industry has segregated trade effluent into weak stream & strong stream and provided Effluent Treatment Plant (ETP) comprising of;

- **Strong COD/TDS stream of 14.16 CMD:** Treatment scheme comprising of primary (Equalization tank, primary clarifier/ primary settling tank) stripper, Multi-effect evaporator with design capacity of 15 CMD followed by centrifuge.

- **Weak COD/TDS stream of 22.0 CMD:** Treatment system comprising of primary (equalization tank), Secondary (Activated sludge process), Tertiary (Pressure Sand filter. Activated carbon filter) with design capacity of 25 CMD. Followed by Reverse Osmosis of 50 CMD capacity.

b) Domestic Effluent:

The domestic effluent is treated in sewage treatment plant of capacity 15 CMD.

(ii) Air Emission Load ;

Sr. No.	Stack attached to	Fuel	Before product Mix	After Product Mix	Remark
1	Boiler –I	Briquette	7 MT/ Day	7 MT/ Day	No change
2	Boiler- II /	LDO	0.5 MT/Day	0.5 MT/Day	No change

	Thermo-pack				
3	D.G. Set 500 KVA	HSD	0.3 TPD	0.3 TPD	No change
4	D.G. Set 1100 KVA	HSD	1.0 TPD	1.0 TPD	No change
5	Fire D.G. Set	HSD	1.0 TPD	1.0 TPD	No change

(iii) Hazardous Waste Load

Sr. No.	Type of Waste	Category (As per Schedule)	Generation per Year		Remark
			Before product Mix	After Product Mix	
1	Used / spent Oil	5.1/5.2	200 kg/M	200 kg/M	No Change
2	Spent Solvent	20.2	190000 kg/M	190000 kg/M	No Change
3	Process Waste & Residue	28.1	34666 kg/M	34666 kg/M	No Change
4	Spent Catalyst/ Spent Carbon	28.2	6845 kg/M	6845 kg/M	No Change
5	Spent Catalyst/ Spent Carbon	28.2	2000 Kg/M	2000 Kg/M	No Change
6	Off Specification/ Discarded Drug, medicine product	28.4	1000 kg/M	1000 kg/M	No Change
7	Spent Mother Liquor (Dilute Caustic Lye)	28.6	10 MT/M	10 MT/M	No Change
8	Spent Mother Liquor	28.6	17600 kg/M	17600 Kg/M	No Change
9	Spent organic Solvent	28.6	81300 kg/M	81300 Kg/M	No Change
10	Discarded Containers/Barrel/ liner	33.1	100 Nos./M	100 Nos./M	No Change
11	Chemical Sludge from Waste Water treatment	35.3	5823 kg/M	5823 kg/M	No Change
12	Chemical Sludge, Oil & grease skimming residue	35.4	100 kg/M	100 kg/M	No Change

13	Cotton rags and other cleaning material	33.2	100 Kg/M	100 Kg/M	No Change

Technical Committee Deliberations:

The proposed project was discussed on the basis of documents – NIPL Certificate and presentation made by the industry. Product wise load calculation in terms of Wastewater, Air emissions & Hazardous waste generation was discussed. Existing Consent to Operate, Environmental Clearance, NIPL Certificate issued by M/s. SD Engineering Services Pvt. Ltd. and Product – Mix Proforma are taken on the record.

After due deliberations, Committee noticed that:

i. Industry has applied for Change in Product Mix with no increase in the production quantity. The total production quantity will be remaining same after product mix i.e. 65 MT/ M.
ii. The water consumption, trade effluent generation will be reduced by 0.45 CMD & 0.57 CMD respectively after product mix change.
iii. COD load will reduce by 28.5 Kg/day and TDS load will reduce by 34.2 Kg/day
iv. Committee noticed that, industry have segregated effluent into strong and weak stream
v. The overall hazardous waste quantity after product mix will remain same.
vi. The overall pollution load is not increased after change in product – mix.

Technical Committee Decision:

Technical Committee decided to recommend the case for change in product under product mix with a compliance of the following conditions.

(i) Industry shall comply with all the conditions stipulated in Environmental Clearance and ensure display/upload of six-monthly compliance monitoring report on their official website.
(ii) Industry should not manufacture any other product for which permission is not granted by the Board.
(iii) Industry shall ensure connectivity of OCEMS to Board server.

Agenda Item No.	**Item No. 6**
Proposal No.	MPCB-CONSENT-0000143507
Project Details	**M/s. Varuneshwar Organic** B-48, MIDC Taswade, Karad
NIPL Certificate	NIPL certificate issued by M/s.

The committee was informed that, M/s. **Varuneshwar Organic** had expressed their inability to attend the said meeting. The committee considered the same and it was decided to defer the case.

Agenda Item No.	**Item No. 7**
Proposal No.	MPCB-CONSENT-0000143371
Project Details	M/s. Sahkar Maharshi Shankarrao Kolhe Sahkari Sakhar Karkhana Ltd. 20/2 At Sahajanandnagar, Post Shingnapur Kopargaon
NIPL Certificate	NIPL certificate issued by M/s.

The committee was informed that, **M/s. Sahkar Maharshi Shankarrao Kolhe Sahkari Sakhar Karkhana Ltd.** had expressed their inability to attend the said meeting. The committee considered the same and it was decided to defer the case.

Agenda Item No.	**Item No .8**
Proposal No.	MPCB-CONSENT-0000147687.
Project Details	Addition of De- Aromatized Solvent (DAS) products at existing refinery of M/s.Bharat Petroleum Corporation (BPCL), Mahul Village ,Chembur,Mumbai
NIPL Certificate	NIPL Certificate issued by M/s. Aditya Environmental Services Private Limited vide letter ref: AESPL/22-23/NIPL04 dated 05/01/2023

Introduction:

This has reference to the online proposal submitted vide No. MPCB-CONSENT-0000147687 along with the copies of documents seeking amendment in existing CTE under change in product-mix under the provisions of EIA Notification 2006 as amended on 23/11/2016 & 02/03/2021.

Existing Environment Clearances (EC):

1. EC was granted to BPCL by MoEF& CC for PRFCCU project (under implementation) (Petro Resid Fluidized Catalytic Cracking Unit F. No. J-11011/145/2018-IA II (I) dt 05.08.19 valid upto 4th Aug-2024) which gives complete product mix for BPCL and shows total production of refinery as 42000 MTPD
2. Refinery has Consent to operate for existing products RED/L.S.I (R56) No. Format 1.0/CAC/UAN No.-0000148651/CO-221200459 dated 7th December 2022 valid upto 31st August 2023 and is sanctioned for total production of 40836 MTPD

The existing product quantities as per EC and as per CTO granted by MPCB are as below:

Product Name	**UOM**	**Products Quantity as per**		**Remark**
		EC dt 05/08/2019	**CTO dt 07/ 12/2022 (*)**	
LPG, poly Propylene Feed Stock	**MT/D**	**1860**	**1764**	
Benzene, Toluene, Xytol	MT/D	180	180	

SBP 55/115oC), Hexane (FGH 64-69 C) MS, MTBE, NAPTHA.	**MT/D**	**9429**	**9122**	**Consented product quantities are within EC sanctioned limits**
KSO,MTO, ATF	**MT/D**	3450	3450	
HSD, LDO	**MT/D**	19500	19500	
FO, LSHS, Bitumen Sulphur	**MT/D**	**6681**	**5587**	
Lube Oil Base Stock (LOBS) (*)	**MT/D**	**900**	**1233**	
Total	**MT/D**	**42000**	**40836**	

(*) Thus, it is seen that overall production is within the EC sanctioned limit. Earlier BPCL was granted CTO in August 22 under change in product-mix cleared in 2nd meeting of Technical Committee (2020-21) held on 15/4/2020 for Revamp of LOBS Unit and Reconfiguration of Hydrocracker Unit – whereby product mix different than EC was approved

Project Details:

A. Products with change in product mix as below:

BPCL Mumbai Refinery is proposing to establish De-Aromatized Solvent (DAS) unit to manufacture De-Aromatized Solvent products of various grades i.e. D40, D80, D110, D130, and MBL so as to meet increasing market demand of Eco-friendly Solvent products. DAS solvents will be produced by decreasing production of High-speed diesel (HSD), Light Diesel Oil (LDO) as mentioned in table below:

Sr. No	Products	As per CTO MT/day	Changes in Product Mix MT/day	Total MT/day	Remark
1	LPG, Poly Propylene feed stock	1764	-	1764	No change
2	Benzene, Toluene, Xytol	180	-	180	No change

3	Special Naphtha (SBP 55/115 DEG C), Hexane (FGH 64-69 DEG C) Motor Spirit (MS), MTBE, NAPHTHA.	9122	-	9122	No change
4	Superior Kerosene (SK, LABFS), mineral Turpentine (MTO), Aviation Turbine Fuel (ATF)	3450	-	3450	No change
5	HS Furnace Oil (FO), low Sulphur heavy Stock (LSHS), Bitumen (VG40, VG30 & VG10) , Sulphur	5587	-	5587	No change
6	Lube Oil Base Stock (LOBS) and White Oils (HLPO, LLPO)	1233		1233	No change
7	High speed diesel (HSD BSVI, Navy Grade HSD), light Diesel Oil (LDO)	19500	**Reduced by 634.5**	18866	
8	**De-Aromatized Solvent products (D40, D80, D110, D130, MBL)**	**0**	**634.5**	**634.5**	**Addition of De-Aromatized Solvent products**
	Total	**40836**	**634.5**	**40836**	

The highlights of the proposal are

a) No change in overall product quantity which remains unchanged at 40,836 MTPD by decreasing the decreasing production of High-speed diesel (HSD), Light Diesel Oil (LDO) by 634.5 MT/D and producing equivalent quantity of DAS.

b) DAS products will find use in Paint, Pesticide, Pharma and Petroleum industry (as Drilling Fluid) applications where the reduced aromatic content (from 10 % to 0.1 %) will ensure number of benefits like lower toxicity, elimination of odour, lower carcinogenicity, reduced VOC content etc.

B. Pollution load Details:

i) Water & waste water aspects

a) Resource Requirements

- During this process there is no requirement of furnace as hydro dearomatization reaction is exothermic which is used for energy integration (for pre-heating feedstock). Hence there is no additional fuel requirement consequently no increase in emissions.
- Since Feed is hydrotreated in upstream HCU unit (sulfur < 5 ppm), there is no acid gas generation in DAS unit.
- Process water is not required for this process hence there is no effluent generation.
- CHPS gas and Stripper overhead gas (OVHD) will be diverted to existing refinery fuel gas system for internal consumption.
- Recycled gas (RGC) will be reused back in DAS reactor.

Comparison of resource requirements in Existing scenario and Post Product Mix Change is given below:

Sr. No	Particulars	Details		Difference	Remark
		As per Valid CTO	After Product Mix		
1	**Raw Material MT/D**				
	Crude oil	43500	43500	0	No Change
	RLNG Feed	420	420	0	No Change
	Methanol	33	33	0	No Change
2	**Process Water Input (CMD)**	20405	20405	0	No Change
3	**Power Requirement (MW)**	100	99.914	0	Increase in power requirement 0.551 MW will be offset by Encon Schemes for reducing power consumption by 0.637 MW. Hence no additional power requirement.

4	**Steam Requirement (MT)**	12000	11910	0	Increase in steam 166 MTPD will be offset by Encon Schemes for reducing steam consumption by 256 MTPD. Hence no additional steam requirement.
5	**Fuel (MT/day)**				
	LSHS	637.1	637.1	0	No Change
	Fue Gas	1277.4	1277.4	0	No Change
	NAPTHA	25.4	25.4	0	No Change
6	**Number of stacks**	33	33	0	No Change

The above illustrates that there will be no change in resource requirement after implementation of DAS project.

b) Water aspect

- Process water is not required for this process.
- No additional water requirement for steam generation as there is reduction in steam consumption by 90 MTPD due to EnCON scheme under implementation
- As this is exothermic process, Reactor outlet stream heat will be utilized for reactor feed preheating. The sea cooling water requirement is 136 m^3/hr which can be met from existing sea cooling water requirement (which is well within consented value)
- **Thus, water requirement for process (as per CTO vs actual) is presented below:**

Sr. No.	Use /Purpose	Qty of Water Required (cmd)				Remarks
		as per CTO	Actual	Net Addition due Product Mix change	Final Desired Qty	
1	Raw Water to DM plant	20405	8500	Nil	20405	No process water requirement
2	Service Water		811	Nil		Steam requirement reduction by 90 MTPD

3	Cooling Tower Makeup		3500	Nil		
4	Industrial Cooling (*)	154486	65,520	Nil	154486	Even with 3264 cmd for cooling of DAS process, sea water required is lower than CTO value
5	Domestic Water	1408	800	Nil	1408	No additional manpower
6	Unaccounted/Loss	0	77	Nil	0	
	Total	**176299**	**79,208**	**Nil**	**176299**	

Thus, there is no change in water requirement from existing Consented quantity.

c) Effluent Generation & Its disposal

No process effluent generation. Steam requirement is reduced. Slight increase in Sea Cooling Tower blowdown quantity. However, BPCL has implemented recirculating Cooling water system, even for sea water use thereby reducing the sea cooling water blowdown quantity substantially from the consented quantity. The summary of quantity as per CTO, Actual quantity of effluent, addition due to Product Mix change and final desired quantity is presented below:

Source of Effluent Generation	**Qty of Effluent (cmd)**				**Mode of Disposal & Ultimate Receiving Body**
	as per CTO	**Actual**	**Net Addition due product Mix change**	**Final Desired Qty**	
Trade Effluent	5760	2500	Nil	5760	BPCL is ZLD – entire quantity of Treated effluent is recycled back to Cooling Tower
Cooling (Sea water Blow Down)	1,46,649.24	48000	Nil	1,46,649.24	Even with additional 163 cmd, no net addition in requirement for cooling as due to installation of recirculating Sea water Cooling Water system actual BD is much lower than CTO
Domestic	235		Nil	235	Entire quantity of Treated effluent is recycled back to Cooling Tower

		24			
Total Effluent	**1,52,644.24**	**50,524**	**Nil**	**1,52,644.24**	No Change

d) Effluent Quality:

There is no effluent generation from DAS. Hence, there is no change in untreated or treated effluent quality. BPCL has well designed ETP comprising Primary- Secondary and Tertiary Treatment units and entire quantity of treated effluent is recycled for cooling tower, and there is no discharge outside premises. Results of On line Effluent Monitoring system and MoEFCC recognized laboratories are well within MPCB norms.

ii) Process / Air Emission Load:

No addition of Boiler/ process furnace (reduction in steam requirement by 90 TPD), No addition of fuels, No addition of stacks and hence, No change in emissions. Thus, existing stack details remain unchanged.
Thus, there is no change in air emissions due fuel burning from the Consented quantities
Also, since the feed is hydro treated and the off gases are recycled by using Recycle Gas Compressor, there is no process vent in proposed process.

iii) Hazardous Waste Generation and its Disposal:

Hazardous Waste Generation in proposed operations is only due to use of catalyst in proposed DAS unit. HW scenario in existing and proposed operations is presented below:

Sr. No.	Type of Waste	Category (As per Sch)	Generation (MT/A)				Mode of Treatment & Disposal
			As per CTO	Actual	Net Addition Due Product Mix change	Final Desired Qty	
1	Spent Catalyst (*)	4.2	2538.75	508.73	Nil	2538.75	Sale to authorised party/ CHWTSDF
2	Oil Sludge or emulsion	4.1	8100	339	Nil	8100	Bioremediation + landfill
3	Spent carbon	28.3	100	59.6	Nil	100	CHWTSDF

4	Contaminated Cotton rags or other cleaning Material	33.2	50	0	Nil	50	CHWTSDF
5	Empty Barrels / containers/ liners contaminated with hazardous chemicals /waste	33.1	10000 Nos /Y	2662	Nil	10000 Nos /Y	Sale to authorised party/CHWTSDF
6	Used oil/Slop Oil	4.3	270000	109714 MT	Nil	270000	Recycle and reprocessing along with Crude inside refinery

Technical Committee Deliberations:

The project proposal was discussed on the basis of presentation made and documents- NIPL Certificate, NIPL proforma submitted by the proponent. Product wise load calculation in terms of wastewater, Air Emissions & Hazardous Waste generations were discussed. Existing Consent to Operate, Environmental Clearance, No Increase in Pollution Load certificate issued by M/s. Aditya Environmental Services Private Limited vide letter dated 05th Jan. 2023 and product-mix proforma are taken on the record.

Committee after due deliberations noticed that:

i. The PP has proposed change of product mix by reducing quantity of Diesel (HSD and LDO) by 634.5 MT/D, while adding DAS solvent at same quantity that is 634.5 MT/D. Thus, there is no change in production quantity which remains same at 40,836 MTPD. Unit has earlier EC and also production is in same category viz Refinery, thus it is permissible to grant consent to establish based on NIPL.

ii. Post change of product mix, there is no change in net water consumption & effluent generation

iii. No addition of Boiler/process furnace (reduction in steam requirement by 90 TPD), No addition of fuels, No addition of stacks and hence, No change in emissions. Thus, existing stack details remain unchanged. Thus, there is no change in air emissions due fuel burning from the Consented quantities.

iv. Hazardous Waste Generation in proposed DAS unit is only periodic due to use of catalyst (HW cat 4.2) (17 MT - once in 8 years) & will be accommodated within existing Consent quantity since existing generation is 508.73 MTPA while consented quantity is 2538.75 MTPA. Thus, there is no change in hazardous waste generation quantities also

Technical Committee Decision:

Technical Committee decided to recommend the case for change in product under product mix with a compliance of the following conditions.

(i) Industry shall comply with all the conditions stipulated in Environmental Clearance and ensure display/upload of six-monthly compliance monitoring report on their official website.

(ii) Industry should not manufacture any other product for which permission is not granted by the Board.

(iii) Industry shall ensure connectivity of OCEMS to Board server.

Agenda item No	**item No. 9**
Proposal No.	**MPCB- Consent - MPCB-CONSENT-0000147892**
Project Details	M/s. Kunjir Bioenergy India LLP, S.NO. 47/1,47/2,48,49,50,51,52 &53 (P), Village Mirwadi, Post Dahitane,Tal Daud,Dist Pune
NIPL Certificate	NIPL Certificate issued by Ultratech on 7th September 2022

Introduction:

This has reference to the online proposal submitted vide No MPCB consent - MPCB-CONSENT-**0000147892** along with the copies of documents seeking amendment in existing consent to operate under change in product mix under the provision of EIA Notification 2006 amended on 02.03.2021.

Exiting Clearances:

1. Environmental Clearance is granted to the industry vide FF. No. J-11011/305/2016-IA II (I) Dated 15th November 2018.
2. The unit has valid consent to operate vide No. Format1.0/CAC/UAN No. MPCB CONSENT-0000115463/CR/21100001011, Dated 21/10/2021

Project details:

A. **Products with change in product mix as below:**

Industry is having existing 60 KLPD distillery utilizes C- heavy molasses as raw material to produce rectified spirit (RS), Extra Neutral Alcohol (ENA) and ethanol. Industry has proposed increase ethanol production by 30 KLPD to use raw material namely heavy molasses and syrup.

Production details

Particulars	**Existing**	**After product Mix**
Capacity	60 KLPD	90 KLPD
Raw Material	C Molasses 230MT/day	B- heavy Molasses 290 MT/day
Production	1) ENA; 60 KLPD or Rectified spirit: 60KLPD or Ethanol: 60KLPD 2) Power; 2 MW	1) ENA; 60 KLPD or Rectified spirit: 90 KLPD or Ethanol: 90 KLPD 2) Power; 2 MW
Co products	CO2:45 TPD	CO2:68 TPD

B. Pollution load Details:

i) Water & Wastewater Aspect

Sr. No.	Particulars	Existing (60 KLPD)			After Product Mix (90 KLPD)		
		C- Molasses			B- heavy Molasses		
		Quantity in CMD	COD in mg/l	COD in kg/day	Quantity in CMD	COD in mg/l	COD in kg/day
1	Water Consumption in CMD	1125 (Fresh water 485+Recycle 640)	NA	NA	1059 (Fresh water 453+ Recycle 606	NA	NA
2	Industrial Effluent generation						
A	Spent Wash In CMD	514	140000	71960	436	130000	56680
B	Other in CMD	294	1500	441	324	1500	486
	Total	808		72401			57166

COD will reduce by 152358 kg/day using B- heavy Molasses.

Treatment System

a) **Trade Effluent:** Spent wash directly treated through multi-effect evaporator Followed Incineration Boiler. Condensate from MEE treated and other effluent treated in CPU.

b) **Other effluent: Industry has provided Effluent Treatment Plant and treated effluent is recycled in the process**

ii) Air Emission Load:

a) Flue Gas Emissions

Sr. No.	Stack Attached to	Fuel	Existing Fuel Consumption	Fuel Consumption after Change in Product Mix	Remark
1	Incineration Boiler 22.5 TPH	Conc. Spent wash + Coal	Conc. 120 MT/day + Coal: 24 MT/day	Conc. 100 MT/day + Coal: 20 MT/day	Reduced

iii) **Solid and Hazardous Waste Load: No hazardous waste generation**
Solid Waste;

Sr. No.	Particulars	Existing	After products Mix	Remark
1	Yeast Sludge	6 MT/day	6 MT/day	No change

Technical Committee Deliberations:

The proposed project was discussed on the basis of documents – NIPL Certificate and presentation made by the industry. Product wise load calculation in terms of wastewater, Air emissions & Hazardous waste generation were discussed. Existing consent to operate, Environmental Clearance, NIPL Certificate issued by Techno green Environmental Solutions and product mix Pro-forma are taken on the record.

Committee after due deliberations noticed that;

Technical Committee Decision:

Technical Committee decided to recommend the case for change in product under product mix with a compliance of the following conditions.

(i) Industry shall comply with all the conditions stipulated in Environmental Clearance and ensure display/upload of six-monthly compliance monitoring report on their official website.
(ii) Industry should not manufacture any other product for which permission is not granted by the Board.
(iii) Industry shall ensure connectivity of OCEMS to Board server.

Agenda item No	**item No .10**
Proposal No.	**MPCB-CONSENT-0000148145**
Project Details	**M/s. Ramdev Chemicals Pvt. Ltd.** Plot No. E-41/129 & 128/2, MIDC Tarapur, Tal & Dist:- Palghar.
NIPL Certificate	NIPL certificate issued by Goldfinch Engineering Systems Pvt. Ltd.

Introduction:

This has reference to the online proposal submitted vide No. MPCB-CONSENT-0000148145 along with the copies of documents seeking **Renewal with Amendment in Consent to operate based** on change in product mix under the provision of EIA Notification 2006 amended on 02.03.2021.

Exiting Clearances:

1. Environmental Clearance is granted to the industry for expansion ref no. SEIAA-EC-0000000097 dated 12.05.2017.
2. The unit has valid consent to operate vide No: - Format 1.0/CC/UAN No. 0000102914/CO/2108000987 dated 18.08.2021.

Project details:

A. Products with change in product mix as below:

Sr. No.	Name of product	As Per CTO, MT/M	Existing Qty., MT/M	Qty. After product Mix, MT/M	Remark
1	Intermediate-A	0.5	0.0	0.50	No change
2	2-Amino Pyridine	0.5	0	0.5	No change
3	Other Bulk Products	0.5	0	0.5	No change
4	Premaquine Phosphate IP/BP	0.1	0	0.1	No change
5	Benzocaine I.P.	10	1	11	Existing Product Increase by 1 MT/M.
6	Piroxicam USP	10	1	11	Existing Product Increase by 1 MT/M.
7	Enalaprilmateate EP/BP/USP	0.75	0	0.75	No change
8	Mesalamine	10	-10	0	Existing Product Deleted
9	Carbamezapin	5	-5	0	Existing Product Deleted

Sr. No.	Name of product	As Per CTO, MT/M	Existing Qty., MT/M	Qty. After product Mix, MT/M	Remark
10	Pregabalin-INT	2	0	2	No change
11	Entacapone	1	2	3	Existing Product Increase by 2 MT/M.
12	Meloxicam	10.79	0	10.79	No change
13	Metaxalone	3	2	5	Existing Product Increase by 2 MT/M.
14	Fenofibrate-INT	3	0	3	No change
15	Metaformin-INT	13.1	-13.1	0	Existing Product Deleted
16	Levetiracetam-INT	1	0	1	No change
17	Mirtazapine	1	1	2	Existing Product Increase by 1 MT/M.
18	Quitipine Fumarate-INT	1	0	1	No change
19	Ziprasidone	3	0	3	No change
20	Baclofen	0.1	0	0.1	No change
21	Meta Chloropropiophenone	2	-2	0	Existing Product Deleted
22	2-Amino-5-Methyl Thiazole	2.5	1.7	4.2	Existing Product Increase by 1.7 MT/M.
23	Methyl Benzothiazine Isopropyl Ester	8	2	10	Existing Product Increase by 2 MT/M.
24	6-Chloro 2-Oxindole	2	0	2	No change
25	1,3-Benzisothiazole Piperazine	2	0	2	No change
26	Celecoxib-INT(4-HBS)	10	0	10	No change
27	Clopidogrel Bisulphate	1	0	1	No change
28	Metoprolol	5	-5	0	Existing Product Deleted
29	Pentaprazole	2	0	2	No change
30	Etodolac-INT	5	-5	0	Existing Product Deleted

Sr. No.	Name of product	As Per CTO, MT/M	Existing Qty., MT/M	Qty. After product Mix, MT/M	Remark
31	Ciprofloxacin	5	0	5	No change
32	Zonisamide	1	0	1	No change
33	Montelukast	0.05	0	0.05	No change
34	Rabeprazole	2	0	2	No change
35	Sodium Barbital	3	0	3	No change
36	HCQS	3	0	3	No change
37	Propranol HCl	5	0	5	No change
38	Carbediliol (CV3)	3	0	3	No change
39	Glimepridel (GP4)	3	0	3	No change
40	PIP Acid	0.5	0	0.5	No change
41	Hydroxizine Pamoate	0.5	0	0.5	No change
42	Imipiramine HCl	0.5	0	0.5	No change
43	RBX	0.3	0	0.3	No change
44	4-TBD	5	0	5	No change
45	5 Nitro vaniline	2	0	2	No change
46	3,4 Dihydroxy 5 Nitro benzaldehyde	2	0	2	No change
47	5 - CEO	0.6	0.4	1	Existing Product Increase by 0.4 MT/M.
48	3-Piperazinyl -1,2 BenzisothiazoleHCL(ZP)	1	0	1	No change
49	Piroxicam Beta Cyclodextrine	1	0	1	No change
50	**Celecoxib Final**	**0**	**5**	**5**	**Added New Product**
51	**Aripriprazole**	**0**	**5**	**5**	**Added New Product**
52	**Pregabalin**	**0**	**5**	**5**	**Added New Product**

Sr. No.	Name of product	As Per CTO, MT/M	Existing Qty., MT/M	Qty. After product Mix, MT/M	Remark
53	**Sacubitril Valsartan**	**0**	**5**	**5**	**Added New Product**
54	**Retanilic Acid**	**0**	**2**	**2**	**Added New Product**
55	**Terbinafine**	**0**	**5**	**5**	**Added New Product**
56	**Dexritalinic acid**	**0**	**2**	**2**	**Added New Product**
Total Quantity		**154.29**	**0.00**	**154.29**	

Note: After Change in product mix total production capacity will be remains same i.e. 154.29 MT/M

Change in the product mix in its existing facility will be achieved by

I) Increasing production capacity of 8 existing products,
II) Addition of 7 new products
III) No Change in 35 Existing Products
IV) 6 Existing Products Deleted

B. Pollution load Details:

i) Water & Wastewater Aspect;

Before Product Mix

Sr. No.	Particulars	Quantity in CMD										
1	Water Consumption	183.44										
2	**Trade Effluent Generation**											
		Total Flow, CMD	**Flow, CMD**		**COD**				**TDS**			
			Strong	**Weak**	**Strong**		**Weak**		**Strong**		**Weak**	
					Mg/L	**Kg/Day**	**Mg/L**	**Kg/Day**	**Mg/L**	**Kg/Day**	**Mg/L**	**Kg/Day**
a	Process & Washing Activity	32.50	15	17.5	--	--	--	--	--	--	--	--

Sr. No.	Particulars	Quantity in CMD										
b	Cooling Tower & Boiler	32.64	0	32.64	--	--	--	--	--	--	--	--
Total (Trade)		**65.14**	**15**	**50.14**	**60739**	**910.81**	**340**	**17.0**	**24954**	**374.19**	**860**	**43.14**
c	Domestic Effluent Generation, CMD	5.67	5.67		0	0	600	3.40	0	0	600	3.40

Domestic -5.67 CMD + Industrial – 65.14 CMD total effluent 70.81 CMD

After Product Mix

Sr. No.	Particulars	Quantity in CMD										
1	Water Consumption	182.53										
2	**Trade Effluent Generation**											
Sr. No	**Particular**	**Total Flow, CMD**	**Flow, CMD**		**COD**				**TDS**			
			Strong	**Weak**	**Strong**		**Weak**		**Strong**		**Weak**	
					Mg/L	**Kg/Day**	**Mg/L**	**Kg/Day**	**Mg/L**	**Kg/Day**	**Mg/L**	**Kg/Day**
a	Process & Washing Activity	32.40	14.9	17.5	--	--	--	--	--	--	--	--
b	Cooling Tower & Boiler	32.64	0	32.64	--	--	--	--	--	--	--	--
Total (Trade)		**65.04**	**14.9**	**50.14**	**59215**	**882.3**	**340**	**17**	**24735**	**368.5**	**860**	**43.1**
c	Domestic Effluent Generation, CMD	5.67	5.67		0	0	600	3.40	0	0	600	3.40

Domestic - 5.67 CMD + Industrial – 65.04 CMD; Total effluent 70.71 CMD

- Water Consumption will reduce by 0.91 CMD
- Effluent generation will reduce by 0.1 CMD

- Average COD Load will reduce by 28.5 Kg/Day

- It is seen from above figures that, after change in product mix the COD & TDS values of effluent are decreased. The existing ETP is treating the waste water generated from the existing products to the consented standards. Since the waste water generated from the proposed product mix will have reduction in pollution load in terms of COD, BOD & TDS, existing ETP is adequate to treat the waste water generated after change in product mix. However, the adequacy study based on the values of existing waste water is also carried out and presented in upcoming slide.

Treatment System

a) Trade Effluent:

- Generated effluent is segregated into Strong stream & lean stream. High COD/TDS stream of 15 CMD from process is treated in Primary treatment, Stripper, MEE (design capacity of 20 CMD) followed by centrifuge. Condensate from MEE & lean stream (50.17 CMD) is treated in conventional ETP (design capacity of 100 CMD) consisting of primary (Collection tank, Neutralization tank, Equalization tank, primary clarifier/primary Settling tank), Secondary (Activated sludge process followed by Secondary clarifier), Tertiary treatment (Pressure Sand Filter, Activated Carbon Filter). After tertiary treatment effluent is pass through RO (design capacity of 100 CMD). RO permeate is recycled into the cooling tower & scrubbing and RO reject is fed to MEE to achieve Zero Liquid Discharge.
- Salts from MEE sent to CHWTSDF & solvents recovered from the stripper Sale to authorized Party/CHWTSDF
- Domestic sewage 5.67 CMD is being treated separately in STP having capacity 6 CMD. Treated domestic sewage after meeting the MPCB norms mentioned in the consent is being used for gardening.
- This existing effluent treatment facility is adequate even after proposed change in product mix.

ii) Air Emission load:

Sr. No.	Stack Attached to	Fuel	As per CTO	Existing Fuel Consumption	Fuel Consumption after Change in Product Mix	Stack Height	Remark
1	Boiler -1 (2 - TPH)	Coal	Coal: 84 Kg/Hr	Coal: 84 Kg/Hr	Coal: 84 Kg/Hr	30 m	No Change
2	Boiler -2 (0.65 - TPH)	LDO*	FO*: 25 Kg/Hr	LDO: 25 Kg/Hr	LDO-25 Kg/Hr	11 m	Switched over to cleaner fuel LDO in place of Furnace oil

3	Thermopack (3 Lakh Kcal/Hr)	LDO*	FO*: 4 Kg/Hr	LDO: 4 Kg/Hr	LDO: 4 Kg/Hr	11 m	Switched over to cleaner fuel LDO in place of Furnace oil
4	DS Set-1 (250 KVA)	HSD	HSD: 40 Ltr/Hr	HSD:40 Ltr/Hr	HSD:40 Ltr/Hr	3.5 m Above the Roof	No Change

Note: * Switched over to cleaner fuel LDO in place of Furnace oil

(i) Process Emissions:

Sr. No.	Stack Attached to	Scrubbing Media	Stack Height	Remark
S-1	Process Stack-I	Alkali Scrubber	7 m	No Change
S-2	Process Stack-II	Alkali Scrubber	7 m	No Change
S-3	Process Stack-III	Alkali Scrubber	7 m	No Change
S-4	Process Stack-IV	Alkali Scrubber	7 m	No Change
S-5	Process Stack-V	Alkali Scrubber	7 m	No Change
S-6	Process Stack-VI	Alkali Scrubber	7 m	No Change
S-7	Process Stack-VII	Alkali Scrubber	7 m	No Change
S-8	Process Stack-VIII	Alkali Scrubber	7 m	No Change
S-9	Process Stack-IX	Alkali Scrubber	7 m	No Change
S-10	Process Stack-X	Alkali Scrubber	7 m	No Change
S-11	Process Stack-XI	Alkali Scrubber	7 m	No Change
S-12	Process Stack-XII	Alkali Scrubber	7 m	No Change
S-13	Process Stack-XIII	Alkali Scrubber	7 m	No Change
S-14	Process Stack-XIV	Alkali Scrubber	7 m	No Change
S-15	Process Stack-XV	Alkali Scrubber	7 m	No Change
S-16	Process Stack-XVI	Alkali Scrubber	7 m	No Change

Note: There is no change in the process stacks, existing process scrubbers with heights are adequate to control the process air emission.

Flue Gas Emission and process emissions:

Stack No.	Source	APC System Provided/Proposed	Fuel of Type	Sulphur Content (in %)	Pollutant	Standard
S-1	Boiler -1 (2 - TPH)	Dust Collector & Wet Scrubber	Coal: 84 Kg/Hr	0.5	TPM	150 ug/Nm^3
					SO_2	20.16 Kg/Day
S-2	Boiler -2 (0.65 - TPH)	Stack with Adequate Height	LDO*: 25 Kg/Hr	1.8	TPM	150 ug/Nm^3
					SO_2	21.6 Kg/Day
S-3	Thermopack (3 Lakh Kcal/Hr)	Stack with Adequate Height	LDO*: 4 Kg/Hr	1.8	TPM	150 ug/Nm^3
					SO_2	3.45 Kg/Day
S-4	DS Set-1 (250 KVA)	Acoustic Enclosure	HSD:40 Ltr/Hr	1.0	TPM	150 ug/Nm^3
					SO_2	19.2 Kg/Day
S-5	Process Stack-I	Alkali Scrubber	--	--	Acid Mist	35 mg/Nm^3
S-6	Process Stack-II	Alkali Scrubber	--	--	Acid Mist	35 mg/Nm^3
S-7	Process Stack-III	Alkali Scrubber	--	--	Acid Mist	35 mg/Nm^3
S-8	Process Stack-IV	Alkali Scrubber	--	--	Acid Mist	35 mg/Nm^3
S-9	Process Stack-V	Alkali Scrubber	--	--	Acid Mist	35 mg/Nm^3

S-10	Process Stack-VI	Alkali Scrubber	--	--	Acid Mist	35 mg/Nm^3
S-11	Process Stack-VII	Alkali Scrubber	--	--	Acid Mist	35 mg/Nm^3
S-12	Process Stack-VIII	Alkali Scrubber	--	--	Acid Mist	35 mg/Nm^3
S-13	Process Stack-IX	Alkali Scrubber	--	--	Acid Mist	35 mg/Nm^3
S-14	Process Stack-X	Alkali Scrubber	--	--	Acid Mist	35 mg/Nm^3
S-15	Process Stack-XI	Alkali Scrubber	--	--	Acid Mist	35 mg/Nm^3
S-16	Process Stack-XII	Alkali Scrubber	--	--	Acid Mist	35 mg/Nm^3
S-17	Process Stack-XIII	Alkali Scrubber	--	--	Acid Mist	35 mg/Nm^3
S-18	Process Stack-XIV	Alkali Scrubber	--	--	Acid Mist	35 mg/Nm^3
S-19	Process Stack-XV	Alkali Scrubber	--	--	Acid Mist	35 mg/Nm^3
S-20	Process Stack-XVI	Alkali Scrubber	--	--	Acid Mist	35 g/Nm^3

*** Switched over to cleaner fuel LDO in place of Furnace oil**

iii) Hazardous Waste Load:

Sr. No	Type of Waste	Cat. No.	UOM	As Per CTO.	Existing Qty.	After CIPM Qty.	Disposal
1	Distillation Residue	20.3	MT/M	2.896	2.896	3.023	Sale to Auth. Party/ Pre-processing, Co-processing -Cement Plant / CHWTSDF
2	Chemical-containing residue arising from decontamination	34.1	Lit/M	500	500	500	CHWTSDF
3	Empty Barrels/ Containers /Liners contaminated with hazardous Chemicals/ Wastes	33.1	MT/M	4.85	4.85	4.85	Sale to Authorized reconditioner
4	Exhaust Air or Gas cleaning Residue	35.1	MT/M	1	1	1	CHWTSDF
5	Spent ion exchange resin containing toxic metals	35.2	Kg/M	4	4	4	CHWTSDF
6	Oil & Grease Skimming	35.4	Ltr/M	100	100	100	CHWTSDF
7	Used or Spent oil	5.1	Lit/M	9	9	9	Sale to authorized recycler
8	Contaminated cotton rags	33.2	Kg/M	150	150	150	CHWTSDF
9	Spent Carbon or Filter Medium	36.2	Kg/M	600	600	600	Pre-processing, Co-processing - Cement Plant /CHWTSDF
10	Sludge from Wet Scrubber	37.1	MT/M	4.5	4.5	4.5	Pre-processing, Co-processing & Cement /CHWTSDF
11	Off Specification products	28.4	MT/M	1	1	1	CHWTSDF
12	Spent Carbon from process	28.3	MT/M	0.454	0.454	0.369	Pre-processing, Co-processing - Cement /CHWTSDF

Sr. No	Type of Waste	Cat. No.	UOM	As Per CTO.	Existing Qty.	After CIPM Qty.	Disposal
13	Spent Catalyst	28.2	MT/M	0.03	0.03	0.03	CHWTSDF
14	Spent Solvent	28.6	MT/M	19.93	19.93	19.93	Sale to Auth. Party/CHWTSDF
15	Empty Barrels/Containers/ Liners	33.1	No/M	550	550	550	Sale to authorized reconditioner
16	Process Residue & Waste	28.1	MT/M	4.92	4.92	4.87	Pre-processing, Co-processing - Cement /CHWTSDF
17	Chemical Sludge from waste water treatment	35.3	MT/M	14.8	2.3	2.3	CHWTSDF
18	Concentration or evaporation residues (MEE Salts)*	37.3	MT/M		12.5	12.5	CHWTSDF

*** In the existing CTO, chemical sludge from waste water treatment is mentioned as 14.8 MT/M which is including MEE salts. Now, PP have bifurcated it i.e. 12.5 MT/M MEE salts and 2.5 MT/M is ETP sludge.**

Battery Waste				
1	Battery Waste		1 MT/A	Sale to Authorized Battery Recycler
E-Waste				
1	E-Waste		1 MT/A	Sale to Authorized E-Waste Recycler
Biomedical Waste				
1	Yellow	a) Solid Waste	1 Kg/M	CBMWTSDF

Technical Committee Deliberations:

The proposed project was discussed on the basis of documents – NIPL Certificate and presentation made by the industry. Product wise load calculation in terms of wastewater, Air emissions & Hazardous waste generation were discussed. Existing consent to operate, Environmental Clearance, NIPL Certificate issued by Goldfinch Engineering Systems Pvt. Ltd and product mix Performa are taken on the record.

After due deliberations, Committee noticed that:

1. Industry has applied for Change in Product Mix with no increase in the production quantity. The total production quantity will be remaining same after product mix.
2. The water consumption, trade effluent generation will remain same after product mix.
3. Even after change in product mix the COD & TDS values of effluent are decreased. The existing ETP is treating the waste water generated from the existing products to the consented standards. Since the waste water generated from the proposed product mix will have reduction in pollution load in terms of COD, BOD & TDS, existing ETP is adequate to treat the waste water generated after change in product mix
4. There is no change in the process stacks, existing process scrubbers with heights are adequate to control the process air emission.
5. In the existing CTO, chemical sludge from waste water treatment is mentioned as 14.8 MT/M which is including MEE salts. Now, PP have bifurcated it i.e. 12.5 MT/M MEE salts and 2.5 MT/M is ETP sludge
6. The overall hazardous waste quantity after product mix will remain same.
7. The overall pollution load is not increased after change in product – mix

Technical Committee Decision:

Technical Committee decided to recommend the case for change in product under product mix with a compliance of the following conditions;

(i) Industry shall comply with all the conditions stipulated in Environmental Clearance and ensure display/upload of six-monthly compliance monitoring report on their official website.
(ii) Industry should not manufacture any other product for which permission is not granted by the MPCB.
(iii) Industry shall ensure connectivity of OCEMS data to Boards server and transmit the data continuously for wastewater treatment facility.

Agenda Item No.	**Item No.11**
Proposal No.	MPCB-CONSENT-0000154116
Project Details	**M/s. Sumitomo Chemical India Ltd.** Address: Plot No. T-113, 137, 138, 251, MIDC Tarapur, Taluka & District – Palghar, Maharashtra - 401506
NIPL Certificate	NIPL certificate issued by M/s. Enviro Resources.

Introduction:

This has reference to the online proposal submitted vide No. MPCB-CONSENT-0000154116 along with the copies of documents seeking amendment in existing consent to operate under change in product-mix under the provision of EIA Notification 2006 amended on 02.03.2021.

Exiting Clearances:

1. Environmental Clearance is granted to the industry vide J-11011/71/2001-IA II dated 14.06.2002.
2. Consent to Operate granted vide no. 1.0/ AS(T)/ UAN No. MPCB CONSENT-0000120558/ CR/ 2202001628 dated 25/02/2022. The validity of the existing consent is up to 31/8/2025.

Project details:

A. Production Details:

Sr. No.	Product Name	Existing Quantity (MT/M)	Proposed Quantity (MT/M)	Total Quantity (MT/M)	Remarks
1	Cypermethrin Technical (CPM)	150	-99.6	50.4	Production capacity decreased by 99.6 MT/A
2	Fenvalerate Technical (FNV)	150	-99.6	50.4	Production capacity decreased by 99.6 MT/A
3	Meta Phenoxy Benzaldehyde (MPB)	300	-300	0	Product to be removed
4	d-Allethrin (Pynamin Forte / PPY)	150	-150	0	Product to be removed
5	Prallethrin Technical (ETOC)	300	-170.4	129.6	Production capacity decreased by 170.4 MT/A

6	d-Phenothrin (98 Transphenothrin Technical) (98 Sum)	288	0	288	No Change
7	Fenpropathrin Technical (DTL)	1170	499.2	1669.2	Production capacity increase by 499.2 MT/A
8	**Cyphenothrin Technical (GKL)**	**0**	**60**	**60**	**New Product**
9	**Pyriproxyfen Technical (SLV)**	**0**	**200.4**	**200.4**	**New Product**
10	**Dimefluthrin (PWL)**	**0**	**60**	**60**	**New Product**
	Total	**2508**	**0**	**2508**	

The overall production quantity will remain same. Maximum 8 Nos. of products shall be manufactured at any given point of time. The overall total production quantity will not exceed 2508 MT/M.

B. Pollution load Details:

(i) Water & Wastewater Aspect

Before Product Mix

Sr. No.	Particular	Quantity in CMD	Effluent Segregation in CMD		COD (Strong)		COD (Weak)		TDS (Strong)		TDS (Weak)	
			Strong	Weak	mg/l	Kg/day	mg/l	Kg/day	mg/l	Kg/day	mg/l	Kg/day
1	Water Consumption	127	Not applicable									
2	**Trade Effluent Generation**											
A	Process Activity	24	16	--	92155	344.33	--	--	661677	2509.2	--	--
B	Cooling Tower & Boiler	56	--	24	--	--	350	19.6	--	--	900	50.4
C	Gardening	37	--	--	--	--	--	--	--	--	--	--
D	**Total**	**117**	**16**	**24**	**92155**	**344.33**	**350**	**19.6**	**661677**	**2509.2**	**900**	**50.4**

3	Domestic Effluent Generation, CMD	10	--	8	--	--	300	3	--	--	--	--

After Product Mix:

Sr. No.	Particular	Quantity in CMD	Effluent Segregation in CMD		COD (Strong)		COD (Weak)		TDS (Strong)		TDS (Weak)	
			Strong	Weak	mg/l	Kg/day	mg/l	Kg/day	mg/l	Kg/day	mg/l	Kg/day
1	Water Consumption	125	Not applicable									
2	**Trade Effluent Generation**											
A	Process Activity	22	16	--	114662	330.37	--	--	554086.1	2495.6	--	--
B	Cooling Tower & Boiler	56	--	24	--	--	350	19.6	--	--	900	50.4
C	Gardening	37	--	--	--	--	--	--	--	--	--	--
D	**Total**	**115**	**16**	**24**	**114662**	**330.37**	**350**	**19.6**	**554086.1**	**2495.6**	**900**	**50.4**
3	Domestic Effluent Generation, CMD	10	--	8	--	--	300	3	--	--	--	--

- Water Consumption will decrease 127 CMD to 125 CMD

- COD load for trade effluent will reduce by 13.96 Kg/day
- TDS load for trade effluent will reduce by 13.6 Kg/day

Treatment System

a) Trade Effluent:

Industry has segregated trade effluent into weak stream & strong stream and provided Effluent Treatment Plant (ETP) comprising of;

- **Strong COD/TDS stream of 16 CMD:** Treatment system comprising of Primary (Collection tank, Neutralization tank, Equalization tank, Flash mixer, Primary Clarifier/Primary Settling Tank) , Multi effect evaporator (3 stage) with design capacity of 20 CMD followed by ATFD. The MEE condensate is treated in weak stream ETP.

- **Weak COD/TDS stream of 24 CMD:** Treatment system comprising of Primary (Collection tank, Neutralization tank, Equalization tank, Flash mixer, Primary Clarifier/Primary Settling Tank), Secondary (Activated sludge process), Tertiary (Pressure sand filter, Activated carbon filter) with design capacity of 40 CMD

b) Domestic Effluent:

The domestic effluent is treated in sewage treatment plant of capacity 12 CMD.

(ii) Air Emission Load :

Sr. No.	Source	Fuel	Before Product Mix	After Product Mix	Remark
1	Boiler No.1 (1.5 TPH)	Briquettes (Solid) / LDO	4 MT/Day	4 MT/Day	No Change
2	Boiler -2 (1.5 TPH) (Standby)				
3	(S4) DG Set – 1	750 kVA	110 Lit/day	110 Lit/day	No Change
	(S5) DG Set – 2	750 kVA			

(iii) Hazardous Waste Load:

Sr. No.	Description	Category No.	UOM	Before Product Mix	After Product mix	Remark
1	Used or spent oil	5.1	MT/A	1	1	No change
2	Wastes or residues containing oil	5.2	MT/A	0.5	0.5	No change
3	Contaminated aromatic, aliphatic or napthenic solvents may or may not be fit for reuse.	20.1	MT/A	1	1	No change
4	Spent solvents	20.2	MT/A	1	1	No change
5	Process wastes, residues and sludges	21.1	MT/A	0.2	0.2	No change
6	Process wastes or By – Products (HCL Solution, Sodium Sulphite Solution, Aluminium Chloride Solution, Phenolic Solution, Potassium Bromide Solution)	29.1	MT/A	2844	2844	No change
7	Sludge containing residual pesticides	29.2	MT/A	15	15	No change
8	Date-expired and off-specification Pesticides	29.3	MT/A	0.3	0.3	No change
9	Discarded Liners used for Haz. Chemicals	33.1	MT/A	0.5	0.5	No change
10	Empty barrels /containers /liners contaminated with hazardous chemicals /wastes	33.1	Nos./A	1700	1700	No change
11	Spent ion exchange resin containing toxic metals	35.2	MT/A	0.4	0.4	No change
12	MEE Salts	38.3	MT/A	922	922	No change
13	Oil and grease skimming	35.4	MT/A	0.4	0.4	No change
14	ETP Sludge	35.3	MT/A	360	360	No change
15	Spent catalysts	29.5	MT/A	0.3	0.3	No change
16	Spent carbon or filter medium	36.2	MT/A	1.2	1.2	No change
17	Miscellaneous Wastes contaminated glass, wool, rock wool, asbestos, Teflon, used gaskets, Teflon impregnated/graphite rope glands, waste lumina separated from dryer, thermocol, used safety items.	other	MT/A	4	4	No change

All 17 nos. of category of Hazardous wastes remain unchanged.

Technical Committee Deliberations:

The proposed project was discussed on the basis of documents – NIPL Certificate and presentation made by the industry. Product wise load calculation in terms of Wastewater, Air emissions & Hazardous waste generation was discussed. Existing Consent to Operate, Environmental Clearance, NIPL Certificate issued by M/s. Enviro Resources and Product – Mix Proforma are taken on the record.

After due deliberations, Committee noticed that:

i. Industry has applied for Change in Product Mix with no increase in the production quantity. The total production quantity will be remaining same after product mix i.e., 2508 MT/ M.
ii. The water consumption will decrease by 2 CMD whereas trade effluent generation will remain same after product mix.
iii. COD load will reduce by 13.96 Kg/day and TDS load will reduce by 13.6 Kg/day
iv. Committee noticed that, industry have segregated effluent into strong and weak stream and has provided separate treatment for segregated trade effluent.
v. There is no change in the process stacks, existing process scrubbers with heights are adequate to control the process air emission
vi. The overall hazardous waste quantity after product mix will remain same.
vii. The overall pollution load is not increased after change in product – mix.

Technical Committee Decision:

Technical Committee decided to recommend the case for change in product under product mix with a compliance of the following conditions.

(i) Industry shall comply with all the conditions stipulated in Environmental Clearance and ensure display/upload of six-monthly compliance monitoring report on their official website.
(ii) Industry should not manufacture any other product for which permission is not granted by the Board.
(iii) Industry shall ensure connectivity of OCEMS to Board server.

Agenda item No	**item No.12**
Proposal No.	**MPCB-CONSENT-0000150853**
Project Details	**M/s. Clean Science & Technology Limited.** **Plot No-28,MIDC Kurkumbh, Tq-Daund Dist.- Pune 413802**
NIPL Certificate	NIPL Certificate issued by Goldfinch Engineering Systems Pvt. Ltd.

Introduction:

This has reference to the online proposal submitted vide No. MPCB-CONSENT-0000150853 along with the copies of documents seeking amendment in existing consent to operate under change in product mix under the provision of EIA Notification 2006 amended on 02.03.2021.

Exiting Clearances:

1. Environmental Clearance is granted to the industry for expansion ref no. SEAC-2014/CR-85/TC-2 dated 04.06.2016. The unit has valid consent to operate vide No: - Format1.0/CC/UAN No. 0000103840/CR/2106000635 dated 14.06.2021.
2. Industry has submitted proposal on PARIVESH portal on 09.12.2022. Single Window No (SW/2350/2022)

Project details:

A. Products with change in product mix as below:

Sr. No	Name of Product under API & Intermediates	Existing Production Quantity as per CTO, MT/A	Addition (+)/ Deletion (-) (TPA)	Proposed Production Quantity, MT/A
1	Hydroquinone/Catechol/Mono Methyl Ether of Hydroquinone (MEHQ)/Guaiacol & Derivatives	8400	(-) 1200	7200
2	4-Methoxy Acetophenone / 4- Methoxy Propiophenone	3000	0	3000
3	Butylated Hydroxy Anisole (BHA) & Derivatives (Route 1- Without Using Tolene / Route 2- By Using Tolene)	1800	0	1800

4	4- Methyl Catechol	100	(-) 100	0
5	Anisole & Derivatives	1200	(-) 1100	100
6	Zeolite/Zirconium Catalyst	50	0	50
7	Veratrole & Derivatives	0	(+) 1200	1200
8	Guethol	0	(+) 200	200
9	TBT (Tertiary Butyl Toluene)	0	(+) 540	540
	Total	**14550**	**-460**	**14090**

i. **Change in the product mix in its existing facility is achieved by Addition of 3 new products, No Change in 3 Existing Products, decrease in production capacity of 2 existing products & Deletion of 1 Existing Products.**

ii. **The proposed activity is in such a way that the total production will decreased i.e. 460 MT/A, keeping the pollution load within the consent limit.**

B. Pollution load Details:

i) Water & Wastewater Aspect

Before Product Mix

Sr. No.	Particulars	Quantity in CMD			
1	Water Consumption	568.4			
2	**Trade Effluent Generation**				
Sr. No	**Particular**	**Total Flow, CMD**	**Flow, CMD**	**COD**	**TDS**

Sr. No.	Particulars	Quantity in CMD											
			Strong	Weak	Strong		Weak		Strong		Weak		
					Mg/L	Kg/Day	Mg/L	Kg/Day	Mg/L	Kg/Day	Mg/L	Kg/Day	
a	Process & Washing Activity	42.8	0	42.8	--	--	--	--	--	--	--	--	
b	Cooling Tower & Boiler	114.4	0	114.4	--	--	--	--	--	--	--	--	
Total (Trade)		**157.2**	**0**	**157.2**	--	--	**9652**	**1516.9**	--	--	**7155**	**1124.5**	
c	Domestic Effluent Generation, CMD	19	0	19	--	--	600	11.4	--	--	600	11.4	
Grand Total		**176.2**	0	**176.2**	--	--	**8676**	**1528.3**	--	--	**6448.2**	**1135.9**	

After Product Mix

Sr. No.	Particulars	Quantity in CMD											
1	Water Consumption	568.4											
2	**Trade Effluent Generation**												
Sr. No	**Particular**	**Total Flow, CMD**	**Flow, CMD**		**COD**				**TDS**				
			Strong	**Weak**	**Strong**		**Weak**		**Strong**		**Weak**		
					Mg/L	**Kg/Day**	**Mg/L**	**Kg/Day**	**Mg/L**	**Kg/Day**	**Mg/L**	**Kg/Day**	
a	Process & Washing Activity	39.8	0	39.8	--	--	--	--	--	--	--	--	

Sr. No.	Particulars	Quantity in CMD										
b	Cooling Tower & Boiler	114.4	0	114.4	--	--	--	--	--	--	--	--
Total (Trade)		**154.1**	**0**	**154.1**	**0**	**0**	**9524**	**1467.5**	**0**	**0**	**6180**	**952.5**
c	Domestic Effluent Generation, CMD	19	0	19	--	--	--	--	--	--	--	--
	Grand Total	**173.1**	**0**	**173.1**	--	--	**8544**	**1479.1**	--	--	**5568**	**963.9**

- No Change in Water Consumption
- Effluent generation will reduce by: 3.1 CMD
- Average COD Load will reduce by: 49.2 Kg/Day

- **It is seen from above figures that, after change in product mix the COD, BOD & TDS values of effluent are reducing by about 3.21%, 20.57 % & 15.14 % respectively**

- **The existing ETP is treating the waste water generated from the existing products to the consented standards. Since the waste water generated from the proposed product mix will be reduced by 3.1 CMD and has the reduction pollution parameters viz. COD, BOD and TDS than the existing production profile, it is clear that the existing ETP is adequate to treat the waste water generated after the change in the product mix. However, the adequacy analysis is based on the values of existing waste water parameters as they are the same as the parameters of the waste water generated from the proposed product mix.**

- **Pollution load of all parameters are calculated on the basis of worst case scenario .**

Treatment System

Trade Effluent:

- Effluent Treatment Plant (ETP) of Design capacity of 192.00 CMD

- Consisting of Primary (Collection tank, Neutralization tank, Equalization tank, Flash mixer, Primary Clarifier/Primary Settling tank), Secondary /(Activated sludge process), Tertiary Treatment (Pressure sand filter, Activated carbon filter).
- Advance treatment (Reverse Osmosis, Multi effect evaporator) for treatment of 173.1 CMD of trade and Domestic effluent.
- The Effluent plant shall operate to treat the trade effluent and recycle the entire treated effluent into the process for various purpose such as for cooling, process and scrubbing with metering system so as to achieve Zero Liquid Discharge.
- There shall be no discharge on land or outside factory premises.
- Sewage is being treated in secondary treatment of ETP as combined treatment.
- MEE salts are dispose to CHWTSDF.
- This existing effluent treatment facility is adequate even after proposed change in product mix.

ii) Air Emission Load:

Sr. No.	Stack Attached to	Fuel	Existing Fuel Consumption	Fuel Consumption after Change in Product Mix	APC system	Stack Height
S-1	Boiler-1 (5 TPH)	Coal	16 MT/Day	16 MT/Day	Fabric Bag Filter/ Multi Cyclone	30m
	Thermopack (8 Lacs Kcal/Hr)	Coal	2.5 MT/ Day	2.5 MT/Day	Fabric Bag Filter /Multi Cyclone	
S-2	Boiler (12 TPH)	Coal	25 MT/Day	25 MT/Day	Fabric Bag Filter/ multi Cyclone	35 m
S-3	Thermopack (4Lacs Kcal/Hr)	Coal	1.5 MT/ Day	1.5 MT/Day	Fabric Bag Filter/ multi Cyclone	30 m
	Thermopack (10 Lacs Kcal/Hr)	Coal	03 MT/Day	3 MT/Day	Fabric Bag Filter/ multi Cyclone	
S-4	DG Set (750 KVA)	HSD	50 Ltr/Hr	50 Ltr/Hr	Acoustic Enclosure Stack	22 m

Sr. No.	Stack Attached to	Fuel	Existing Fuel Consumption	Fuel Consumption after Change in Product Mix	APC system	Stack Height
	DG Set (1010 KVA)	HSD	70 Ltr/Hr	70 Lit/Hr	Acoustic Enclosure Stack	

Flue Gas Emissions:-

Sr. No.	Source	Parameters:	Before change in product-mix	After change in product-mix	MPCB Norms
S-1	Boiler-1	TPM (From Coal)	40-60 mg/Nm^3	No Change	150 mg/Nm^3
		SO_2 (Coal)	9-25 kg/day	No Change	160 Kg/day
	Thermopack	TPM (From Coal)	40-60 mg/Nm^3	No Change	150 mg/Nm^3
		SO_2 (Coal)	9-25 kg/day	No Change	25 kg/day
S-2	Boiler	TPM (From Coal)	40-60 mg/Nm^3	No Change	150 mg/Nm^3
		SO_2 (Coal)	9-25 kg/day	No Change	250 Kg/day
S-3	Thermopack	TPM (From Coal)	40-60 mg/Nm^3	No Change	150 mg/Nm^3
		SO_2 (Coal)	9-25 kg/day	No Change	15 Kg/day
	Thermopack	TPM (From Coal)	40-60 mg/Nm^3	No Change	150 mg/Nm^3
		SO_2 (Coal)	9-25 kg/day	No Change	30 Kg/day
S-4	DG Set-1	TPM (From HSD)	40-70 mg/Nm^3	No Change	150 mg/Nm^3

		SO_2 (From HSD)	1-3 kg/day	No Change	24 Kg/day
	DG Set-2	TPM (From HSD)	40-70 mg/Nm^3	No Change	150 mg/Nm^3
		SO_2 (From HSD)	1-3 kg/day	No Change	34 Kg/day

iii) Hazardous Waste Load

Sr. No	Type of Waste	Cat. No.	As Per EC	As Per CTO.	Existing Qty.	After Change in Product Mix Qty.	UOM	Disposal
1	Process residue & Waste	28.1	1.305	1.305	1.305	1.305	MT/M	CHWTSDF
2	Chemical Sludge from waste water treatment	35.3	5*	5*	60	60	MT/M	CHWTSDF
3	Empty barrels/ containers/ liners contaminated with hazardous chemicals	33.1	15	15	15	15	No/M	Sale to Authorized Party/ CHWTSDF
4	Process residue (DMC)	28.1	650	650	650	53.6	MT/A	Sale to Authorized Party
5	Process residue (Acetic Acid/Propionic Acid)	28.1	1250	1250	1248.3	1248.3	MT/A	Sale to Authorized Party
6	Process residue (10% phenol)	28.1	100	100	100	8.2	MT/A	Sale to Authorized Party
7	Process residue (Sodium Sulphate 100%)	28.1	-	419.75*	0	480	MT/A	Sale to Authorized Party
10	Process Residue 4-Ethoxy phenol	28.1	-	-	0	200	MT/A	Sale to Authorized Party

*** MPCB had put a condition in current valid CTO for amendment in EC for Sodium sulphate and ETP sludge.** Sodium Sulphate was used as dehydrating agent in manufacturing process of some products. As PP have removed the dehydrating step from the manufacturing process, there will not be any generation of Sodium suphate from existing activity. Hence, **while applying for EC amendment, PP applied for amendment in EC, for ETP sludge i.e. from 5 MT/M to 60 MT/M only and have omitted the plan of amendment in EC for Sodium sulphate 419.75 MT/M.**

Note: After Change in Product Mix, Hazardous waste is decreased from 2004.8 to 1998.2 MT/A i.e. 6.6 MT/A. While calculating total hazardous waste from existing production profile, Sodium Sulphate is not considered as PP is not applied it for amendment in EC

Non-Hazardous Waste

Sr. No	Type of Waste	As Per EC	As Per CTO	Existing Qty.	After Change in Product Mix Qty.	UOM	Disposal
1	Plastic waste	150 - 200 Kg/M	400	400	400	Kg/M	Sale to Recycler
2	Packing Material		2	2	2	MT/A	Sale to Recycler
3	Boiler Ash	3	6	6	6	MT/Day	Sale to Brick Manufacturer

Technical Committee Deliberations:

The proposed project was discussed on the basis of documents – NIPL Certificate and presentation made by the industry. Product wise load calculation in terms of wastewater, Air emissions & Hazardous waste generation were discussed. Existing consent to operate, Environmental Clearance, NIPL Certificate issued by Goldfinch Engineering Systems Pvt. Ltd and product mix Proforma are taken on the record.

Committee after due deliberations noticed that;

i. Change in the product mix in its existing facility is achieved by Addition of 3 new products, No Change in 3 Existing Products, decrease in production capacity of 2 existing products & Deletion of 1 Existing Products.
ii. The proposed activity is in such a way that the total production will decreased i.e. 460 MT/A, keeping the pollution load within the consent limit.

iii. It is seen from above figures that, after change in product mix the COD, BOD & TDS values of effluent are reducing by about 3.21%, 20.57 % & 15.14 % respectively.

iv. The existing ETP is treating the waste water generated from the existing products to the consented standards. Since the waste water generated from the proposed product mix will be reduced by 3.1 CMD and has the reduction pollution parameters viz. COD, BOD and TDS than the existing production profile, it is clear that the existing ETP is adequate to treat the waste water generated after the change in the product mix. However, the adequacy analysis is based on the values of existing waste water parameters as they are the same as the parameters of the waste water generated from the proposed product mix.

v. Pollution load of all parameters are calculated on the basis of worst case scenario

vi. There is no change in the process stacks, existing process scrubbers with heights are adequate to control the process air emission.

vii. After Change in Product Mix, Hazardous waste is decreased from 2004.8 to 1998.2 MT/A i.e. 6.6 MT/A. While calculating total hazardous waste from existing production profile, Sodium Sulphate is not considered as PP is not applied it for amendment in EC.

viii. The overall pollution load is not increased after change in product – mix.

Technical Committee Decision:

Technical Committee decided to recommend the case for change in product under product mix with a compliance of the following conditions.

(i) Industry shall comply with all the conditions stipulated in Environmental Clearance and ensure display/upload of six-monthly compliance monitoring report on their official website.

(ii) Industry should not manufacture any other product for which permission is not granted by the Board.

(iii) Industry shall ensure connectivity of OCEMS to Board server.

Agenda item No	**item no 13**
Proposal No.	**MPCB-CONSENT-0000155539**
Project Details	**M/s. Sarex Overseas Ltd.** Plot No. N 129,130,131 & N 132 MIDC Tarapur
NIPL Certificate	NIPL certificate issued by M/s.

The committee was informed that, M/s. **Sarex Overseas Ltd** had expressed their inability to attend the said meeting. The committee considered the same and it was decided to defer the case.

Agenda item No	**item No. 14**
Proposal No.	**MPCB-CONSENT-0000156815**
Project Details	**M/s. Emcure Pharmaceuticals Ltd.** Plot No. 12/1, 12/2, F II Block, MIDC Pimpri, Haveli, Pune-Pune
NIPL Certificate	NIPL certificate issued by Goldfinch Engineering Systems Pvt. Ltd.

Introduction:

This has reference to the online proposal submitted vide No. MPCB-CONSENT-0000156815 along with the copies of documents seeking amendment in existing consent to operate under change in product mix under the provision of EIA Notification 2006 amended on 02.03.2021.

Exiting Clearances:

1. Environmental Clearance is granted to the industry for expansion ref no. SEAC-2511/CR-741/TC2 dated 12.05.2014. The unit has valid consent to operate vide No: - Format1.0/AS(T)/UAN No. 0000124193/CR/2207000763 dated 15.07.2022.
2. Industry has submitted proposal on PARIVESH portal on 14.01.2023. Single Window No (SW/2362/2022)

Project details:

A. Products with change in product mix as below:

Sr. No	Name Of Product	Existing Production Quantity as per CTO, MT/M	Proposed Production Quantity, MT/M
1	S- Amlodipine Besilate	2.0	2.0
	API and Pharmaceutical Intermediates (#)		
	R & D Products (Max. 100 Kg/M)		

(#) List of Products under API and Pharmaceutical Intermediates is as below;

1	Acetozolamide	Desvenlafaxine	Cidofovir
2	Dexrabeprazole sodium	Dexmedetomidine Hydrochloride	Milrinone
3	Ferric Carboxy Maltose	S (-) Pantoprazole Sodium	Dydrogesterone
4	Metoprolol Succinate	Pentamidine Isethionate	Progesterone
5	Sevelamer Hydrochloride	Nefopam Hydrochloride	R & D Products (Max. 100 Kg/M)
6	Mefloquine Hydrochloride	Adenosine	
7	Tenofovir Disoproxil Fumarate	S (-) Amlodipine Besilate	
8	Lisdexaphetamine Dimesylate	Atenolol	
9	Seratrodast	Dexketoprofen Trometamol	
10	Tolperisone Hydrochloride	Febuxostat	
11	Cilnidipine	Iron Sucrose Complex	
12	Calcium Citrate Malate	Isosulfan Blue	
13	Amlexanox	Metoclopramide Hydrochloride	
14	Canrenone	Prochlorperazine Edisylate	
15	Emtricitabine	Etodolac	
16	Lafutidine	Zoledronic Acid	
17	Lumefantrine	Triamterene	
18	Carprofen	Neostigmine Methylsulphate	
19	Levosulpiride	Ritonavir	
20	(S)- Pregabalin		
21	Troxipide		
22	Cobicistat		

23	Esomeprazole (ESP09)		
24	Ferrous Ascorbate		
25	Maraviroc		
26	Sucroferric Oxyhydroxide		
27	Dexmethylphenidate Hydrochloride		
28	Levocarnitine		
29	Lamivudine		
30	Nevirapine		
31	Topiramate		

Note:

i. **In EC and in the current valid CTO combined capacity of the product is mentioned under API and Pharmaceutical intermediates without mentioning the names of individual products. However, while in the application of the CTO available on the MPCB portal manufacturing process of 50 number of products with names were uploaded.**

ii. **Calculation of pollution load is done on the basis of list of products mentioned under API and Pharmaceutical Intermediates uploaded by PP on the MPCB portal. Detailed list of product before & after change in product mix is as mentioned above;**

i. **After the change in product mix, the total combined production capacity of the plant will be remained same i.e., 2.0 MT/M.**

ii. **Change in the product mix in its existing facility will be achieved by Addition of 4 new products and inclusion of R & D product. No Change in 19 Existing Products, Deletion of 31 Existing Products.**

iii. **The proposed activity is in such a way that the total production will remains same i.e. 2.0 MT/M, keeping the pollution load within the consent limit.**

iv. **Pollution load is calculated on the basis of worst case scenario i.e. considering manufacturing of each product to the tune of 2 MT/M. Emcure can manufacture combination of products or each product to the tune of 2 MT/M (as per CTO).**

B. Pollution load Details:

i) Water & Wastewater Aspect

Before Product Mix

Sr. No.	Particulars	Quantity in CMD											
1	Water Consumption	80.8											
2	**Trade Effluent Generation**												
Sr. No	**Particular**	**Total Flow, CMD**	**Flow, CMD**		**COD**				**TDS**			
			Strong	**Weak**	**Strong**		**Weak**		**Strong**		**Weak**	
					Mg/L	**Kg/Day**	**Mg/L**	**Kg/Day**	**Mg/L**	**Kg/Day**	**Mg/L**	**Kg/Day**
a	Process & Washing Activity	16	0	16	--	--	--	--	--	--	--	--
b	Cooling Tower & Boiler	3.0	0	3.0	--	--	--	--	--	--	--	--
Total (Trade)		**19.0**	0	**19.0**	**0**	**0**	**8453**	**160.6**	**0**	**0**	**2721**	**51.7**
c	Domestic Effluent Generation, CMD	5	5.0		--	--	600	3.0	--	--	600	3.0
d	Total Effluent	24.0	24.0		0	0	6816	163.6	0	0	2279	54.7

Domestic -5 CMD + Industrial – 19 CMD total effluent 24 CMD

After Product Mix

Sr. No.	Particulars	Quantity in CMD											
1	Water Consumption	80.8											
2	**Trade Effluent Generation**												
Sr. No	**Particular**	**Total Flow, CMD**	**Flow, CMD**		**COD**				**TDS**			
			Strong	**Weak**	**Strong**		**Weak**		**Strong**		**Weak**	
					Mg/L	**Kg/Day**	**Mg/L**	**Kg/Day**	**Mg/L**	**Kg/Day**	**Mg/L**	**Kg/Day**
a	Process & Washing Activity	16	0	16	--	--	--	--	--	--	--	--
b	Cooling Tower & Boiler	3.0	0	3.0	--	--	--	--	--	--	--	--
Total (Trade)		**19.0**	0	**19.0**	**0**	**0**	**8453**	**160.6**	**0**	**0**	**2721**	**51.7**
c	Domestic Effluent Generation, CMD	9	5.0		--	--	600	3.0	--	--	600	3.0
d	Total Effluent	24.0	24.0		0	0	6816	163.6	0	0	2279	54.7

Domestic -5 CMD + Industrial – 19 CMD total effluent 24 CMD

- No change in Water Consumption, Effluent generation and its quality.
- **It is seen from the above figures that, after a change in product mix there is no change in the COD, BOD & TDS values of effluent coming from process and utility.**
- **The existing ETP is treating the waste water generated from the existing products to the consented standards. Since the waste water generated from the proposed product mix has the same parameters as the existing it is clear that the existing ETP is adequate to treat the waste water generated after the change in the product mix. However, the adequacy analysis is based on the values of existing waste water parameters as they are the same as the parameters of the waste water generated from the proposed product mix.**
- **Pollution load of all parameters are calculated on the basis of worst case scenario i.e. considering manufacturing of each product to the tune of 2 MT/M.**

Treatment System

a) Trade Effluent:

- The generated waste water is being treated in full-fledged Effluent Treatment Plant (ETP) of designed capacity of 25.00 CMD. Existing ETP is consisting of Primary (Collection tank, Neutralization tank, Equalization tank, Flash mixer, Primary Clarifier/Primary Settling Tank), Secondary (Activated sludge process), Tertiary (Pressure sand filter, activated carbon filter), Sludge treatment (Sludge drying bed) for the treatment of 19 CMD of trade effluent from process.
- Further primary treated sewage effluent 5 CMD combine to Effluent Treatment plant at Secondary stage (Aeration Tank). Total 24 CMD trade effluent is being treated in the existing ETP having designed capacity of 25.00 CMD. As per the existing CTO treated effluent 9.5 CMD is being recycled/reused for utility purposes. Remaining is being discharged on land for gardening within premise after confirming MPCB standards.
- This existing effluent treatment facility is adequate even after proposed change in product mix.

ii) Air Emission:

Sr. No.	Stack Attached to	As per CTO	Existing Fuel Consumption	Fuel Consumption after Change in Product Mix	Stack Height	Remark
1	Boiler-1 (0.6 TPH stand By)	LDO: 432 Lit/Day	LDO: 432 Lit/Day	LDO: 432 Lit/Day	30 m (Combined stack)	No Change
	Boiler-2 (1.5 TPH)	FO: 78* Kg/Hr	LDO*-78 Kg/Hr	LDO-78 Kg/Hr Or LSHS-78 Kg/Hr		Switched over to cleaner fuel LDO/LSHS in place of Furnace oil
2	DS Set-1 (500 KVA)	HSD- 22 Lit/Hr	HSD- 22 Lit/Hr	HSD- 22 Lit/Hr	3 m (from above the roof)	No Change
3	DS Set-1 (500 KVA)				3 m (from above the roof)	

4	Process Vent-1	--	--	--	10 m	No Change
5	Process Vent-2	--	--	--	5 m	No Change
6	Process Vent-3	--	--	--	5 m	No Change

Note: * Switched over to cleaner fuel LDO/LSHS in place of Furnace oil

Fuel Gas Emission & Process Emission

Stack No.	Source	APC System provided/proposed	Fuel of Type	Sulphur Content (in %)	Pollutant	Standard
S-1	Boiler-1	Stack	LDO 432 Lit/Day	1.8	TPM	50 Mg/Nm3
					SO_2	15.55 Kg/Day
	Boiler-2	Stack	LDO-78 Kg/Hr or LSHS-78 kg/Hr	1.8	TPM	50 Mg/Nm3
					SO_2	67.4 Kg/Day
S-2	DS Set-1 (500 KVA)	Acoustic Enclosure	HSD: 22 Lit/Hr	1.0	TPM	50 Mg/Nm3
S-3	DS Set-2 (500 KVA)	Acoustic Enclosure			SO_2	3.52 Kg/Day
S-4	Process Vent-1	Scrubber	--	--	Acid Mist	35 mg/Nm^3
S-5	Process Vent-2	Scrubber	--	--	Acid Mist	35 mg/Nm^3
S-6	Process Vent-3	Scrubber	--	--	Acid Mist	35 mg/Nm^3

iii) Hazardous Waste Load;

Sr. No	Type of Waste	Cat. No.	As Per CTO. MT/M	Existing Qty. MT/M	After CIPM Qty. MT/M	Disposal
1	Used/Spent Oil	5.1	0.21	0.21	0.21	Sale to authorized party / CHWTSDF
2	Process Residue and wastes	28.1	1.1	1.1	1.5	CHWTSDF
3	Off specification products	28.4	1	1	1	CHWTSTF
4	Date-expired products	28.5	3	3	3	CHWTSTF
5	Spent solvents	20.2	7.5	7.5	10.0	Sale to authorized party / CHWTSDF
6	Chemical sludge from waste water	35.3	5	5	2.5	Co-Processing/ Pre-Processing/ CHWTSTF
7	Spent catalyst	28.2	0.5	0.5	0.1	Authorized recycler/ CHWTSDF
8	Empty barrels /containers /liners contaminated with hazardous chemicals/wastes	33.1	0.5	0.5	0.5	Sale to authorized party / CHWTSDF
	Total Hazardous Waste Quantity (MT/M)		**18.81**	**18.81**	**18.81**	--
Note: There is no change in the Overall total hazardous waste quantity even after proposed Change in product mix.						

E – Waste

Sr. No	Type of Waste	Qty.	Disposal Path
1	E - Waste	100 Kg/Annum	Authorized re-processor

There is no change in E-waste quantity after proposed Change in product mix.

Biomedical Waste;

Sr. No	Type of Waste	Qty.	Disposal Path
1	Yellow- (Biomedical Waste-Yellow colored non-chlorinated plastic bags)	50 Kg/M	Common BMW Treatment Facility
2	Red - (Biomedical Waste- Autoclave safe plastic bags or containers)	50 Kg/M	Common BMW Treatment Facility

There is no change in Biomedical waste quantity after proposed Change in product mix.

Technical Committee Deliberations:

The proposed project was discussed on the basis of documents – NIPL Certificate and presentation made by the industry. Product wise load calculation in terms of wastewater, Air emissions & Hazardous waste generation were discussed. Existing consent to operate, Environmental Clearance, NIPL Certificate issued by Goldfinch Engineering Systems Pvt. Ltd and product mix Performa are taken on the record.

Committee after due deliberations noticed that;

i. In EC and in the current valid CTO combined capacity of the product is mentioned under API and Pharmaceutical intermediates without mentioning the names of individual products. However, while in the application of the CTO available on the MPCB portal manufacturing process of 50 number of products with names were uploaded.
ii. Calculation of pollution load is done on the basis of list of products mentioned under API and Pharmaceutical Intermediates uploaded by PP on the MPCB portal. Detailed list of product before & after change in product mix is as mentioned above;
iii. After the change in product mix, the total combined production capacity of the plant will be remained same i.e., 2.0 MT/M.
iv. Change in the product mix in its existing facility will be achieved by Addition of 4 new products and inclusion of R & D product. No Change in 19 Existing Products, Deletion of 31 Existing Products.
v. The proposed activity is in such a way that the total production will remains same i.e. 2.0 MT/M, keeping the pollution load within the consent limit.
vi. Pollution load is calculated on the basis of worst case scenario i.e. considering manufacturing of each product to the tune of 2 MT/M. Emcure can manufacture combination of products or each product to the tune of 2 MT/M (as per CTO).
vii. No change in Water Consumption, Effluent generation and its quality.
viii. Switched over to cleaner fuel LDO/LSHS in place of Furnace oil
ix. There is no change in the Overall total hazardous waste quantity even after proposed Change in product mix

Technical Committee Decision:

Technical Committee decided to recommend the case for change in product under product mix with a compliance of the following conditions;

(i) Industry shall comply with all the conditions stipulated in Environmental Clearance and ensure display/upload of six-monthly compliance monitoring report on their official website.

(ii) Industry should not manufacture any other product for which permission is not granted by the MPCB.

(iii) Industry shall ensure connectivity of OCEMS data to Boards server and transmit the data continuously for wastewater treatment facility.

Agenda item No	**Item No. 15**
Proposal No.	**MPCB-CONSENT-0000156973**
Project Details	**M/s. Lupin Ltd.** Plot No. 30/10 to 30/13 & 64/7 T-142, MIDC Tarapur, Palghar.
NIPL Certificate	NIPL certificate issued by Goldfinch Engineering Systems Pvt. Ltd.

Due to paucity of time, it was decided to defer the case.

The meeting ended with vote of thanks to Chair.

(Shri. N. N. Gurav)
RO (BMW)
and Member-Convenor of Committee

(Dr. J.B.Sangewar)
Asst. Secretary (Tech.)
and Chairman of the Committee