Minutes of First Sitting of 2nd meeting of Technical Committee (2022-23) for assessment of application of under change in product-mix

Date

: 18/08/2022

Venue

: 4th Floor, Conference Hall, Kalpataru Point, Sion, Mumbai & Microsoft

Team Video conferencing.

Agenda item No	Item No. 1				
Proposal No.	MPCB-CONSENT-0000134276				
Project Details	M/s. Aarti Drugs Ltd., Plot No. W-60(B),61(B),62(B),71(B),72(B),73(B), M.I.D.C., Tarapur, Dist. Palghar				
NIPL Certificate	NIPL Certificate issued by M/s. Goldfinch Engineering Systems Pvt. Ltd., dtd. 14.03.2022.				

Introduction:

This has reference to the online proposal submitted vide No. MPCB-CONSENT-0000134276 along with the copies of documents seeking amendment in existing consent to operate under change in product – mix under the provisions of EIA Notification, 2006 amended on 23/11/2016 & on 02/3/2021.

Exiting Clearances:

- 1. Environmental Clearance is vide No. SEAC/2016/CR-20/TC-2, Dated. 06/02/2017.
- Amendment in consent to Operate obtained for change in product mix vide No. Format1.0 / AS(T)/ UAN No.0000079161/ CO-B- 5096 dated 12/12/2019 valid upto 31/01/2023.

Project details:

A. Production Details:

Sr. No.	Name of Product	Existing Consent quantity (MT/M)	Proposed (+)Addition & (-) Deletion (MT/M)	Proposed quantity (MT/M)
1	Aceclofenac (MCA route)	15	-5	10
OR	Aceclofenac (CAC route)	12	0	12
OR	Ticlo.HCL	5	0	5
OR	Diclofenac Sodium	15	0	15
OR	Diclofenac Potassium	10	0	10
OR	Pioglitazone HCI	2.7	0	2.7
OR	Fluconazole	0	2	2

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Sr. No.	Name of Product	Existing Consent quantity (MT/M)	Proposed (+)Addition & (-) Deletion (MT/M)	Proposed quantity (MT/M)	
OR	Tenligliptin	0	13	13	
0.0	Vildagliptin	0	5	5	
OR	Potassium Chloride (KCI)	0	9	9	
2	Tolnaftate	3	0	3	
OR	Celecoxib	25	0	25	
OR	Moxifloxacin Hydrochloride	0	4	4	
3	Ornidazole (Oil Base)	40	0	40	
OR	Secnidazole	10	0	10	
OR	Itraconazole	15	0	15	
	Total	80.00		80.00	

 The industry has proposed change in the product mix in its existing facility by Decreasing production capacity of 1 existing product, Addition of 4 new products.

B. Pollution load Details:

i) Water & Wastewater Aspect

	Consumption (CMD)			Loss(Loss(-) /gain(+) (CMD)			Effluent (CMD)		
ralph in In Paris	Existing as per CTO	Proposed reduction after CIPM	Total after CIPM	Existing	Proposed reduction after CIPM	Total after CIPM		Proposed reduction after CIPM	LOTAL	
Process	10.89	-0.09	10.80	-3.56	0	-3.56	7.33	-0.09	7.24	
Washing Activity	0	0	0	0	0	0	0	0	0	
Cooling Tower & Boiler	48	0	48	-45.34	0	-45.34	2.66	0	2.66	
Total - Trade (only)	58.89	-0.09	58.80	-48.90	0	-48.9	9.99	-0.09	9.90	
Gardening	1	0	1	-1	0	-1	0	0	0	
Domestic	7	0	7	-2	0	-2	5	0	5	
Grand Total	66.89	-0.09	66.80	-51.90	0	-51.90	14.99	-0.09	14.90	
Grand Total as per CTO		67			-57	The Land		10		

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Grand Total as per EC	67	-57	10

 After Change in product mix the water consumption & effluent generation will reduce by 90 Lit/Day & 90 Lit/Day respectively.

Treatment System

a) Trade Effluent:

Industry has segregated trade effluent into strong & weak stream and provided treatment system as below.

Strong Stream: The concentrated effluent 0.66 CMD is being treated separately in MEE installed in the Aarti Drugs Ltd., Located at Plot No. T-150 unit.

Weak Stream: ETP comprising of Primary (Collection tank, Neutralization tank, Equalization Tank, Flash Mixer, Primary Clarifier/Primary settling Tank), Secondary (Bio Reactor), Tertiary (Pressure sand Filter & Activate Carbon Filter) and further connected to CETP.

ii) ___ Air Emission Load: -

Sr N o	Stack Attache d to	Fuel	As Per CTO	As Per EC	Existing Fuel Consumpti on	Proposed Fuel Consumptio n	APC system	Stack Heigh t
		Coal			Dust			
1 Boiler (4 TPH)		FO	Not Mentione d	800 Ltr/Day	Coal: 125 Kg/Hr	No Change	Collector & Bag Filter	30 m
2	D.G. Set (500 KVA)	HS D	50 Lit/Hr	Not Mentione d	50 Lit/Hr	No Change	Acoustic Enclosure	12 m
3	D.G. Set (320 KVA)	HS D	30 Lit/Hr	Not Mentione d	30 Lit/Hr	No Change	Acoustic Enclosure	12 m
4	Scrubber				Towns of		Alkali Scrubber	3.5 m above the roof level
				Air Emissi	ons			
Des	cription			Solvent los	ss (MT/M)		le al	
	ution Load flucts	rom exi	sting	7.4	area per s	1 10-1		

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Pollution Load After Change in Product Mix	7.4
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· Industry has not proposed any change in fuel and process emissions.

iii) Hazardous Waste Load

Sr. No	Type of Waste	Cat. No.	As Per CTO	As Per EC	Existing Qty.	After Change in Product Mix Qty.	Remarks
1	Spent Catalyst	28.2	2364 Kg/M	2368 Kg/M	914 Kg/M	610 Kg/M	Reduction
2	Spent Carbon	28.3			1442 Kg/M	1714 Kg/M	Increased
3	Chemical sludge from waste water treatment	35.3	300	300 Kg/M	300 Kg/M	300 Kg/M	No Change
4	Spent Solvent	28.5	43923 Kg/M	44 MT/M	43745 Kg/M	42957* Kg/M	Reduction
5	Process Residue (Spent HCI Generating from Fluconazole only)	28.1	1-1	3 -		840* Kg/M	New Proposed
6	Process Residue (Sodium Hypochlorite Solution Generating from Fluconazole only)	28.1				13457 Kg/M	New Proposed

Total hazardous waste quantity after change in product mix will be 45749
 Kg/M which is less than the existing Hazardous Waste quantity i.e. 46401
 Kg/M.

Technical Committee Deliberations:

The proposed project was discussed based on documents – NIPL Certificate and presentation made by the industry. Product wise load calculation in terms of wastewater, Air emissions & Hazardous waste generation were discussed. Existing

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consent to operate, Environmental Clearance, NIPL Certificate issued by Goldfinch Engineering Systems Pvt. Ltd. and product –mix Proforma are taken on the record.

After due deliberations, Committee noticed that:

- 1) PP was unable to show the comparison of pollution load with respect to the exisitng product which are proposed to decrease and new products which are proposed to add, along with the changes in raw materials, if any. Also, unable to show the quality and the quantity of the pollutants exisitng and proposed along with pollution load.
- 2) PP has not discontinued the Furnace Oil as a fuel and not switched to the cleaner fuel.
- 3) The Hazardous Waste is increasing after change in product mix.
- 4) PP was unable to show the details of emissions, its concentration and load. Also, industry has not showed about the emissions such as chlorine generating from the proposed products.
- 5) Committee also, noticed that the presentations are not clearly specifying the comparison of pollution load with respect to Environmental Clerance, Consent and Proposed changes for water, air and Hazardous Waste etc.

Technical Committee Decision:

Technical Committee decided to defer the case and asked PP to reassess their pollution load, along with the NIPL certificate and was advised the PP to furnish above details, before the committee.

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Agenda Item No.	2
Proposal No.	MPCB-CONSENT-0000144332
Project Details	M/s. Karmayogi Ankushrao Tope Sahakari Sakhar Karkhana Ltd, Village-Ankushnagar, Tal. Ambad, Dist. Jalna.
NIPL Certificate	NIPL Certificate issued By UltraTech Environmental Consultancy & Laboratory NO. NIPL/KATSSKL/2022/Certificate, Dtd. 14/07/2022

Introduction:

This has reference to the online proposal submitted vide No. MPCB-CONSENT-0000144332 along with the copies of documents seeking amendment in existing consent to operate under change in product-mix under the provisions of EIA Notification 2006 amended on 23/11/2016 & amended on 02/3/2021. Industry has obtained Consent to Operate on 07/05/2022 for 60 KLPD Distillery unit & requested for amendment in consent to operate under change in product mix.

Existing Clearances:

- 1. Environment Clearance for 60 KLPD Distillery obtained on dated 16.03.2020 (EC Letter. SIA/MH/IND2/49815/2018 dated 16/03/2020.
- 2. Consent to 1st Operate for expansion for 30 KLPD Distillery unit with Ethanol production by using molasses as raw material with amalgamation with existing 30 KLPD distillery (Total 60 KLPA) vide no. Format1.0 / CAC / UAN No. MPCB-CONSENT- 0000133046 / CO / 2205000379 issued on 07.05.2022 and valid up to period 31.08.2022.

Project Details:

Industry is having existing 60 KLPD distillery & using C Heavy molasses as raw material to produce Rectified Spirit (RS) OR Impure Spirit OR Ethanol and Fusel Oil. Industry has proposed to switch over the raw materials namely 'B Heavy' Molasses and 'Cane Juice (Syrup)' from conventional 'C Molasses'.

Project Details:

Project Details Particulars	Existing	After product Mix			
Capacity	60 KLPD	90 KLPD	90 KLPD		
Raw Material	C- Molasses	B-heavy Molasses	Syrup		
Production	RS: 60 KLPD [OR] Ethanol: 60 KLPD [OR] ENA: 60 KLPD	RS: 90 KLPD			
By-product	CO2 – 45 TPD	CO2 - 68 TPD			

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- Addition of Ethanol [OR] Rectified Spirit by 30 KLPD.
- CO₂ Gas is sent to Bottling plant.

B. Pollution load Details:

(i) Water & Wastewater Aspect:

Sr.N o	Particulars	Existing (60 KLPD)		Scenario -1 (90 KLPD B- Heavy molasses)			Scenario -2 (90 KLPD Sugar Cane Juice (Syrup)			
		Quanti ty in CMD	COD in mg/l	COD in Kg/da	Quanti ty in CMD	COD in mg/l	COD in Kg/da y	Quanti ty in CMD	COD in mg/l	COD in Kg/da y
1	Water Consumpti on in CMD	1242 (Fresh Water 612 CMD + Recycle 415 CMD)	NA	NA	1004 (Fresh Water 504 CMD + Recycle 500 CMD)	NA	NA	883 (Fresh Water 456 CMD + Recycle 427 CMD)	NA	NA
2	Industrial Ef	fluent ger	neration							
Α	Spent Wash in CMD	650	14000	91000	576	13000	74880	315	9000	28350
В	Spent Lees in CMD & other effluent	170	1500	255	185	1500	277.5	185	1500	277.5
	Total	700		91255	626		75157. 5	365	7	28627. 5

 Fresh water consumption reduces by 108 CMD in B-Heavy Molasses and 156 CMD in Cane Juice (Syrup).

COD load will reduce by 16097.5 kg/day using B- heavy Molasses and 62627.5 kg/day by using syrup.

Treatment System:

a. Spent wash Treatment:

Spent wash directly treated through Multi-effect evaporator and concentrated will be used for incineration boiler of capacity 22 TPH and condensate from MEE treated in CPU.

b. Other Effluent:

Industry has provided Effluent Treatment Plant (CPU) comprising Equalization Tank, Anaerobic Digester, Lamella Clarifier, Aeration Tank, Clarifier, MMF, ACF, Reverse Osmosis and treated effluent is recycled in the process.

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(ii) Air Emission Load:

Sr. No.	Particulars	Existing Fuel Consumption		Remarks
	22 TPH Incineration Boiler	Coal – 52 MT/Day. [OR] Bagasse – 100 MT/Day And Concentrated Spent wash – 130 MT/D	Coal – 48 MT/Day. [OR] Bagasse – 98 MT/Day And Concentrated Spent wash – 122 MT/D	Overall fuel consumption will be reduced resulting decrease in pollution load.

- Industry has provided ESP as an Air Pollution Control System to Incineration Boiler.
- Stack Emissions SO₂ load decreases from 1040 Kg/D & 970 Kg/D.

(iii) Solid Waste Load:

Sr. No.	Particulars	Existing (60 KLPD- C Molasses)	After product mix (90 KLPD)	Remarks
01	Yeast Sludge	6 MT/D	9 MT/D	Increased
02	Boiler Ash	37.7 MT/D	35.38 MT/D	Reduced

- Yeast Sludge is taken to MEE and the dried sludge is burnt in incineration boiler.
- (iv) Hazardous Waste Load:

There is no generation of Hazardous Waste before & after product mix.

Technical Committee Deliberations:

The project proposal was discussed based on presentation made and documents- NIPL Certificate, NIPL proforma submitted by the proponent. Product wise load calculation in terms of wastewater and Air Emissions were discussed. Existing Consent to Operate, Environmental Clearance, No Increase in Pollution Load certificate issued by M/s. ULTRA TECH Environmental Consultancy & Laboratory and product-mix proforma are taken on the record.

After due deliberations Committee noticed that:

(i) The proposal submitted for enhancement in capacity of Distillery unit 60 KLPD to 90 KLPD by switching the raw material from C-Molasses to B-Heavy Molasses or Cane Juice Syrup under change in product-mix. It is an integrated

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Sugar & Distillery unit. PP enhance the capacity of distillery unit by switching over raw materials namely 'B Heavy' Molasses and 'Cane Juice (Syrup)' from conventional 'C Molasses' resulting reduction in Sugar Production. Committee advised to reduce the sugar production quantity by amending the sugar unit consent.

- (ii) There is overall reduction in water consumption, wastewater generation and Air Pollution Load. COD load is reduced by 16097.5 kg/day using B- heavy Molasses and 62627.5 kg/day by using syrup.
- (iii) PP installed ESP as an air pollution control system and CO₂ bottling plant.
- (iv) There will be no change in existing utility set up.
- (v) Industry has provided Zero Liquid Discharge system. i.e MEE (5 Stage) followed by Incineration Boiler and condensate is recycled back into process and utilities.

Technical Committee Decision:

Technical Committee decided to recommend the case for change in product mix with a compliance of the following condition.

- (i) The industry shall submit six monthly reports on the status of compliance of the stipulated Environmental Clearance conditions including results monitored data (both in hard copies as well as by e-mail) to the respective Regional Office of MoEF & CC, the respective Zonal Office of CPCB & MPCB. A copy of Environmental Clearance and six-monthly compliance status report shall be posted on the website of the industry.
- (ii) PP should not manufacture any other product for which permission is not granted by the MPCB.
- (iii) PP shall ensure connectivity of OCEMS data to Board server.
- (iv) PP shall install adequate capacity CO2 bottling plant.
- (v) PP shall ensure that there is no increase in the effluent and shall ensure Zero Liquid Discharge system.

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Agenda item No	Item No. 3				
Proposal No.	MPCB-CONSENT-0000137129				
Project Details	M/s. Cipla Limited [Unit 3] Plot No. D-22, MIDC Kurkumbh, Tq. Daund, Dist. Pune				
NIPL Certificate	NIPL certificate issued by Technogreen Environmental Solutions No. Nil, Dated. Nil.				

Introduction:

This is an existing unit engaged manufacturing of Pharmaceutical Products. This has reference to the online proposal submitted vide No. MPCB-CONSENT-0000137129 along with the copies of documents seeking amendment in existing consent to operate under change in product – mix under the provisions of EIA Notification, 2006 amended on 23/11/2016 & on 02/3/2021.

Exiting Clearances:

- Environmental Clearance is obtained in the name of M/s. Meditab Specialties Pvt. Ltd. vide No. F. No. J-11011/47/2005-IA II (I) dated 13th October 2005.
- Consent to Operate obtained vide No. Format1.0 / CAC/ UAN No.0000109542 / CR-2107001039 dated 19.07.2021 valid upto 30/04/2024.

Project details:

C. Production Details:

Sr. No.	*Product Name	Existing Quantity MTA	Propose d MTA	Addition / Reduction MTA
Anti-l	Retrovirai/Anti-Viral			
1 Abacavir Sulphate		35	3	Reduction by 32 MT/A
2	Dolutegravir Sodium	31	31	No Change
3	Tenofovir Disoproxil Fumarate	9	5	Reduction by 4 MT/A
4	Tenofovir Alafenamide Fumarate	0.1	0.1	No Change
5	Emtricitabine	8.8	8.8	No Change
6	Nevirapine / Nevirapine Hemihydrate	1.5	1.5	No Change
7	Remdesivir	0.5	0.5	No Change
8	Zidovudine	0.5	0.5	No Change
9	Oseltamivir Phosphate	20	20	No Change
10	Valacyclovir Hydrochloride	0.2	0.2	No Change
11	Molnupiravir	1	1	No Change
12	Bictegravir	0.1	0.1	No Change
13	Lamivudine	15	15	No Change
14	Baloxavir Marboxil	1	1	No Change

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15	Cabotegravir sodium	5	5	No Change
	Bacterial/Fungal			NA 11-24
16	Terbinafine Hydrochloride	14	14	No Change
	Androgen	0.05	0.05	No Change
17	Danazol			No Change
18	Cyproterone Acetate	0.7	0.7	No Onlarige
	Inflammatory	-		No Chango
19	Tafamidis	1	1	No Change
20	Eluxadoline	0.1	0.1	No Change
	Inflammatory/ Histamine			
21	Fexofenadine Hydrochloride	0.1	0.1	No Change
Chel	ating Agent			
22	Sodium thiosulfate pentahydrate	0.5	0.5	No Change
23	Deferasirox	0.5	0.5	No Change
24	Edaravone	0.1	0.1	No Change
25	Deferiprone	0.1	0.1	No Change
Anti-	Depressant			
26	Escitalopram Oxalate	0.1	0.1	No Change
27	Citalopram Hydrobromide	0.1	0.1	No Change
Anti	Neoplastic			
28	Estramustine Sodium Phosphate	0.04	0.04	No Change
29	Ondansetron Base / HCL	0.5	0.5	No Change
30	Exemestane	0.5	0.5	No Change
Anti-	Diabetic			
31	Rosiglitazone Maleate	0.05	0.05	No Change
32	Dapagliflozin	0.05	0.05	No Change
33	Empagliflozin	0.05	0.05	No Change
- 1	ogenic			
34	Levonorgestrel	0.01	0.01	No Change
-	chodilator		,	90
35		0.5	0.5	No Change
	Formoterol Fumarate /FC-V Parkinson	0.0	0.0	140 Orlange
36		0.25	0.25	No Change
	Pramipexole Dihydrochloride /PX-IV	0.23	0.25	No Change
Card		1.00	1.00	No Ohana
37	Carvedilol	1.00	1.00	No Change
38	Trimetazidine	1.00	1.00	No Change

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39	Omeprazole Sodium	0.00	15.00	Proposed
40	Pantoprazole Sodium	0.00	10.50	Proposed
41	Tenofovir Pivafen Fumarate	0.00	0.50	Proposed
42	Nirmatrelvir	0.00	10.00	Proposed
	Total	150	150	

- Industry has proposed reduction in production quantities of 2 Products and proposed additional 4 new products.
- . The overall production quantity will remain same i.e. 150 MT/A.

D. Pollution load Details:

iv) Water & Wastewater Aspect

Before Product Mix

Sr. No.	Particular	Quantity in CMD	Effluent Segregation in CMD		177	(Strong)		COD (Weak)		TDS (Strong)		TDS (Weak)	
		HE H	Stron	g Weak	mg/l	Kg/day	mg/l	Kg/day	mg/l	Kg/day	mg/l	Kg/day	
1	Water Consumption	230				Not a	pplicable	9					
2				Trade	Effluent G	eneration	on						
Α	Process Activity	97 (+15 Condensate)	15	91.04 (+15 condensate)	84597.95	1268.97	8459.79	770.14	41113.3	616.7	1500	136.6	
В	Cooling Tower & Boiler	5.97	-	5.97		-	400	2.39	-	-	1500	8.9	
С	Total	102.97	15	97.01	84597.95	1268.97	8859.79	772.39	41113.3	616.7	3000	145.5	
3	Domestic Effluent Generation, CMD	38		38	-	-	500	19			600	22.8	

After Product Mix:

Sr. No.	Particular Quantity in CMD	Quantity in CMD	Efflu Segrega CM	tion in	(Stro		(We	DD eak)	(Stro			DS (eak)
		Strong	Weak	mg/l	Kg/day	mg/l	Kg/day	mg/l	Kg/day	mg/l	Kg/day	
1	Water Consumption	228.9					Not appli	cable				
2	Trade Effluent	Generatio	n									
A	Process Activity	95.16	15	89.2	84597.95	1268.97	8261.31	736.89	41113.3	616.7	1500	133.8

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В	Cooling Tower & Boiler	5.97	-	5.97	10-10	V A	400	2.39		12 11	1500	8.9
C	Total	101.13	15	95.17	84597.95	1268.97	8661.31	739.28	41113.3	616.7	3000	145.5
3	Domestic Effluent Generation, CMD	38	-	38			500	19			600	22.8

Water Consumption will reduce by -1.11 CMD.

Effluent generation will reduce by
 Average COD Load will reduce by
 - 33.3 Kg/Day

Pollution Load with respect to the Changes proposed: -

Scenario	Name of product	Product Qty. Kg/D	Water Consumption (CMD)	Effluent (CMD)	Strong Stream (liquid) lit./day	Incinerable Haz. Waste (kg/day)
	Abacavir Sulphate	-87.7	-13.9	-14.6	0.0	40.0
Existing	Tenofovir Disoproxil Fumarate	-11.0	-5.4	-4.1	-0.117	-14.7
Total	al Existing	-98.7	-19.3	-18.7	-0.117	-25.3
	Omeprazole Sodium	41.1	0.7	1.3	0.0	0.0
Droposed	Pantoprazole Sodium	28.8	3.7	2.0	0.0	0.0
Proposed	Tenofovir Pivafen Fumarate	1.4	0.5	0.4	-0.014	1.9
	Nirmatrelvir	27.4	13.3	13.2	0.0	0.0
Tota	al Post PM	98.7	18.2	16.9	14.9	1.9
Re	ductions	0	-1.11	-1.84	-102.10	-29.10

Treatment System

b) Trade Effluent:

Industry has segregated trade effluent into strong & weak stream and provided treatment system as below.

Strong Stream: High COD/TDS stream is treated in Primary, Stripper, Multiple Effect Evaporator (MEE) (3 Stage) and ATFD and condensate treated along with weak stream.

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Weak Stream: ETP of capacity 150 CMD comprising of primary, secondary and tertiary treatment system followed by Reverse Osmosis and treated effluent is 100% recycled in the process to achieve Zero liquid Discharge.

c) Domestic Effluent:

The domestic effluent is combinedly treated with the trade effluent in ETP.

v) Air Emission Load: -

Attached to	Capacity	Existing Fuel	Proposed Fuel	Stack Height (in m)	Control equipment preceding the stack	Pollutants in stack gases	
Thermopacks 2 2 Kcal/hr HSD – 4l Kg/Hr (One Standby)		HSD – 48 Kg/Hr	J. HILL HILL GASE	30	Stack	SO ₂	
Boilers 2 nos. 2 TPH FO		FO – 120 Kg/h	LSHS - 114.2 Kg/h. [OR] PNG - 1.47 SCM	33	Stack	SO ₂	
DG Set 1	DG Set 1 250 KVA HSD - 50 - 4 Acous		Acoustic enclosure/stack	SO ₂			
DG Set 2	500 KVA	HSD – 100 Kg/Hr	5 Acoustic enclosure/stack		SO ₂		
DG Set 3	750 KVA	HSD – 150 Kg/Hr	D – 150 - 6 Acoustic		SO ₂		
Process Vent-1 (BD I)				3	Water Scrubber	HCI & NOx	
Process Vent-2 (BD I)	-			6	Water Scrubber	HCI & Nox	
Process Vent-3 (BD II)	-			6	Caustic Scrubber	HCI & NOx	
Process Vent-4 (BD II)	411	6-11	- 11	4	Caustic scrubber	HCL & NOx	
Process Vent-5 (BD III)			-	6	Water scrubber	HCL & NOx	
Process Vent-6 (BD IV)	-	7		4	Water scrubber	HCL & NOx	
Process Vent-7 (BD IV)	Process Vent-7		9	Water scrubber	HCL & NOx		

- Industry has switched the fuel from Furnace Oil to LSHS and proposed PNG as a cleaner fuel.
- PM emissions will reduce by 745 Kg/Day and SO₂ emissions will reduce by 4193 Kg/Day.
- The process emissions will remain same as per exisitng.

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vi) Hazardous Waste Load

Category	HW Type	Quantity	иом	Method of Treatment	Remarks
5.1	Used Oil or spent Oil	2.020	KL/A	Recycle	No Change
20.2	Spent Solvents	3651.4	KL/A	Recycle/Incineration	No Change
28.3	Spent Carbon	10.6	MT/A	Incineration	No Change
28.5	Date expired products	0.210	MT/A	Incineration	No Change
35.3	Chemical sludge from wastewater treatment	42.1	MT/M	Landfill	No Change
37.1	Sludge from wet scrubbers	0.10	MT/A	Landfill after treatment	No Change
37.3	Concentration or evaporation residues	287.47	MT/A	Landfill after treatment	Reduction
28.6	Spent solvents	259.2	MT/A	Recycle/Incineration	No Change
28.2	Spent catalyst	90	MT/A	Recycle/Secured Landfill	No Change
33.1	Empty barrels/containers/liners contaminated with hazardous chemicals/wastes	1200	Nos/Y	Recycle	No Change
35.4	Oil and grease skimming	63	MT/A	Incineration	

· Total Haz. Waste is reduced by 29.1 kg/day

Technical Committee Deliberations:

The proposed project was discussed based on documents – NIPL Certificate and presentation made by the industry. Product wise load calculation in terms of wastewater, Air emissions & Hazardous waste generation were discussed. Existing consent to operate, Environmental Clearance, NIPL Certificate issued by Technogreen Environmental Solutions and product –mix Proforma are taken on the record.

After due deliberations, Committee noticed that:

- The overall production quantity after product mix will remain same i.e 150 MTA.
- The water consumption, trade effluent generation & organic load will be reduced after product mix by 1.11 CMD, 1.84 CMD and 33.3 Kg/Day respectively.
- iii) Industry has provided Zero Liquid Discharge system and have segregated and provided separate treatment for strong and weak stream trade effluent.
- iv) The overall Hazardous waste quantity after product mix will be reduced by 29.1 Kg/Day.
- v) PP has proposed to switch to cleaner fuel from FO to PNG.
- vi) The overall pollution load is not increased after change in product mix.

Technical Committee Decision:

Technical Committee decided to recommend the case for change in product under product mix with compliance of the following conditions;

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- 1) Industry shall obtain the change in name in Environmental Clearance.
- Industry shall comply with the conditions stipulated in Environmental Clearance and ensure display /upload of six- monthly compliance monitoring report on their official website.
- Industry shall dispose the By-product (if any) to actual user having permission under Rule-9 of Hazardous & Other Wastes (M & TM) Rules, 2016.
- 4) Industry shall not manufacture the other products for which the permission is not granted by the MPCB.
- 5) Industry shall ensure the connectivity of the OCEMS data to the Board Servers.

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Agenda item No	Item No. 4						
Proposal No.	MPCB-CONSENT-0000132766						
Project Details	M/s. Hindustan Petroleum Corporation Limited - Mumbai Refinery, HPCL Mumbai Refinery, B.D. Patil Marg, Mahul, Mumbai.						
NIPL Certificate	NIPL certificate dated 12/4/2021 issued by M/s. MITCON Consultancy & Engineering Services Ltd.						

Introduction:

This has reference to the online proposal submitted vide No. MPCB-CONSENT-0000132766 along with the copies of documents seeking consent to establish for (Expansion) under change in product – mix under the provisions of EIA Notification, 2006 amended on 23/11/2016 & on 02/3/2021.

Exiting Clearances:

- Environmental Clearance granted vide No. vide No. F.No. J-11011/413/2014-IA II (I) dated 31/1/2017.
- Consent to Operate obtained vide No. Format 1.0 / CAC / UAN No.0000079578/ CO-2109000773, Date. 20/09/2021, valid upto 31/08/2025.

Project details:

Proposed Consent to Establish for expansion activity under product mix. Industry propose to decrease the production quantity of BS VI Diesel by 38000 MTPA and proposed to produce HP-DAK solvents- 38000 MTPA.

F Production Details:

SI	Product	Existing As per CTO	Proposed Addition/ Deletion	After Change in product Mix
1.	Light Distillates(2515800)			
1.	LPG + PROPYLENE	542000	0	542000
2.	LAN	156300	0	156300
3.	SCN	96000	0	96000
4.	Treated Hexane	30000	0	30000
5.	Solvent 1425	8500	0	8500
6.	BS VI MS	1683000	0	1683000
II.	Middle Distillates (414200)	0)		
7.	MTO	48000	0	48000
8.	ATF	600000	0	600000
9.	SKO	52000	0	52000
10.	BS VI Diesel	3441000	-38000	3403000
11.	HP-DAK Solvents	0	+38000	38000
12.	LDO	0	0	0
13.	RPO	0	0	0
III	Lube Oil Base Stock (4500	000)		

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	Total	9523800		9523800
26.	Sulphur	61000	0	61000
V.	Elemental Sulfur (61000)			
25.	Fuel & Loss	606000		606000
24.	VG -30 Bitumen	546000	0	546000
23.	VG - 10 Bitumen	234000	0	234000
22.	IFO	969000	0	969000
IV	Other Heavy Products inc	luding refinery fuel & loss (2355000)	
21	IO - 100	15000	0	15000
20	Bright Stock	50000	0	50000
19	500 N Gr-I	100000	0	100000
18	150 N Gr-I	70000	0	70000
17	Spindle Oil GR -II	32000	0	32000
16	Spindle Oil GR -I	15000	0	15000
15	500 N Gr-II	92000	0	92000
14	150 N Gr-II	76000	0	76000

F. Pollution load Details:

vii) Water & Wastewater Aspect

Purpose	Existing Water Consumption	After Change in Product Mix	Proposed Change in Water Consumption
Industrial Cooling (Sea water cooling)	90242	90242	0
Domestic	870	870	0
Processing whereby water gets polluted & pollutants are easily biodegradable	12348	12348	0
Processing whereby water gets polluted & pollutants are not easily biodegradable and are toxic	0	0	0
Agriculture/ Gardening	1500	1500	0
Total (Excluding Sea Water)	14718	14718	0

. There will be no change in water consumption.

Purpose	Existing Effluent Generation As per CTO	After Change in Product Mix	Mode of Disposal/ Treatment
Trade	7200	7200	This effluent is treated in Effluent Treatment Plant and water is recycled to the maximum extent.
Effluent	80354.0	80354.0	Sea cooling water blow down shall be discharged into Mahul Creek through cooling channel

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Domestic Effluent	600	600	The treated sewage is mixed in biological treatment section of Effluent Treatment Plant
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Trade effluent generation will remain same.

Treatment System

d) Trade Effluent: ETP of capacity comprising of primary, secondary and tertiary treatment system is provided.

e) Domestic Effluent:

The domestic effluent is combinedly treated in ETP.

viii) Air Emission Load: -

	(b) Stack	Stack	Existing Fuel	Consumption		sed Fuel umption
Sr. No.	attached to	height Mtr.	Type of fuel	Qty. of Fuel (kg/hr.)	Type of fuel	Qty. of Fue (kg/hr.)
1	FR-APS (11-F- 1)	61	LSHS	4733	LSHS	4733
	17		Fuel gas	4496	Fuel gas	4496
2	24-F-1001 (New VPS)	75	LSHS	4100	LSHS	4100
			Fuel gas	3700	Fuel gas	3700
3	FR-APS (11-F- 2)	61	LSHS	4022	LSHS	4022
			Fuel gas	3821	Fuel gas	3821
4	FCCU-1 Furnace (14- F1-X)	61	LSHS	1411	LSHS	1411
	. , ,		Fuel gas	1340	Fuel gas	1340
5	FCCU-1 FGSU (14 T 1001)	60	**			
6	FRE-APS- (31- F-1)	61	LSHS	5233	LSHS	5233
			Fuel gas	4971	Fuel gas	4971
7	FRE-VPS (32- F-1)	60	LSHS	1777	LSHS	1777
			Fuel gas	1688	Fuel gas	1688
8	DHDS 71-F-01	60	Fuel gas	875	Fuel gas	875
9	H2 Reformer (73-F-02)	60	LSHS	3079	LSHS	3079
-			Fuel gas	2925	Fuel gas	2925
10	Old SRU (75-F- 01)	60	Fuel gas	550	Fuel gas	550
11	PDS Furnace (73-F-01)	60	Fuel gas	78	Fuel gas	78

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12	Boiler SG 10/11	88.5	LSHS	14904	LSHS	14904
			Fuel gas	14159	Fuel gas	14159
13	Boiler SG-12	60	LSHS	7997	LSHS	7997
			Fuel gas	7597	Fuel gas	7597
14	FCCU -II Furnace (114 F-3001)	64	Fuel gas	1430	Fuel gas	1430
15	FCCU-II FGSU (110 T1001)	60		100 100 110		-
16	NSU Furnace 101-F-1001	60	Fuel gas	3487	Fuel gas	3487
17	CCR Inter Heater 102-F- 1001 & 102 F- 2003/2004	71	Fuel gas	2398	Fuel gas	2398
18	CCR Inter Heater 1 & Charge Heater 102 F- 2001/2002	71	Fuel gas	3050	Fuel gas	3050
19	ISOM NHDT Heater 103-F- 1001	60	Fuel gas	208	Fuel gas	208
20	Prime G+ Furnace 105-F- 1001	60	Fuel gas	302	Fuel gas	302
21	DHT 700 F 1001/2 Furnace	60	LSHS	4250	LSHS	4250
			Fuel gas	4037.5	Fuel gas	4037.5
22	DHT New SRU Incinerator 704 F4001	60	Fuel gas	565	Fuel gas	565
23	Gas Turbine (GTG-3)	60	Naphtha	2708	Naphtha	2708
			Fuel gas	2573	Fuel gas	2573
24	Gas Turbine (GTG-4)	60	Naphtha	2708	Naphtha	2708
18			Fuel gas	2573	Fuel gas	2573
25	Gas Turbine (GTG-5)	65	Naphtha	7917	Naphtha	7917
			Fuel gas	7521	Fuel gas	7521
26	LR VPS Furnace (F- 101)	60	LSHS	14904	LSHS	14904
			Fuel gas	14904	Fuel gas	14904
27	NMP I (F- 201/202)	60	LSHS	1636	LSHS	1636
			Fuel gas	1554	Fuel gas	1554
28	NMP-II (F-	60	LSHS	1636	LSHS	1636

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	3201/3202)					
			Fuel gas	1554	Fuel gas	1554
29	NMP-III (F- 4201/4202)	60	LSHS	1636	LSHS	1636
			Fuel gas	1554	Fuel gas	1554
30	LR PDA (F- 4101)	60	LSHS	1176	LSHS	1176
			Fuel gas	1117	Fuel gas	1117
31	LR-IOH (F-401)	30.5	LSHS	14904	LSHS	14904
			Fuel gas	580	Fuel gas	580
32	LOUP (99- F/02/03)	71	Fuel gas	1015	Fuel gas	1015
33	105 – F – 5001 (Prime G)	60	Fuel gas	470	Fuel gas	470
34	NHGU PDS Furnace (173- F-1101)	60	Fuel gas	3384	Fuel gas	3384
35	NHGU Reformer (173- F-211)	60	Fuel gas	78500	Fuel gas	78500
36	New CPP (GTG-6)	60	Naphtha	18450	Naphtha	18450
			Fuel gas	17000	Fuel gas	17000

· PP has proposed no change in fuel consumption.

 Installed a Flue Gas Scrubbing Unit (FGSU) to control emissions (Sox and PM) and Tail Gas Treating Unit (TGTU) is also installed in DHDS SRU for sulfur recovery to 99.9 %.

ix) Hazardous Waste Load

SI.	Type of Waste	Category		Generation (No Change)		Mode of Stora ge	Mode of Treatment & Disposal
		(As per schedule)	Existing	After Change in Product Mix			
1	Oily Sludge from Crude & Product Tanks	4.1	500 MT/M	500 MT/M	Tanks	Lagoon	Recovery
2	Residual sludge cake after recovery of oil	4.1	250 MT/M	250 MT/M	Tanks	Lagoon	Bio- remediation
3	Silt	Other	83.33	83.33	Sea Water	Lagoon	Bio-

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	accumulation from incoming sea water		MT/M	MT/M			remediation
4	Sludge from w.w.t	35.3	1.66 MT/M	1,66 MT/M	Effluent Treatment Plant	Lagoon	Bio- remediation/ solid compaction by dewatering
5	Spent ion exchange resin containing toxic metals	35.2	6.13 MT/M	6.13 MT/M	DM Plant	Drums/S acks	CHWTSDF
6	Spent Catalyst	4.2	4546 MT/A	4546 MT/A	Process Units	Drums/S acks	CHWTSDF
7	Insulation material contaminated with oil	Other	41.66 MT/M	41.66 MT/M	Damaged insulation on pipelines	Yard	CHWTSDF
8	Obsolute chemicals (in qty. as and when generated)	Other	4.17 MT/M	4.17 MT/M		-	CHWTSDF

· Total Haz. Waste will remain same.

Technical Committee Deliberations:

The proposed project was discussed based on documents - NIPL Certificate and presentation made by the industry. Product wise load calculation in terms of wastewater, Air emissions & Hazardous waste generation were discussed. Existing consent to operate, Environmental Clearance, NIPL Certificate issued by M/s. MITCON Consultancy & Engineering Services Ltd. and product -mix Proforma are taken on the record.

After due deliberations, Committee noticed that:

1) Committee pointed that generation of Spent catalyst from proposed change will be increasing, in response to the same PP informed that overall spent catalyst generation will be within the consented limit.

2) Committee pointed that the Environmental Clerance accorded does not mention the products names and quantities, in response to same PP informed that E.C accorded for plant activity, and they have already shown product names and production quantity in EIA Report. Also, they have communicated MoEF & CC for correction in E.C for inclusion of products.

3) PP was unable to produce the details of the process emissions before and after

change in product mix.

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Technical Committee Decision:

Technical Committee decided to recommend the case for change in product mix with submission of following details and compliance of conditions.

- 1) PP shall submit the product wise spent catalyst generation.
- PP shall amend the Environmental Clerance prior to obtain Consent to Operate for inclusion of products names and quantities.
- 3) PP shall submit details of the process emissions before and after change in product mix.
- 4) The industry shall submit six monthly reports on the status of compliance of the stipulated Environmental Clearance conditions including results monitored data (both in hard copies as well as by e-mail) to the respective Regional Office of MoEF & CC, the respective Zonal Office of CPCB & MPCB. A copy of Environmental Clearance and six-monthly compliance status report shall be posted on the website of the industry.
- 5) PP should not manufacture any other product for which permission is not granted by the MPCB.

6) PP shall ensure connectivity of OCEMS data to Board server.

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Agenda item No	Item No. 5
Proposal No.	MPCB-CONSENT-0000137807
Project Details	M/s. Maharashtra Aldehydes & Chemicals LTD., Plot No. A-17, MIDC area Mahad, Tal- Mahad, Dist – Raigad.
NIPL Certificate	NIPL certificate issued by Aditya Environmental Services Pvt. Ltd., No. Nil, Dated.21.06.2022.

Introduction:

This has reference to the online proposal submitted vide No. MPCB-CONSENT-0000137807 along with the copies of documents seeking consent to establish for (Expansion) under change in product – mix under the provisions of EIA Notification, 2006 amended on 23/11/2016 & on 02/3/2021.

Exiting Clearances:

- 1. Environmental Clearance granted vide No. SEIAA-EC-0000002254, Date. 24/04/2020.
- Consent to Establish for expansion granted Vide No. Format 1.0/CC/UAN No. 0000092765/CE- 2011000757, Date. 12/11/2020.
- Consent to Operate obtained vide No. Format 1.0 / AS(T) / UAN No.0000104788/ CO, Date. 17/08/2021, valid upto 28/02/2024.

Project details:

G. Production Details:

No	and the second second	Qty as per EC (*)	As per CTO (#)	Proposed change	After product mix	Remarks
		Quant	ity in MTPM			
1	Alkyl Esters of Phthalic acids	1600	1200	0	1200	No change
2	Ethyl Benzoate	30	30	0	30	No change
3	Ethyl Butyrate	100	50	0	50	No change
4	Ethyl Propionate	50	50	0	50	No change
5	Ethyl Laurate	5	0	0	0	No change
6	Ethyl Caprate	5	0	0	0	No change
7	Ethyl Caproate	5	0	0	0	No change
8	Ethyl Heptanoate	5	0	0	0	No change

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9	Ethyl 2-Methyl Butyrate	5	0	0	0	No change
10	Ethyl Valerate	5	0	0	0	No change
11	Ethyl Cinnamate	4	0	0	0	No change
12	Tri ethyl Citrate	100	50	0	50	No change
13	Tributyl Citrate	15	0	0	0	No change
14	Acetyl Tributyl Citrate	35	35	0	35	No change
15	Syringaldehyde	1.5	1.5	0	1.5	No change
16	Trimethyl Hydroquinone (TMHQ)	20	20	-7	13	Reduction
17	Anisole	500	0	0	0	No change
18	Anethole	300	0	0	0	No change
19	4-Methyoxyl Acetophenone	260	0	0	0	No change
20	1-Piperidino 1- cyclohexene	40	0	0	0	No change
21	Di hydro Anethole	20	0	0	0	No change
22	Cis Anethole	10	0	0	0	No change
23	2-Methoxy Acetophenone (2- MAP)	1	0	0	0	No change
24	2,4-Diacetyl Anisole	1	0	0	0	No change
25	Cyclopentanone	100	100	0	100	No change
26	Anhydrous Alcohol	1200	500	0	500	No change
27	Distillation of solvents	400	365	0	365	No change
28	Maxvit Vitamin	100	100	0	100	No change

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	TOTAL	5442.5	2752	+393	3145	Capacity expansion=11.5% against CTO
34	Diethyl Ketone	0	0	100	100	New Product
33	Acetonitrile	0	0	+300	300	New Product
32	Sanitizers	0	200	0	200	No change
31	Propionic acid	180	0	0	0	No change
30	Acetic Acid	105	0	0	0	No change
29	Sodium Sulphate	500	50	0	50	No change
	Formulation					

Industry has proposed increase in production capacity from 2752 MT/M to 3145 MT/M. Industry has proposed to reduce the production quantity of 2 products and proposed additional 2 new products and their plants namely Acetonitrile and Diethyl Ketone with proposed capacities 300 MT/M & 100 MT/M respectively.

H. Pollution load Details:

x) Water & Wastewater Aspect

Quantity for Water Consumption (cmd)							
Purpose/Category	* as per EC	** Consented	Actual Quantity Existing	Quantity Post expansion			
1) Industrial Cooling	295	125.5	42	298.5			
2) Domestic Purpose	15	11.5	5	11.5			
3) Processing whereby water gets polluted and pollutants are easily biodegradable.	75	82	12	67			
5) Gardening	25	7	7	7			
Total Water	410	225	66	384			

Fresh Water Consumption will increase by 159 CMD.

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Quantity for Effluent Generation (CMD)								
Category	As per EC (*)	** Consented	***Actual Generation Existing	Quantity Post expansion				
1) Trade Effluent	95	99.8	40-50	112.2				
2) Domestic Effluent	12	8	8	8				
Total Effluent	107	107.8	48-58	120.2				
Effluent discharge to CETP	67.5	67.5	19	67.5				

Trade effluent generation will increase from 99.8 CMD to 112.2 CMD.

Treatment System

f) Trade Effluent:

Industry has segregated trade effluent into strong & weak stream and provided treatment system as below.

Strong Stream: High COD/TDS stream is treated in Primary, Multiple Effect Evaporator (MEE) and ATFD.

Weak Stream: ETP of capacity 110 CMD comprising of primary, secondary and tertiary treatment system.

g) Domestic Effluent:

The domestic effluent connected to septic tank and soak pit.

Air Emission Load: -

sr NO	Air Emission As per EC	As per CTO	APC system provided	Stack height		Fuel (CTO)
1	Boiler - 2 TPH	Boiler 2 TPH	Dust Collector and bag filter	32 m	Coal 7 TPD	Coal 7 TPD
2	Boiler (Proposed) - 6 TPH	Boiler 6TPH	Dust Collector and bag filter		Coal 26 TPD	Coal 26 TPD
3	TFH (Existing) - 3 Lakh Kcal/Hour	Thermic Fluid heater 4Lkcal/hr	Dust Collector	20m	Coal 2.8TPD	Coal 1.21 TPD
					* FO 1.2KL/d	*FO 1.2 kl/day

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4	TFH (Proposed) - 8 lakh	Not existing				7.2 TPD	NA	
5	DG set (Existing) – 62 KVA	DG set	62 KVA	Acoustic Enclosure	2 m above the roof	HSD 500 lit/day	HSD	500 lit/day
6	DG set (Proposed) - 250 KVA	Not existing				HSD 1200 lit/day	NA	

Process Emissions:

SR NO	AS PER EC	STACK NO	New stack proposed	APC system provided	Pollutant
1	Process reactor	1 No. (S7)	Proposed new Process stack (acetonitrile)	Wet scrubber	Ammonia Gas will be absorbed in water & scrubber liquid will be Re-used in process.

- Coal consummation and steam requirement will be increased and industry has proposed to install one additional Boiler of capacity 6 TPH and Thermic Fluid Heater of capacity 8.0 Lakh Kcal./Hr.
- There will be increase in SO2 emission from 351 kg/day as stipulated in CTO to 401 kg/day.
- PP has proposed a new process scrubber for the reactor vent in proposed new plant for manufacture of Acetonitrile.

xii) Hazardous Waste Load

S. N.	Waste category	Category (as per HWM Rules, 2016)	UOM	*AS PER EC	**AS PER CTO	Existing Generation (2020-21)	Estimated Quantity - proposed expansion	* Quantity - post expansion	Remark
1	28.1	Process wastes, residue and sludges	KL/M	420	125	0	58	125	no change
2	28.6	Spent Solvents	KL/M	270	270	0	0	270	no change
3	35.3	Chemical sludge from water treatment	MT/M	210	20	11.49 MT	0	20	no change
4	26.1	Process waste sludge/residues containing acid/toxic metals/organic compounds	KL/M	210	60	No generation due to no production during the period	36.55 KL (from TMHQ) + 0.55 mt carbon sludge =37.1	60	no change

 Total Haz. Waste will remain same. However, the Liquor ammonia which will be generated from the proposed products is not included in the waste.

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Technical Committee Deliberations:

The proposed project was discussed based on documents — NIPL Certificate and presentation made by the industry. Product wise load calculation in terms of wastewater, Air emissions & Hazardous waste generation were discussed. Existing consent to operate, Environmental Clearance, NIPL Certificate issued by Aditya Environmental Services Pvt. Ltd. and product —mix Proforma are taken on the record.

After due deliberations, Committee noticed that:

- vii) PP has not switched to the cleaner fuel.
- viii) PP was unable to submit the details of Liquor Ammonia generation either in Byproducts or in Hazardous Wastes Category and disposal of the same.
- ix) The total water consumption and trade effluent generation will be increased.
- x) The Coal consumption and steam requirements will be increased.
- xi) PP was unable to submit the details of the process emissions from the exisiting products as well as from proposed products and details of comparison of the pollution load.

Technical Committee Decision:

Technical Committee decided to defer the case and asked PP to reassess their pollution load, along with the NIPL certificate and was advised the PP to furnish above details.

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Agenda item No	Item No. 6
Proposal No.	MPCB-CONSENT-0000139385
Project Details	M/s. Curia India Private Limited (Formally known as M/s Albany Molecular Research Hyderabad Research Centre Private Limited (Unit-2)) G-1/1, 1/2, MIDC area, MIDC Waluj, Aurangabad
NIPL Certificate	NIPL certificate issued by SD Engineering Services Pvt. Ltd., Date. 20.04.2022

Introduction:

This has reference to the online proposal submitted vide No. MPCB-CONSENT-0000139385 along with the copies of documents seeking amendment in existing consent to operate under change in product – mix under the provisions of EIA Notification, 2006 amended on 23/11/2016 & on 02/3/2021.

Exiting Clearances:

- Environmental Clearance is obtained vide letter no. SEAC-2015/ CR-152/ TC-2 dated 18/07/2016 and amended on 02/03/2017.
- Consent to Operate obtained vide No. Format1.0/CC/UAN No-0000090387/CR 2104000519 dated 25.05.2021 & valid up to 30.04.2023.

Project details:

Proposed change in product mix by deleting existing 3 Nos of products to the tune of 6.0 MT/M and addition of 4 nos of new proposed products to the tune of 6.0 MT/M. Industry has reported that New Products proposed to be added belongs to the same category of existing products and the total production will not exceed 65 MT/M.

I. Production Details:

Sr. No.	New Product Name	Maximum Quantity MT/M	Remarks
1.	Furosemide	15	No Change
2.	Isosorbide-5-mononitrate	6	No Change
3.	Dilute Isosorbide-5-mononitrate (10% to 90%)	10	No Change
4.	4-isothiocyanato-2-(trifluoromethyl) benzonitrile (MDV3100-6) [MDV-6]	4.5	No Change
5	Diatrizoate Sodium	6	No Change
6	Diatrizoate Meglumine	6	No Change
7	Propranolol Hydrochloride	2	No Change
8	7-acetyl-1,2,4,6,7,8,12,13,14,15,16,17-dodecahydrospiro [cyclopenta[a]phenanthrene-3,2'-[1,3]dioxolan]-17-yl acetate (Ketal Acetate)	3	No Change
9	Anecortave (5HC) Hydrocortisone Base (HC) or Tetraene Acetate (2TR)	3	No Change
10	(R)-2,7,8-trimethyl-2-((4R,8R)-4,8,12- trimethyltridecyl) chroman-6-01 or D-α- Tocopheryl	3	No Change

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	polyethylene glycol succinate Vitamin-E TPGS		20 250
11	Solifenacin Succinate	2	No Change
12	Fesoterodine	1	No Change
13	Deferasirox	2	No Change
14	Fluticasone Furoate	2	No Change
15	Indacaterol	2	No Change
16	2-Acetate	6	No Change
17	Ethyl 2,4-dihydroxy-6-pentylbenzoate (Ethyl Olivetolate)	2	No Change
18	(1S,4R)-1-methyl-4-(prop-1-en-2-yl)cyclohex-2-enol (Menthadienol)	2	No Change
19	2-(4-chloro-3-(chlorosulfonyl)benzoyl)benzoic acid (Chlorthalidone Intermediate-1/ intermediates	15	No Change
20	(4S-trans)-4-(N-acetyl-N-ethylamino)-5,6-dihydro-6-methyl-4H-thien-(2,3-b)-thiopyran-7,7-dioxide (Chiral Acetamide)	5	No Change
21	2-(Formamido-1,3-thiazol-4-yl) glyoxylic acid AZTH3 intermediate	3	No Change
22	2-Mercapto-N-methylbenzamide	3	No Change
23	Citarabine intermediate	5	No Change
24	2-3((3-Fluoro-4-(methylcarbamoyl) phenyl) amino)- 2-methylpropanoic acid (MDV 4)	6	No Change
25	4-Bromo-2-fluro-N-methyl benzamide MDV-2	8	No Change
26	6-Chloro 3 methyl Uracil (CMU)	2.5	No Change
27	5-Bromo-2-(2-methyl-2H-tetrazol-5-yl)pyridine (DA-3)	3	No Change
28	Acetyl Benzyl Amine	15	No Change
29	Sodium benzofuran-6-carboxylate (Synthon A)	4	No Change
30	2-(tert-Butoxycarbonyl)-5,7-dichloro-1,2,3,4- tetrahydroisoquinoline-6-carboxylic acid (Synthon B)	4	No Change
31	Benzyl 2-amino-3-(3-methylsulfonyl)phenyl) propanoate Hydrochloride (Synthon C)	4	No Change
32	(S)-methyl 2-methylpyrrolidine-2-carboxylate Neuren-4	3	No Change
33	(S)-dibenzyl 2-((S)-1-(2-(benzyloxy) carbonyl) amino) acetyl)-2-methylpyrrolidine-2-carboxamido) pentanedioate Neuren-7	3	No Change
34	Propionyl Chloride	15	No Change
35	2-Amino-5-bromo Benzoxazole [ML 737] OR tert- butyl (5-bromobenzo[d]oxazol-2-yl) carbamate or (BOC-ML737)	4	No Change
36	4-Amino pyrazolopyrimidine [ML739]	6	No Chang
37	Bromofluro methane (BFM)	0.5	No Chang
38.	Benzyl 2-bromo ethyl ether (BBEE)	0.75	No Chang
39.	1,6-Di Bromo hexane	5.40	No Chang
40	5-bromo-3-methyl-6-oxo-1,6-dihydropyridine-2- carboxamide (Methyl analogue of pyridine der)	1	No Chang

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	(eFT000776) OR N-(6-aminopyrimidin-4-yl) cyclopropanecarboxamide (eFT000775)		
41	1-(benzyloxy)-4-bromo-2,5 dimethoxybenzene Compound 4 (SGL Chemistry)	2	Deletion
42	N,N-bis(2.4-dichlorobenzyl) hydroxylamine (Compound 1534 Water villie)	6.5	No Change
43	tert-butyl((1s,4s)-4-aminocyclohexyl)carbamate [BOC - CIS -Diamine]	3	No Change
44	2-(4-(benzyloxy)-3-nitrophenyl)oxirane [Borregaard NSO]	3	No Change
45	6-((2-(3,4- dihydroxyphentl1)-4-oxo-4H-chromen-3-yl)oxy)-6-oxohexanoic acid [NP-202]	3	No Change
46	Miconazole Nitrate	1	No Change
47	Timolol Maleate (Timolol)	1	No Change
48	Warfarin Sodium Clathrate [Warfarin]	1	Deletion
49	1,2-Di-P-tolylethane-1,2-dione dioxime	3	No Change
50	Ethyl 2,4,6-tri-O-benzoyl-β-D-thiogalactopyranoside (PF-06460245)	3	No Change
51	Amine HCl salt 090602	3	Deletion
52	N-(3,5-dichloro-4-((6-oxo-1,6-dihydropyridazine-3-yl) oxy) phenyl) benzamide (Intermediate-C)	2	No Change
53	N-cyanoacetylurethane (NCAU)	2	No Change
54	4-acetyle-4'-(benzyloxy)-2',5'-dimethoxy-[1,1'-biphenyl]-2-carboxylic acid Compound 7 (SGL Chemistry)	2	No Change
55	(R)-2-(2-(3- (((benzyloxy)carbonyl)amino)propyl)phenoxy) propyl 4-methylbenzenesulfonate (LP101-9c)	1	No Change
56	Adrenalone HCI	5	No Change
57	Dibenzyl Artereone	5	No Change
58	2-(5-((3-Methyloxetan-3-yl)methoxy)-1H-benzo[d] imidazol-1-yl) quinolin-8-ol (ASP-187)	3	No Change
59	Apalutamide	1	No Change
60	Ziprasidone Nucleus	2.5	No Change
61	BG-4 (5-amino-3-(4-phenoxyphenyl)-1H-pyrazole- 4-carbonitrile)	2.5	No Change
62	BG-8 (tert-butyl (E)-4-(3-(dimethyl amino) acryloyl) piperidine-1 -carboxylate)	2	No Change
63	PF -06850062 (((1R,5S,6r)-3-benzyl-3-azabicyclo[3.1.0]hexan-6-yl)methanol)	1.5	No Change
64	1H-Pyrrolo[2,3-D] Pyrimidine -2, 4(3H, 7H)-Dione	2.5	No Change
65	2,4-Dichloro Pyrimidine	2.5	No Change
66	3-Cyano-5-Hydroxy Pyridine	2.5	No Change
67	Bay-28288113 (N-((R)-chroman-4-yl)-7-fluoro-4-(3-fluoroazetidin-1-yl)-8-(2,3,5-trifluorophenyl) quinoline-3 -carboxamide)	1.5	No Change
68	R & D Products	0.5	No Change
69	Distillation of spent solvent	20	No Change

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70	Tolazoline HCI	2	No Change
71	Potassium 6-(4-amino-2,6-dichlorophenoxy)-4-isopropylpyridazin-3-olate [Intermediate F]	1	No Change
72	Pravibismane- API	1	No Change
73	SNDX-5613-5 OR (N-Ethyl-5-fluoro-N-isopropyl-2- (pyrimidin-5-yloxy) benzamide)	1.5	Proposed
74	SNDX-5613-8 OR (Tert-butyl 2- (5- (2- (ethyl (isopropyl) carbamoyl) -4-fluorophenoxy) - pyrimidin-4-yl) -2,7-diazaspiro [3.5] nonane-7-carboxylate)	1.5	Proposed
75	SNDX-5613-10A OR (trans-4- ((ethylsulfonamido)cyclohexyl) methyl-4- methylbenzene sulfonate)	1.5	Proposed
76	Ligand OR (TBUPDI)	1.5	Proposed

 The overall production quantity will remain same i.e. 296.15 MT/M. The production capacity of above products is restricted to 65 MT/M as per the Consent to Operate obtained vide No. Format1.0/CC/UAN No-0000090387/CR 2104000519 dated 25.05.2021

J. Pollution load Details:

xiii) Water & Wastewater Aspect

Propose	Existing water Consumption	Water Consumption Breakup after change in product mix	Proposed Additional Water Consumption	
		Industrial		
Process + APCM	39.40	38.95		
Boiler	11	11	Water	
Cooling	14	14	Requirements	
Washing	1	1	reduced by	
Other	0	0	0.45 CMD after	
Total Industrial	65.40	64.95	proposed Change	
Domestic	10	10	in	
Gardening	5	5	Product Mix.	
Gross Total	80.40	79.95		

Propose	Existing Effluent Generation	Effluent Generation after Proposed change in product mix	Mode of Disposal & Ultimate Receiving Body
Industrial	36.78	33.53	18.48 CMD will be 100% recycle within process. 15.05 CMD will be disposed to CETP. (Reduced by 3.25 CMD after change in Product Mix)
Domestic	7	7	On Land for Gardening

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Water Consumption will reduce by - 0.45 CMD.

Effluent generation will reduce by - 3.25 CMD

Treatment System

h) Trade Effluent:

Industry has segregated trade effluent into strong & weak stream and provided treatment system as below.

Strong Stream: High COD/TDS stream is treated in Primary, Multiple Effect Evaporator (MEE) of capacity 15 CMD.

Weak Stream: ETP (25 CMD Capacity) consists of primary, secondary, and tertiary treatment system along with RO (50 CMD Capacity). 21.73 CMD is recycled and 15.5 CMD disposed to CETP.

i) Domestic Effluent:

The domestic effluent is treated in sewage treatment plant of capacity 15 CMD.

xiv) Air Emission Load: -

Sr. No.	Stack attached to	Fuel	Existing Fuel Consumption	Proposed Fuel Consumpti on	Stack Height in meter
1	Boiler –I	Briquette	7 MT/ Day	7 MT/ Day	30 m, followed by Bag filter and Mechanical dust collector
2	Boiler- II /Thermopack	LDO	0.85 MT/ Day or 0.5 MT/Day	0.85 MT/ Day Or 0.5 MT/Day	30 M
3	D.G. Set 500 KVA	HSD	0.3 TPD	0.3 TPD	4.5 M (Above the roof)
4	D.G. Set 1100 KVA	HSD	1.0 TPD	1.0 TPD	4.5 M (Above the roof)
5	Fire D.G. Set	HSD	1.0 TPD	1.0 TPD	4.5 M

Process Emissions Details:

Stack No.	Stack attached to	Stack Height	APCM	Paramet er	Permissible Limit
1	Scrubber P1	08* m	Catch Pot, Packed column	Acid Mist, HCI	35 ppm

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			with water spray		
2	Scrubber P2	26 m	Catch Pot, Packed column with water spray	SO2, Acid Mist, HCI	35 ppm
3	Scrubber P3	14 m	Catch Pot, Packed column with water spray	SO2	35 ppm
4	Scrubber P4	30 m	Catch Pot, Packed column with water spray	SO2	35 ppm

- The process emissions will remain same as per exisitng.
- Industry has proposed Ammonia as a one of the new raw material, however PP has not shown the details of Ammonia emissions and Pollution Control systems.

xv) Hazardous Waste Load

Sr. No.	Type of Wast	Categor y (As per	Ye	Generation per Year (No change)		Mode of Storag	Mode of Treatme nt&
	e Se	Schedul e)	Existin g	After Change in Produ ctMix	n	е	Disposal
1	Used / spent Oil	5.1/ 5.2	200 kg/M	200 kg/M	D.G. Sets, Gear box of machiner	HDPE Drums	Sale to authorized party/ CHWTSDF
2	Spent Solvent	20.2	190000 kg/M	190000 kg/M	Productio n Plant	HDPE /GI Drums /SS tank	Sale to authorized party/ CHWTSDF
3	Process Waste & Residue	28.1	34666 kg/M	34666 kg/M	Productio n plant	GI Drum	CHWTSDF
4	Spent Catalyst/ Spent Carbon	28.2	6845 kg/M	6845 kg/M	Productio n plant	Polythene Bags	CHWTSDF
5	Spent Catalyst/ Spent Carbon	28.2	2000 Kg/M	2000 Kg/M	Productio n plant	Polythene Bags	Spent Hyflow to CHWTSDF
6	Off Specification/ Discarded Drug, medicine product		1000 kg/M	1000 kg/M	Productio n plant	HDPE drum	CHWTSDF

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7	Spent Mother Liquor (Dilute Caustic Lye)	28.6	10 MT/M	10 MT/M	Productio n plant	HDPE /GI Drums /SS tank	Dil. Caustic Lye Sale to Authorized party/ CHWTS DF
8	Spent Mother Liquor	28.6	17600 kg/M	15563 Kg/M	Productio n Plant	HDPE /GI Drums /SS tank	CHWTSDF
9	Spent organic Solvent	28.6	81300 kg/M	79142 Kg/M	Productio n Plant	HDPE /GI Drums /SS tank	Sale to authorized party/ recycle/CH WTSDF
10	Discarded Containers/Barrel / liner	33.1	100 Nos./ M	100 Nos./M	Painting of structure	HDPE drum	Sale to authorized party/ recycle/CH WTSDF
11	Chemical Sludge from Waste Water treatment	35.3	5823 kg/M	5823 kg/M	Effluent treatme ntplant	Sludge drying Bed / Polythene bags	CHWTSDF
12	Chemical Sludge, Oil & grease skimming residue	35.4	100 kg/M	100 kg/M	Oil & Grease trap	HDPE drum	CHWTSDF
13	Cotton rags and other cleaning material	33.2	100 Kg/M	100 Kg/M	Productio n Plant	At Secure Storage/ As per Guideline	CHWTSDF

Total Haz. Waste will remain same.

Technical Committee Deliberations:

The proposed project was discussed based on documents – NIPL Certificate and presentation made by the industry. Product wise load calculation in terms of wastewater, Air emissions & Hazardous waste generation were discussed. Existing consent to operate, Environmental Clearance, NIPL Certificate issued by SD Engineering Services Pvt. Ltd. and product –mix Proforma are taken on the record.

After due deliberations, Committee noticed that:

- The PP was unable to show the groupwise scheme of products with pollution load of the group.
- The PP was unable to show the change in pollution load, along with the characteristics of the existing and proposed Strong stream and weak stream effluent.
- The PP has proposed Ammonia as new raw material for the proposed product, however, was unable to show the details of Ammonia Emissions, Pollution Control Systems and Liquor Ammonia etc.

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4) PP was unable to submit the details of the process emissions from the existing products as well as from proposed products with comparison of the pollution load.

Technical Committee Decision:

Technical Committee decided to defer the case and asked PP to reassess their pollution load, along with the NIPL certificate and was advised the PP to furnish above details.

June 1